

Micromechanics of granular materials: slow flows

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Applications of granular materials

- geotechnical engineering
- geophysical flows
- bulk solids engineering
- chemical process engineering
- mining
- gas and oil production
- food-processing industry
- agriculture
- pharmaceutical industry

Features

- rate-independent
- elasticity
- plasticity
- frictional
- dilatancy
- anisotropy

- viscous
- multi-phase
- cohesion
- segregation

Overview talk

- Introduction
- Continuum modelling
- Micromechanical modelling
 - Effect of interparticle friction on macroscopic behaviour
 - Validity of mean-field approaches
- Mixing in rotating cylinders

Slow granular flows

- Rate-independent; quasi-static
- Continuum level
 - stress tensor
 - strain tensor

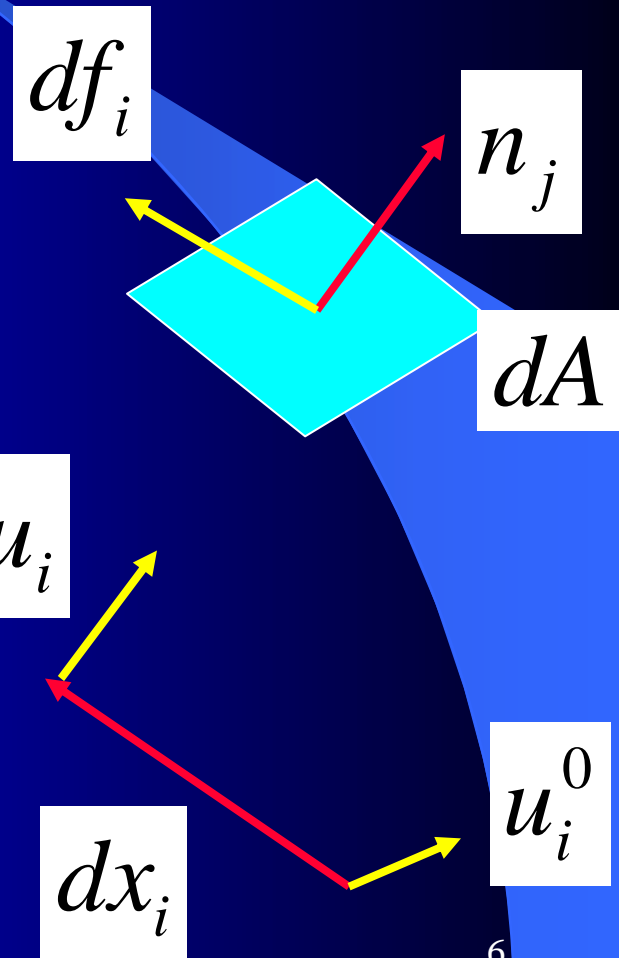
Stress and strain tensors

- Stress tensor

$$df_i = n_j \sigma_{ji} dA$$

- Strain tensor

$$du_i = \varepsilon_{ij} dx_j$$



Constitutive relations

- Continuum theories; elasto-plasticity
 - elastic and plastic strains
 - yield function
 - flow rule: plastic potential
- Micromechanical theories
 - relation with microstructure

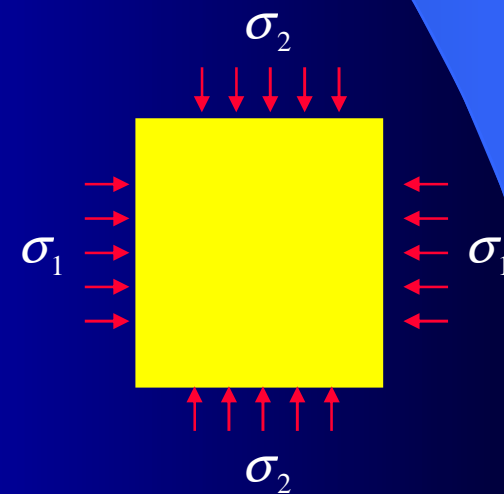
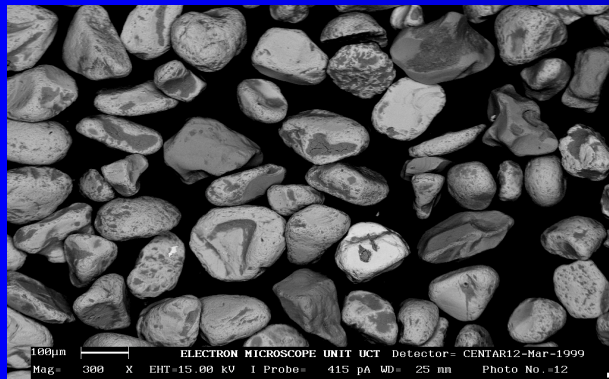
Plasticity of metals \leftrightarrow granular materials

- pressure dependence
- volume changes: dilatancy
- non-associated flowrule
- strain-softening

Micromechanics of slow flows

Study relation between micro and macro level

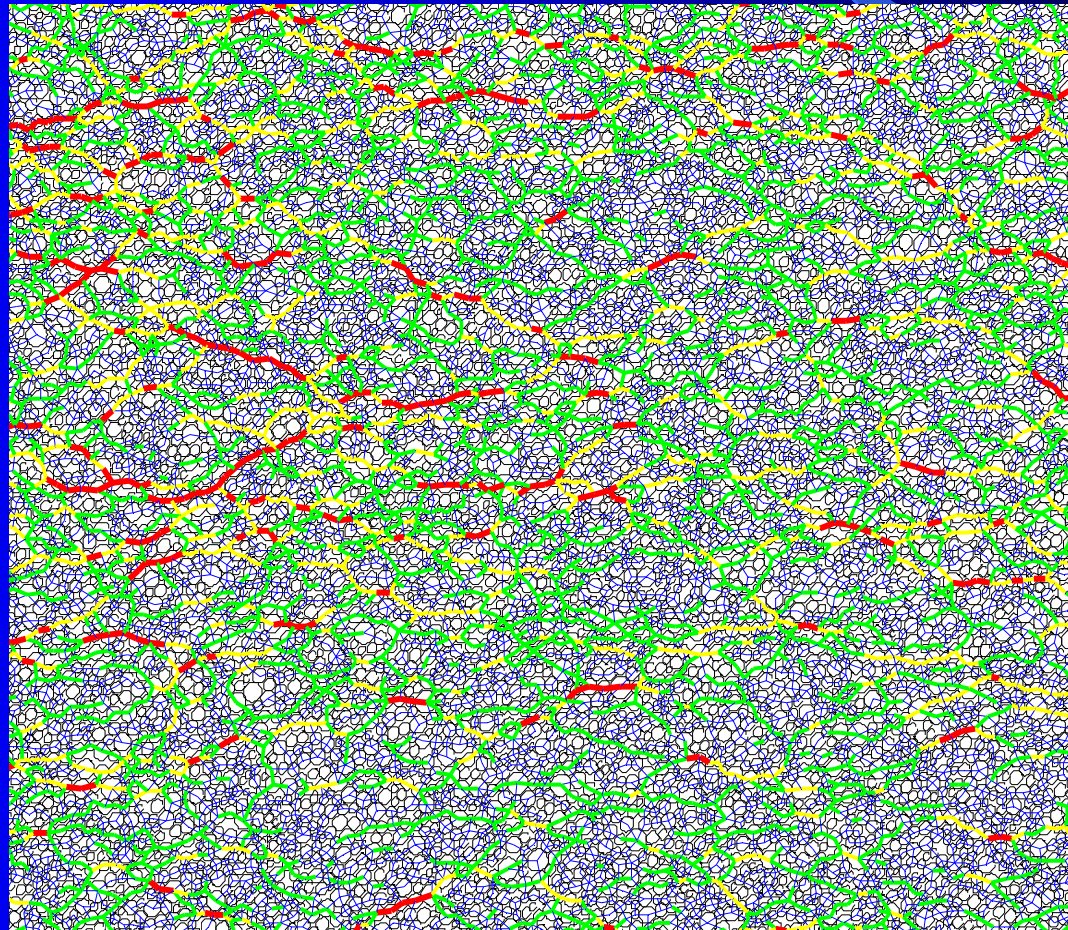
Work with Leo Rothenburg, University of Waterloo,
Canada



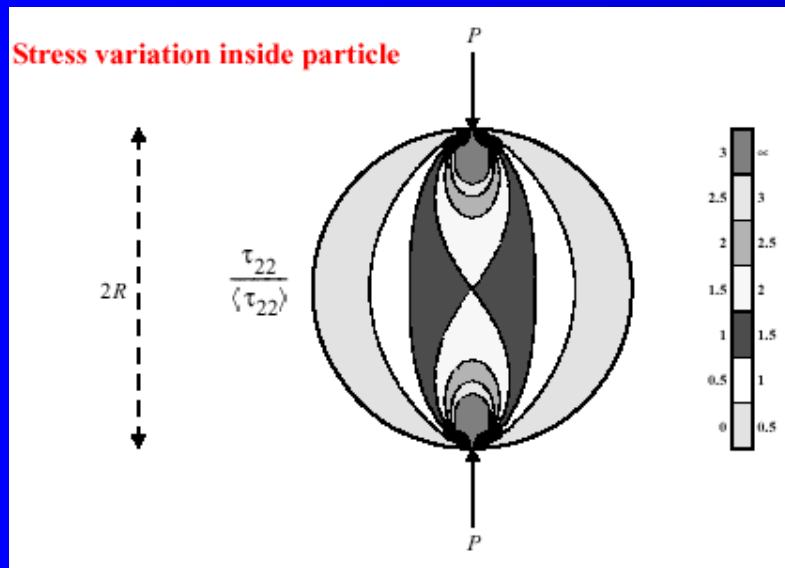
Objective

- Micro-level \rightarrow macro-level
- Account for the discrete nature
- Emphasis on slow flows
 - Elasticity
 - Plasticity
- Theory and DEM simulations

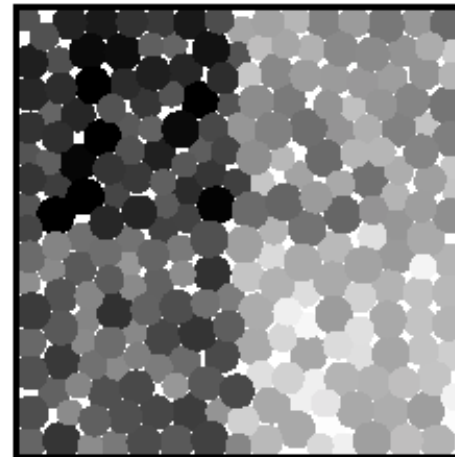
From discrete information → stress and strain



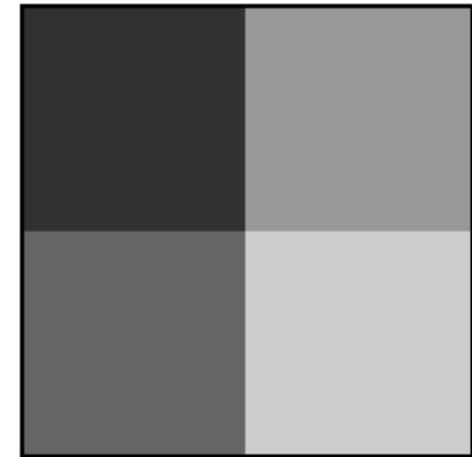
Averaging/homogenisation



Discrete assembly



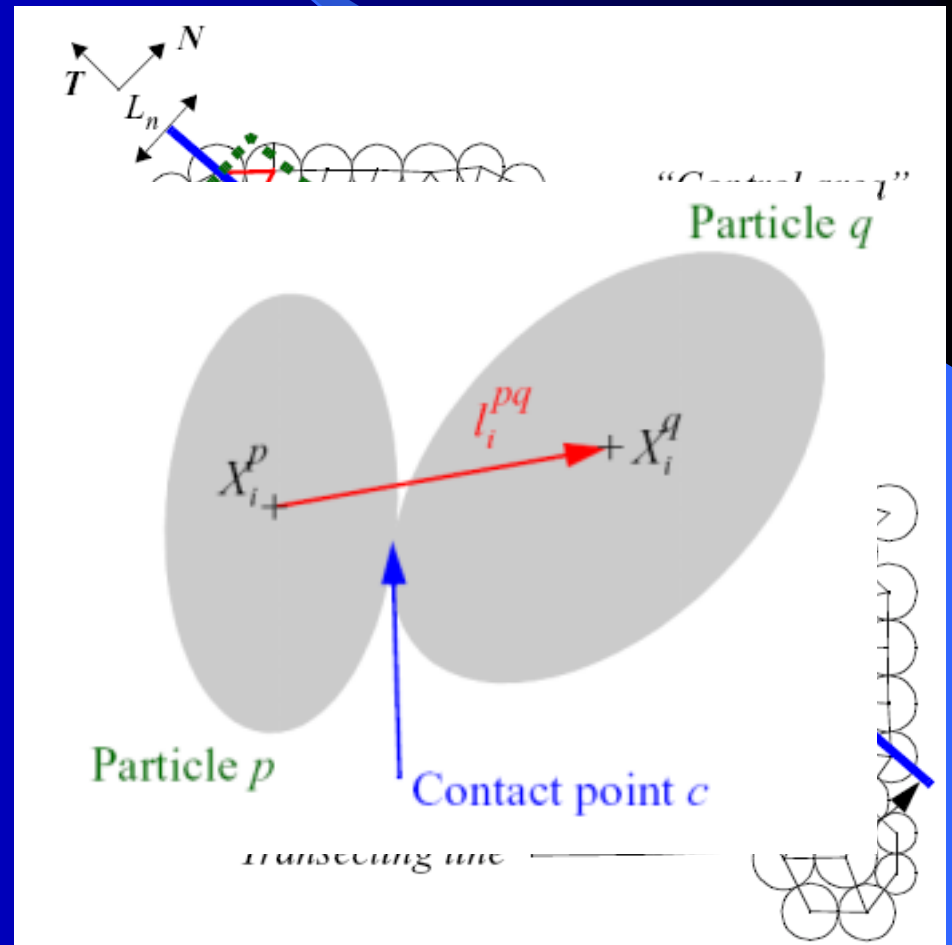
Homogenized continuum



Stress

$$F_i^R = A_{\text{plane}} N_j \sigma_{ji}$$

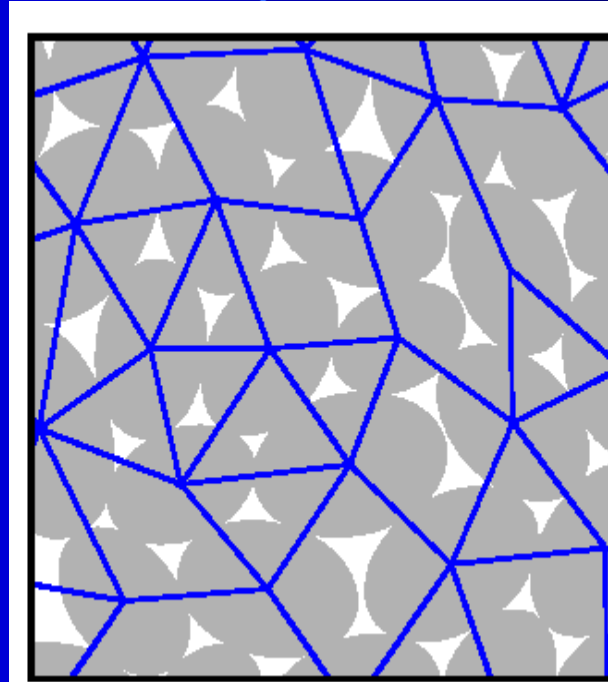
$$\bar{\sigma}_{ij} = \frac{1}{V} \sum_{c \in C} l_i^c f_j^c$$



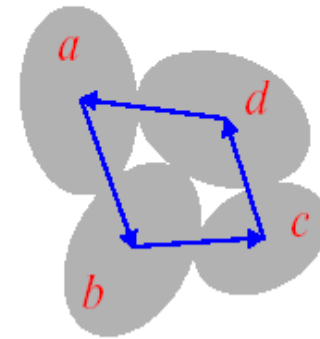
Compatibility equations

$$\Delta_i^{pq} = U_i^q - U_i^p$$

$$\sum_S \Delta_i^{RS} + \Delta_i^{R\alpha} = 0$$



Network connecting
particle centres



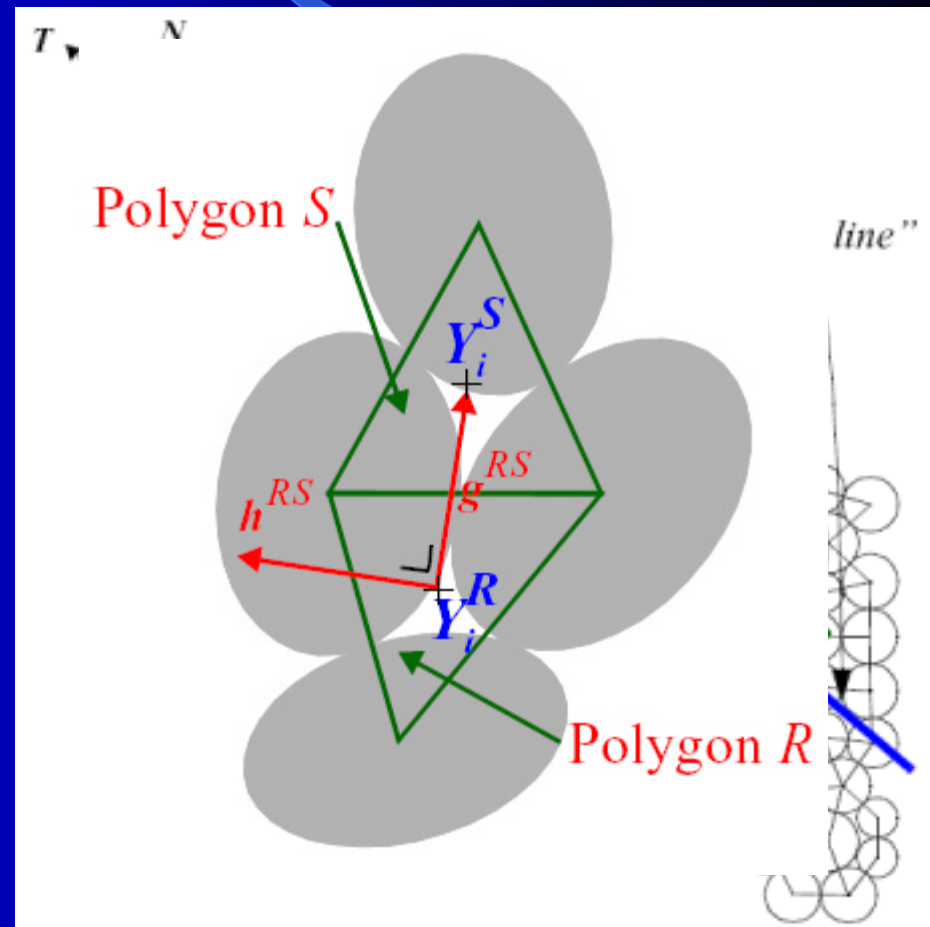
$$\begin{aligned} \sum_S \Delta_i^{RS} &= \Delta_i^{ab} + \Delta_i^{bc} + \Delta_i^{cd} + \Delta_i^{da} \\ &= [U_i^a - U_i^b] + [U_i^b - U_i^c] + [U_i^c - U_i^d] + [U_i^d - U_i^a] \\ &= 0 \end{aligned}$$

Strain

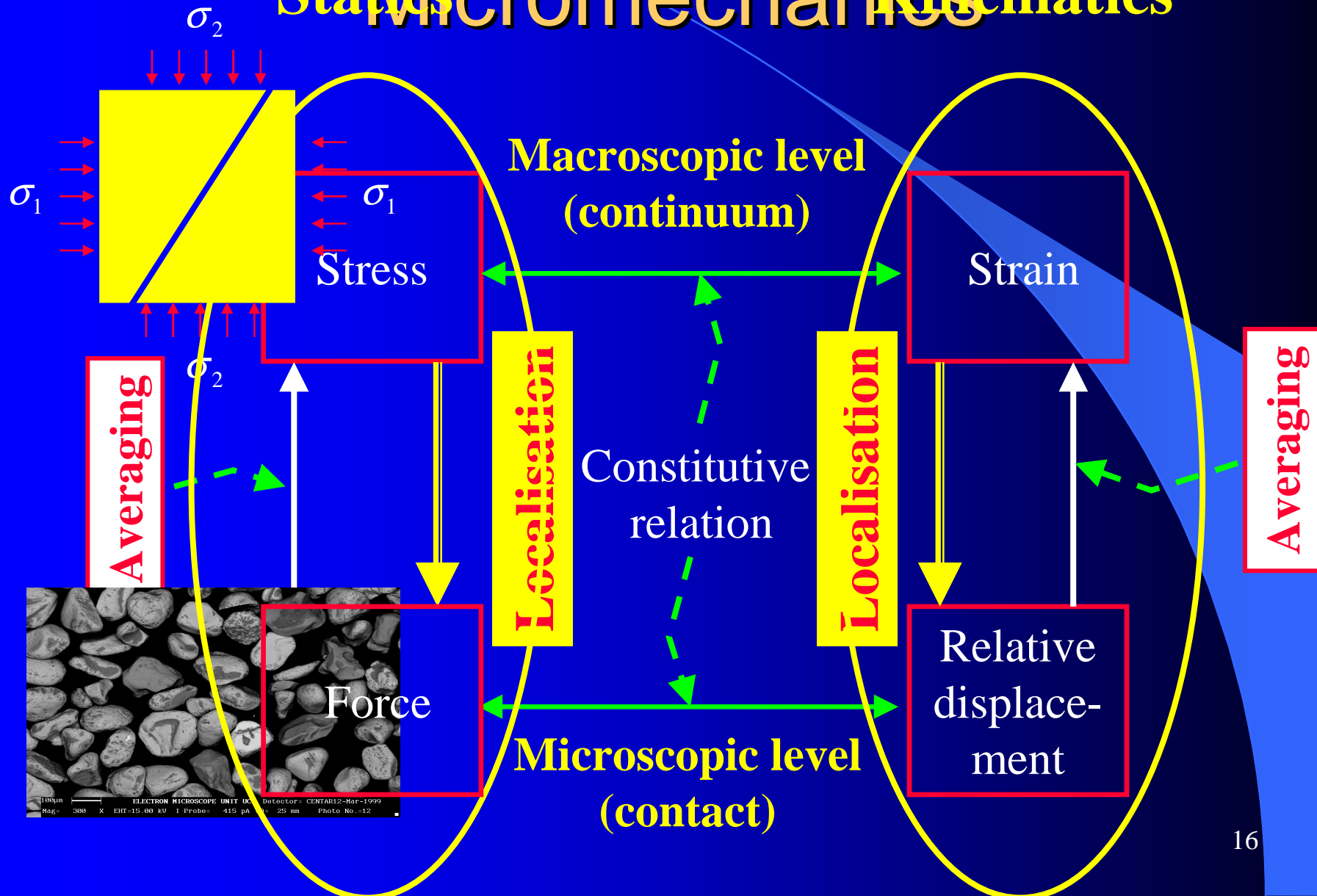
$$dU_i^L = \varepsilon_{ij} dX_j$$

$$\bar{\varepsilon}_{ij} = \frac{1}{A} \sum_{c \in C} h_j^c \Delta_i^c$$

$$\Delta_i^{pq} = U_i^q - U_i^p$$



Static Micromechanics Kinematics

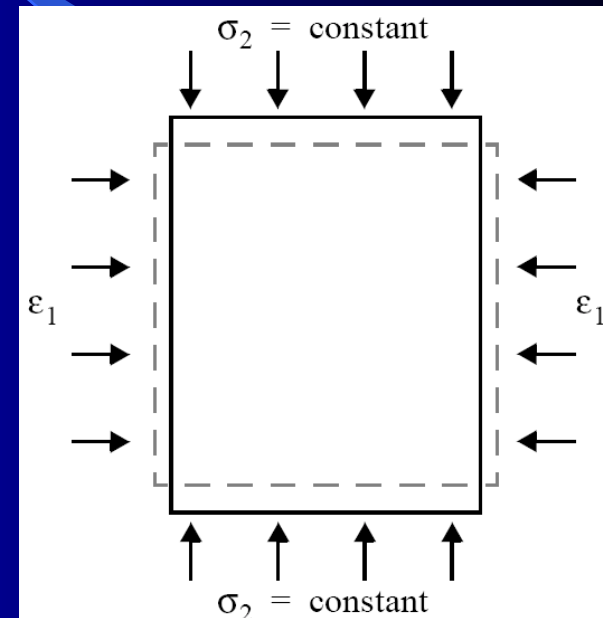


Topics in micromechanics

- Importance of geometrical anisotropy
- Effect of interparticle friction on macroscopic behaviour
- Validity of mean-field approach

DEM simulations

- biaxial deformation
- two-dimensional
- **various friction coefficients μ**
- dense and loose initial assembly
- periodic boundary conditions
- 50,000 disks



Invariants:

$$p = \frac{1}{2}(\sigma_1 + \sigma_2) \quad \epsilon_V = \epsilon_1 + \epsilon_2$$

$$q = \frac{1}{2}(\sigma_1 - \sigma_2) \quad \epsilon_S = \epsilon_1 - \epsilon_2$$

Contact constitutive relation

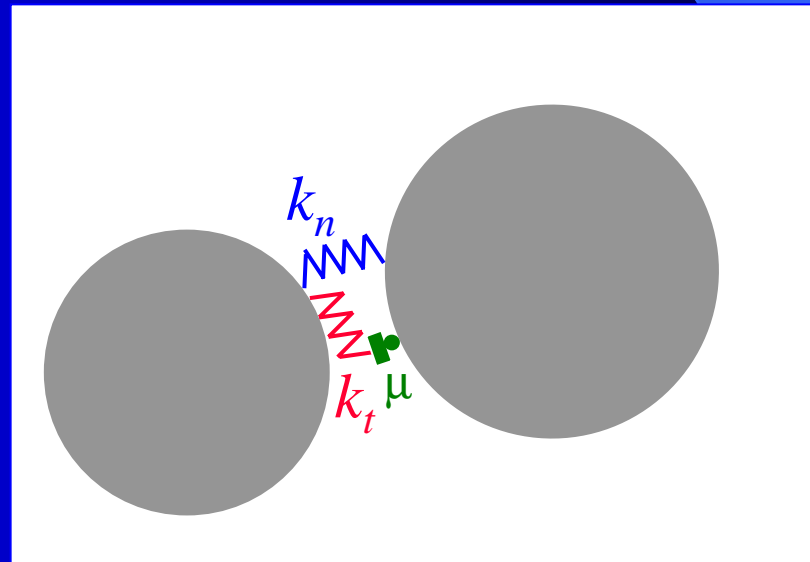
$$f_n^c = k_n \Delta_n^c$$

$$f_t^c = k_t \Delta_t^c$$

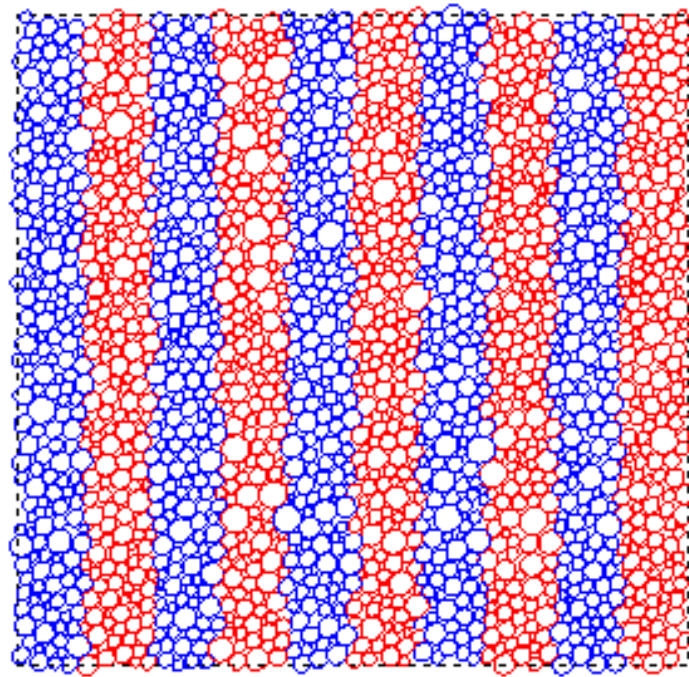
$$|f_t^c| \leq \mu \cdot f_n^c$$

Special cases:

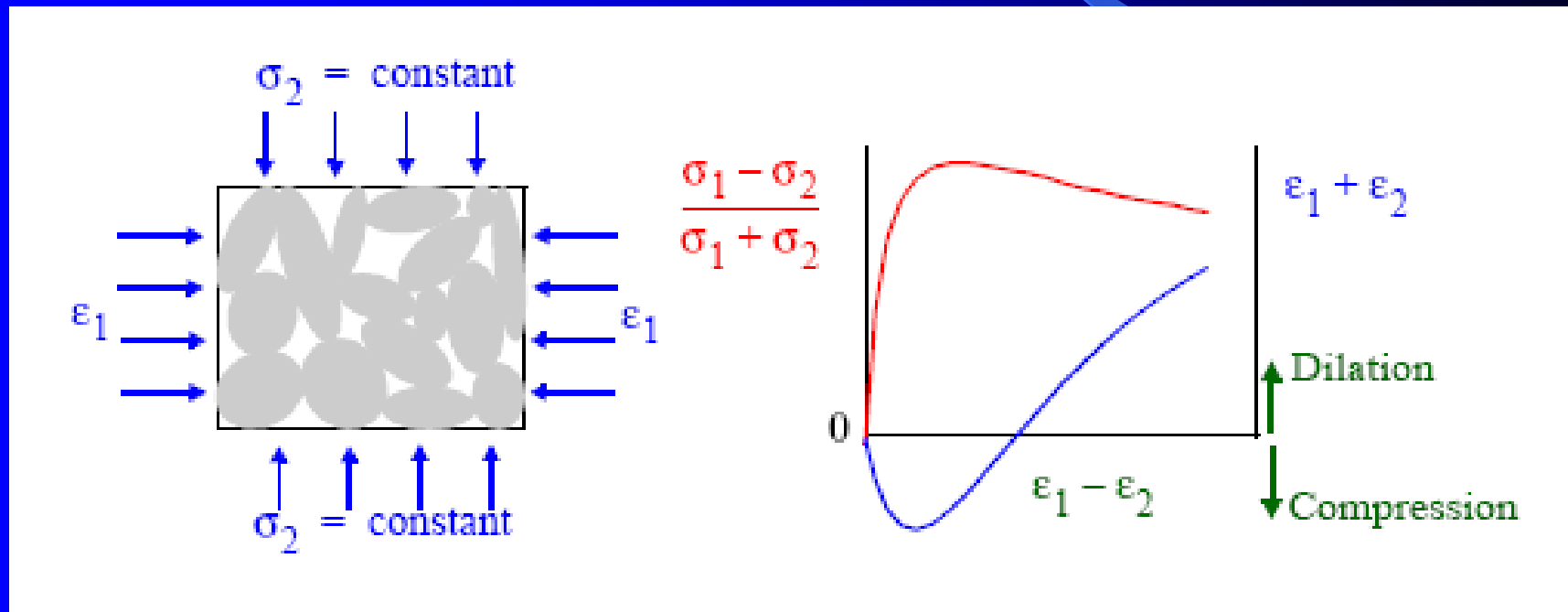
- $\mu \rightarrow 0$
- $\mu \rightarrow \infty$



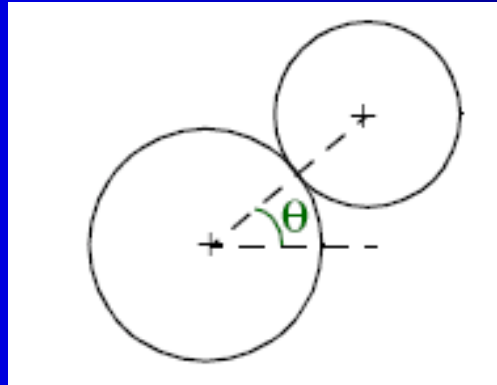
Animation



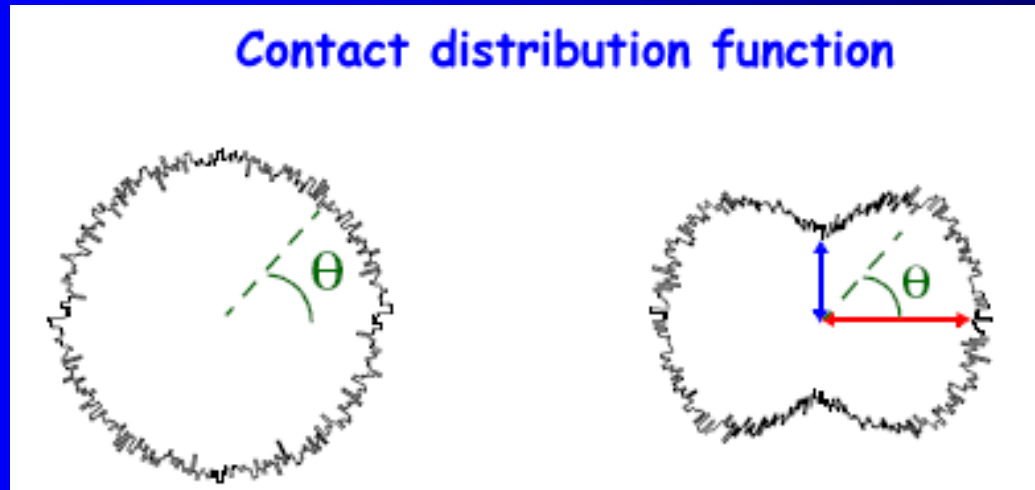
Macroscopic response



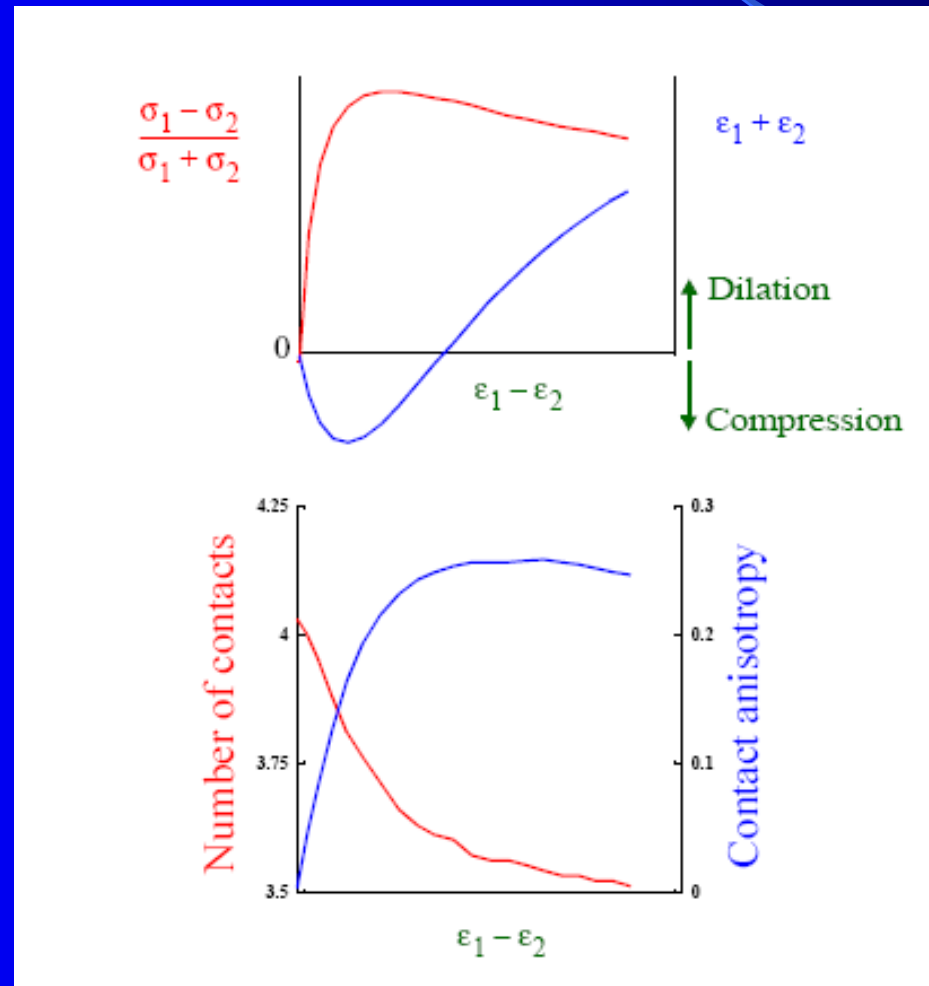
Fabric



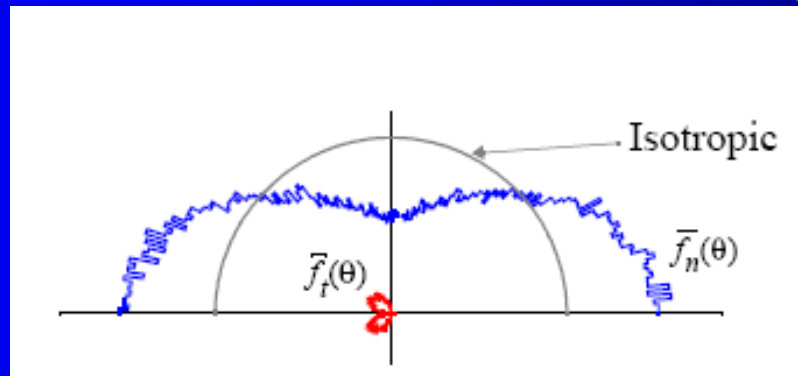
Contact distribution function



Induced anisotropy



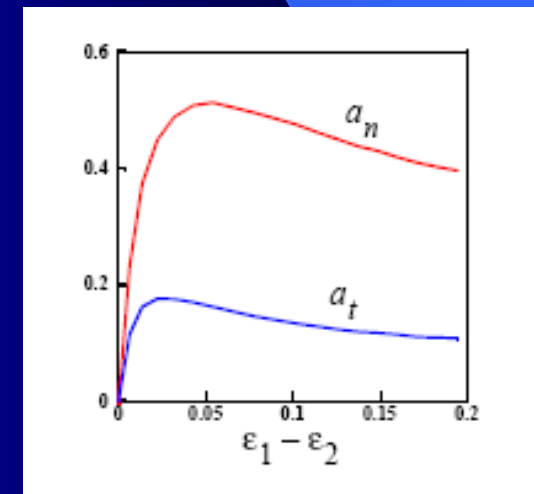
Force-fabric-strength (1)



$$E(\theta) = \frac{1}{2\pi} [1 + a_c \cos 2(\theta - \theta_0)]$$

$$\bar{f}_n(\theta) = f_0 [1 + a_n \cos 2(\theta - \theta_0)]$$

$$\bar{f}_t(\theta) = -a_t f_0 \sin 2(\theta - \theta_0)$$

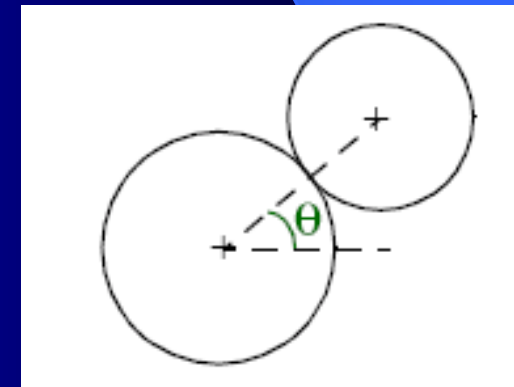


Force-fabric-strength (2)

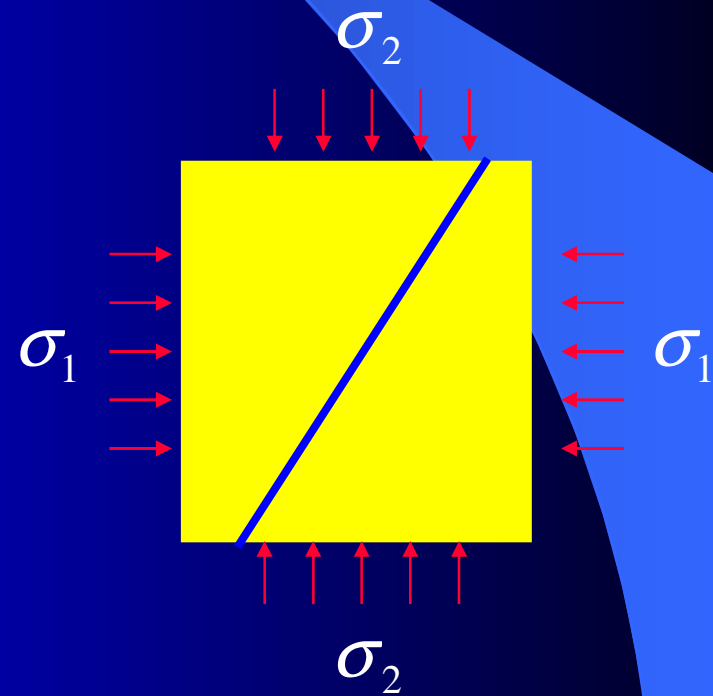
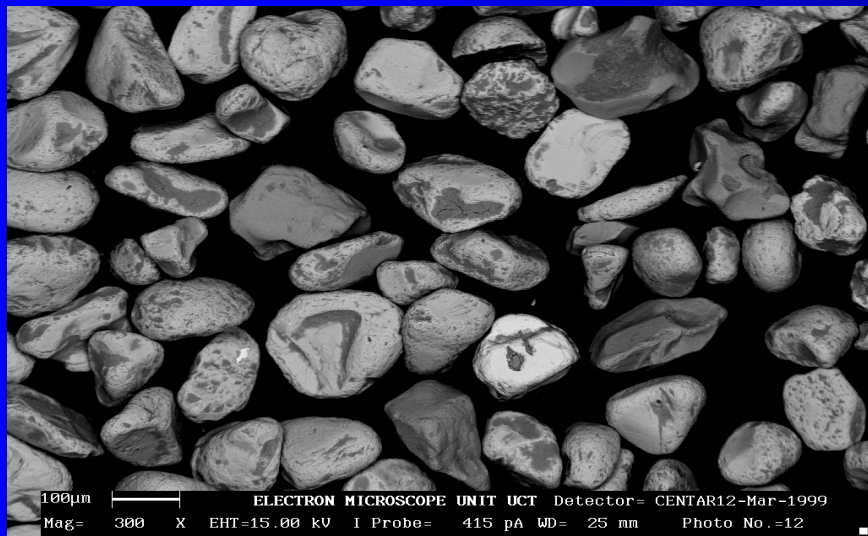
$$\bar{\sigma}_{ij} = \frac{1}{V} \sum_{c \in C} l_i^c f_j^c = \frac{1}{V} \sum_g \sum_{c \in C_g} l_i^c f_j^c$$

$$\bar{\sigma}_{ij} = \frac{1}{V} \sum_g N_{c,g} \overline{l_i f_j}(\theta_g) \cong m_V \int_0^{2\pi} E(\theta) \bar{l}_i(\theta) \bar{f}_j(\theta) d\theta$$

$$\frac{\sigma_1 - \sigma_2}{\sigma_1 + \sigma_2} \cong \frac{1}{2} [a_c + a_n + a_t]$$

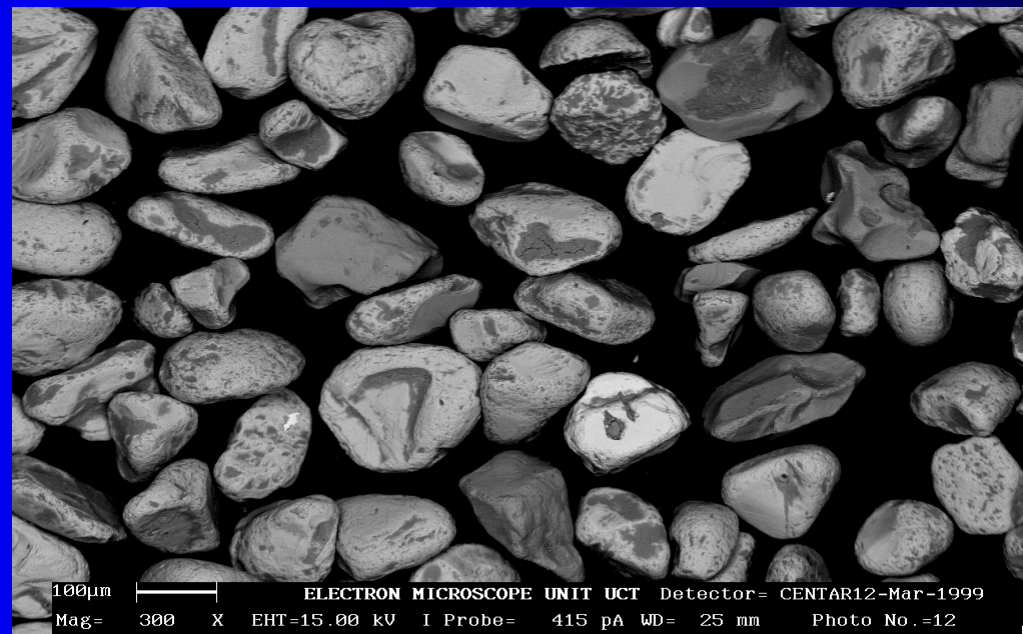


Effect of interparticle friction on macroscopic behaviour



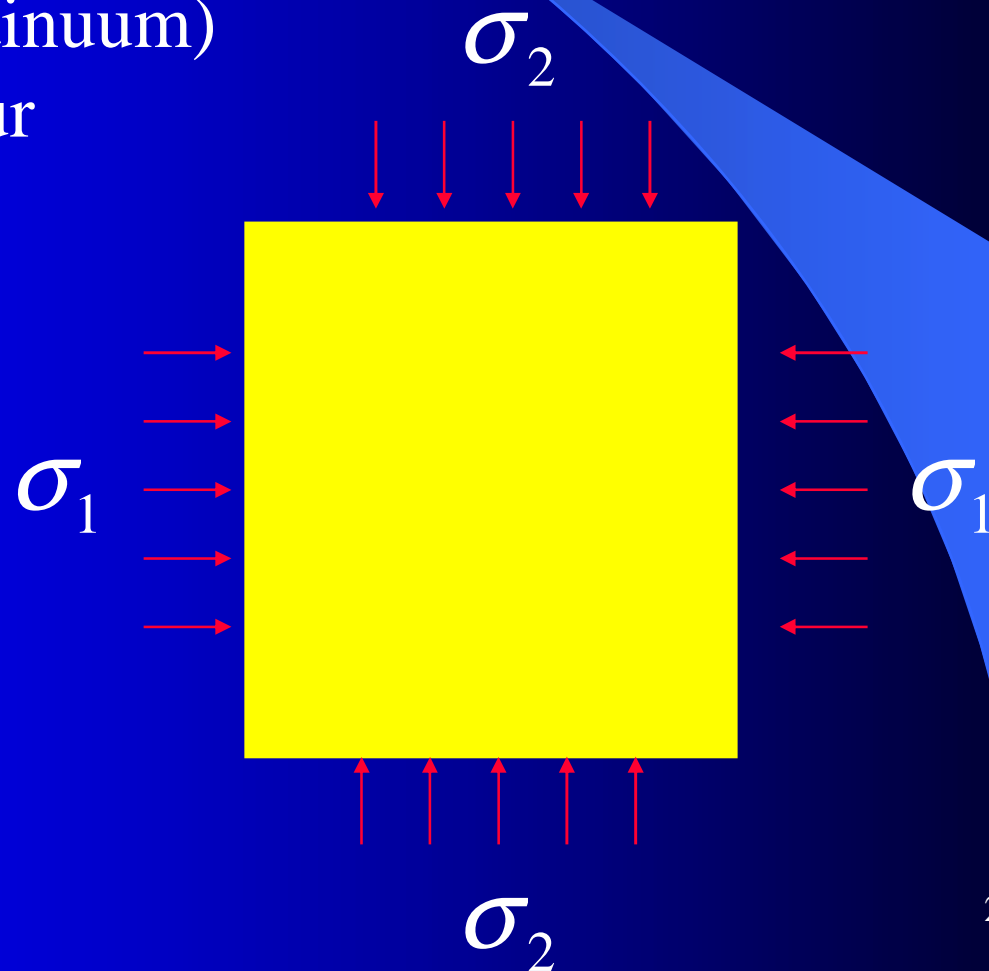
Granular materials are frictional (1)

Microscopic (contact)
frictional behaviour



Granular materials are frictional (2)

Macroscopic (continuum)
frictional behaviour



Correlations between microscopic and macroscopic friction

Horne (1965)

$$\tan^2\left(\frac{\pi}{4} + \frac{1}{2}\phi_{\text{peak}}\right) = 2 \tan\left(\frac{\pi}{4} + \phi_{\mu}\right)$$

Weak dependence of macroscopic friction on microscopic friction:

- experimentally (Skinner, 1969)
- numerically (Cambou, 1993)

Bishop (1954)

$$\sin \phi_{\infty} = \frac{15 \tan \phi_{\mu}}{10 + 3 \tan \phi_{\mu}}$$

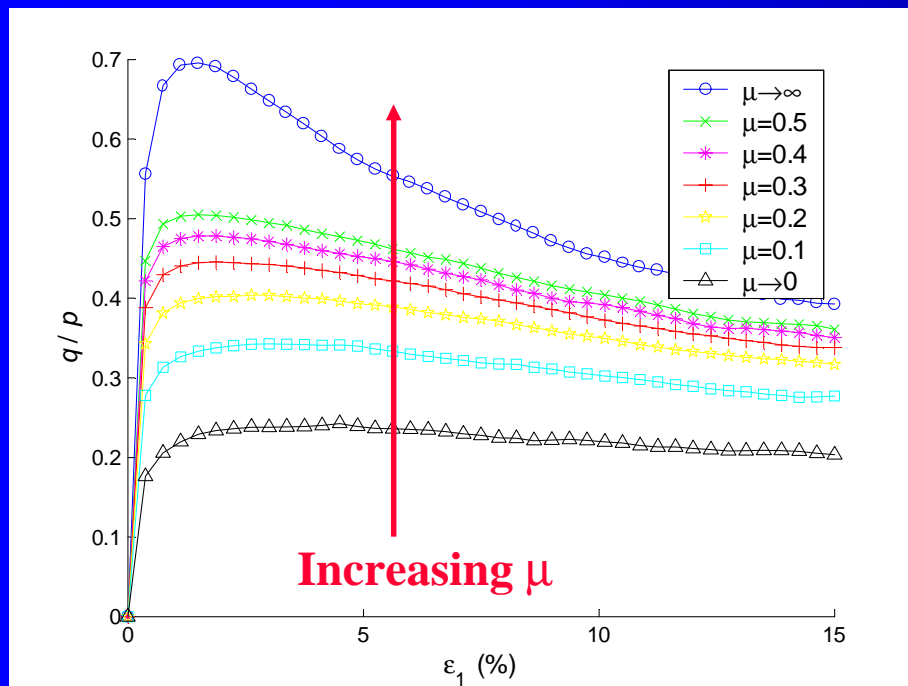
$$\mu = \tan \phi_{\mu}$$

Influence μ

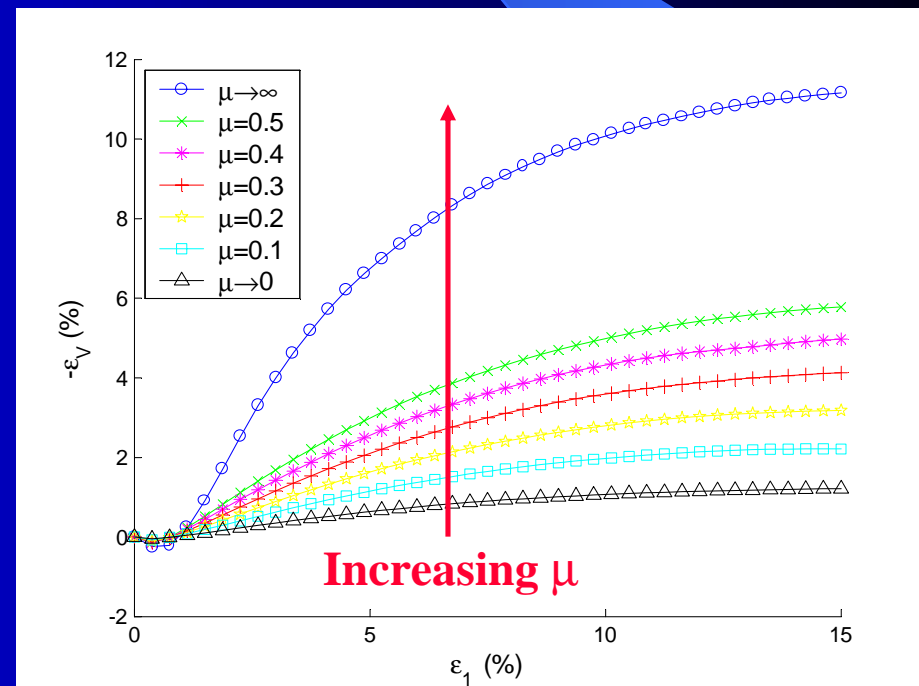
- shear strength
- dilatancy
- energy
- dissipation

Shear strength and dilatancy

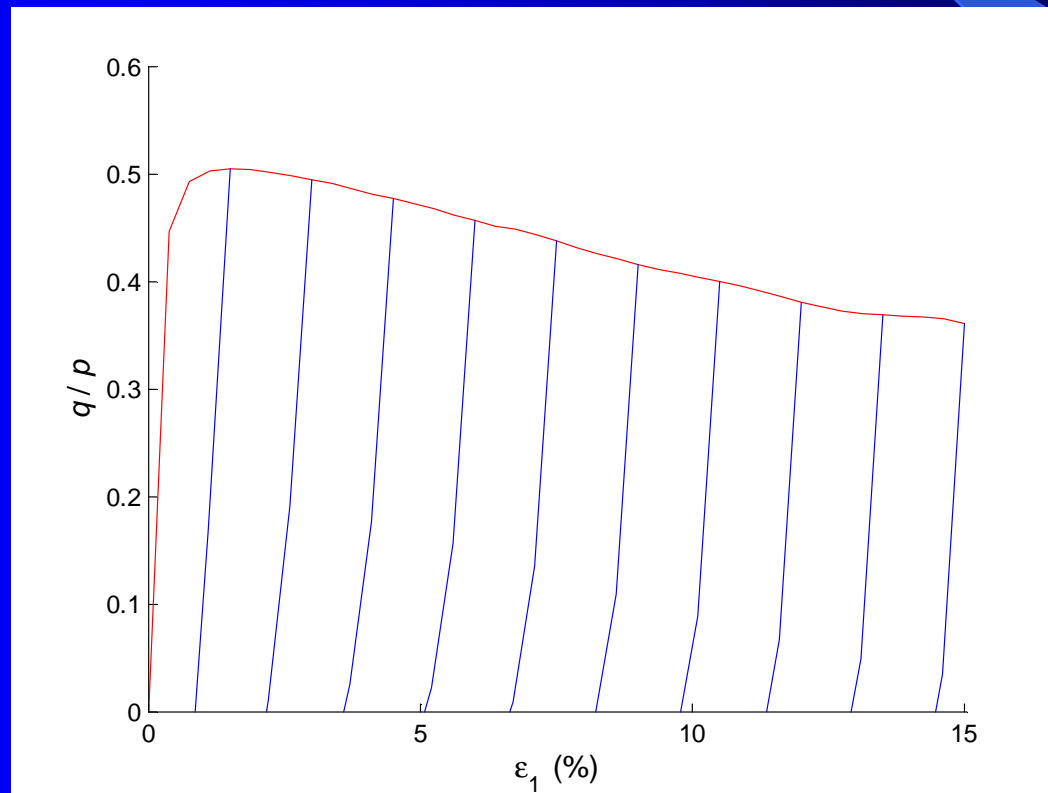
Shear strength



Dilatancy

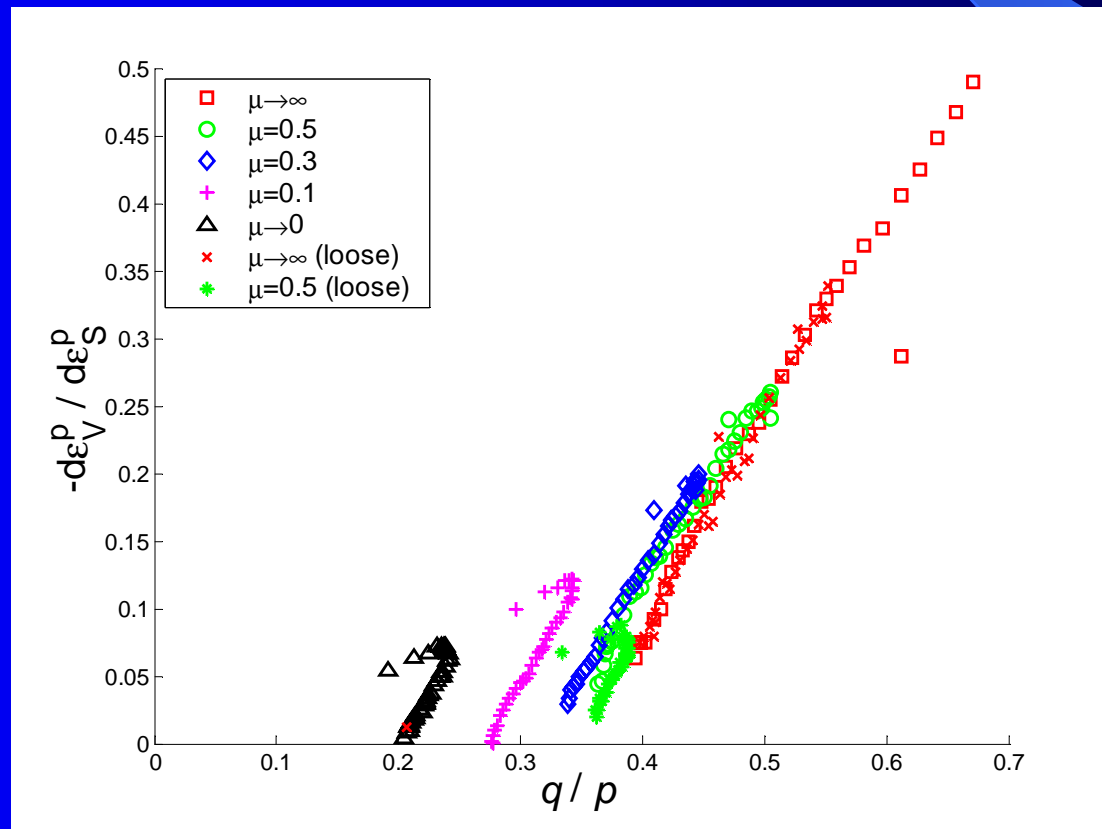


Plastic strains: unloading paths

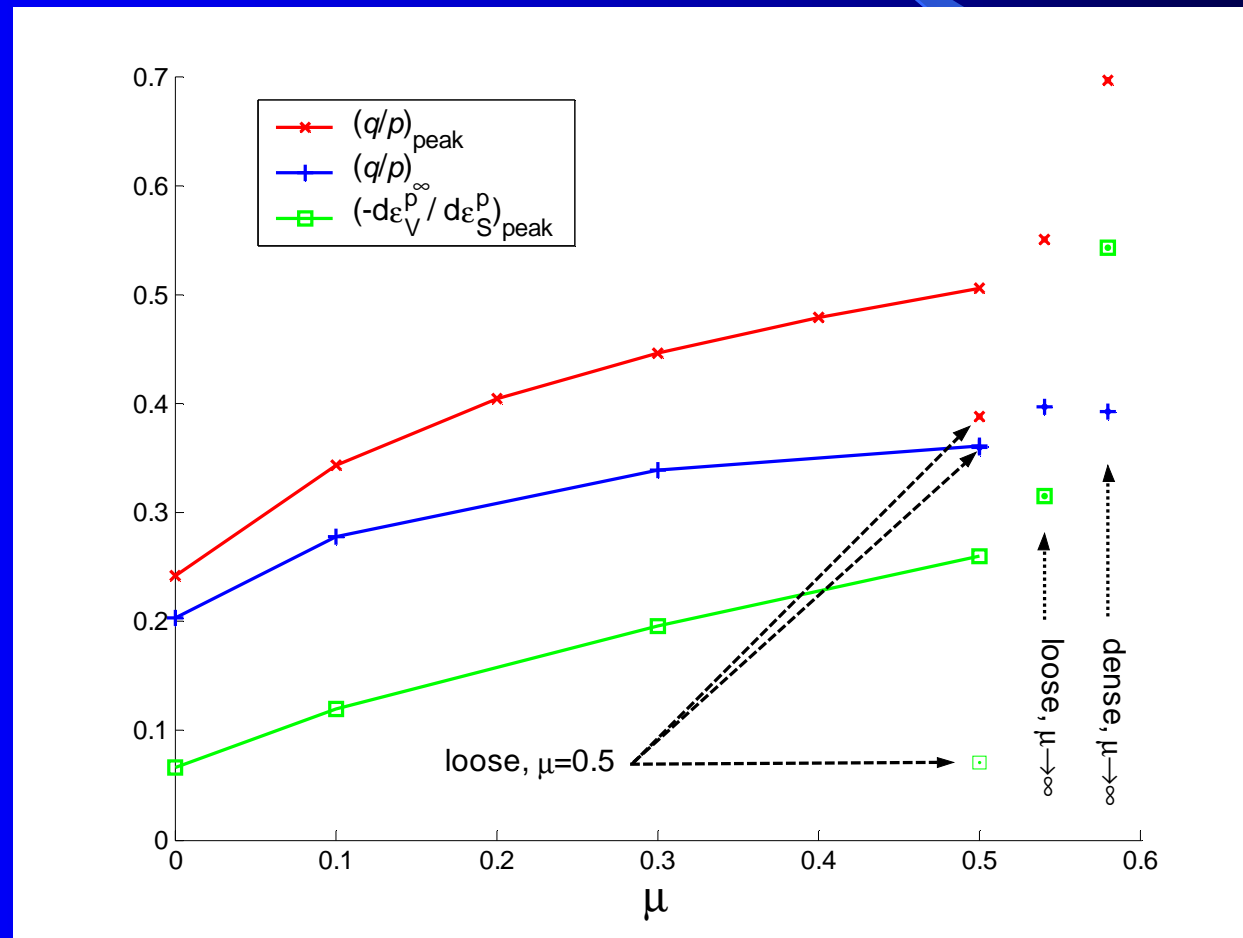


Dilatancy rate $-\frac{d\varepsilon_V^p}{d\varepsilon_S^p}$

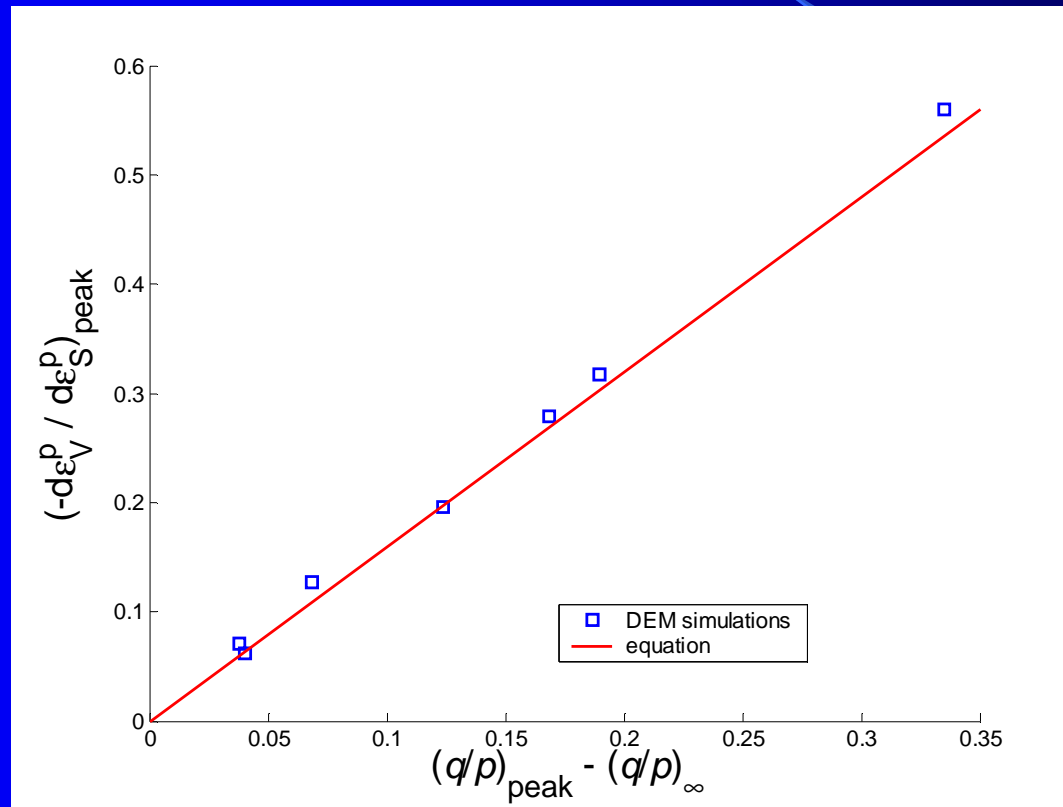
Formulated in *plastic* strains



Strength at peak & steady-state, dilatancy rate at peak strength



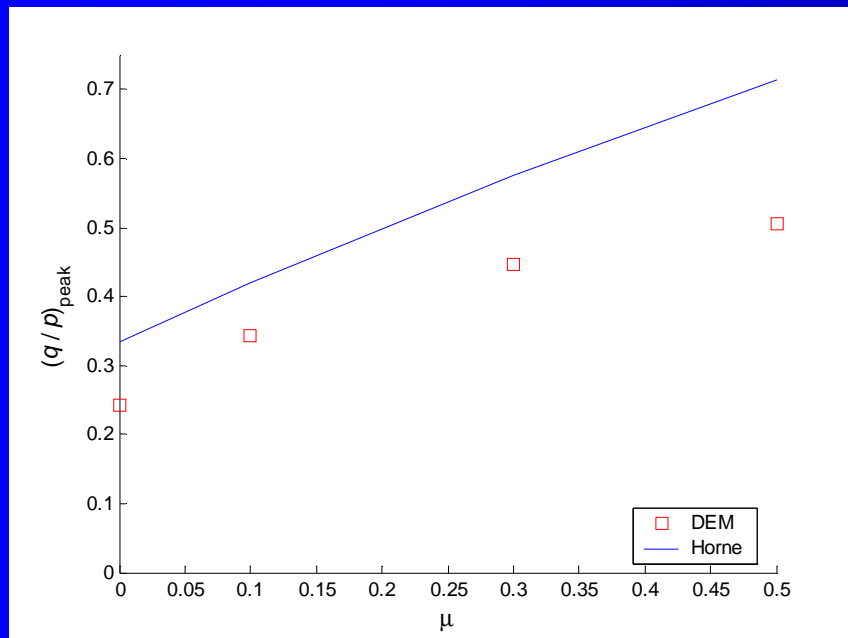
Strength-dilatancy relation



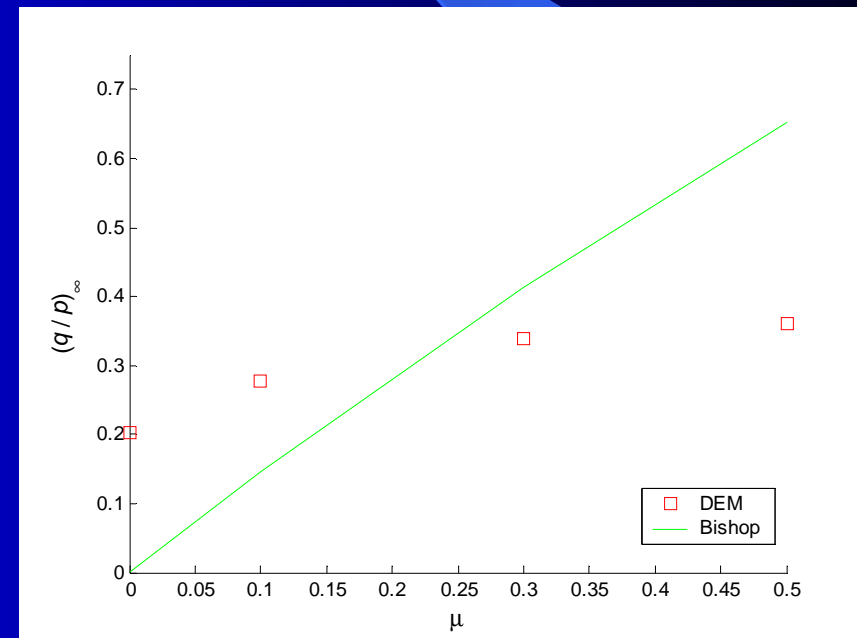
$$\left(-\frac{d\varepsilon_V^p}{d\varepsilon_S^p} \right)_{\text{peak}} = \alpha \left[(q/p)_{\text{peak}} - (q/p)_{\infty} \right]$$

Strength correlations vs. simulations

Peak strength



Steady-state strength

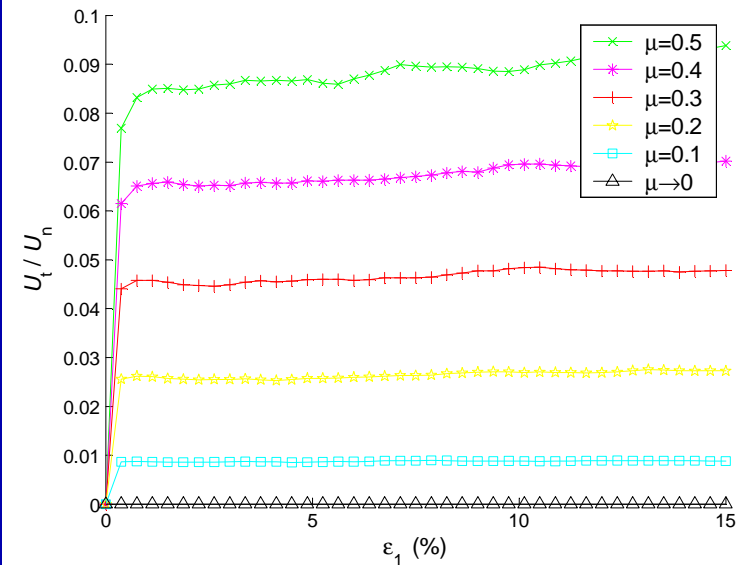
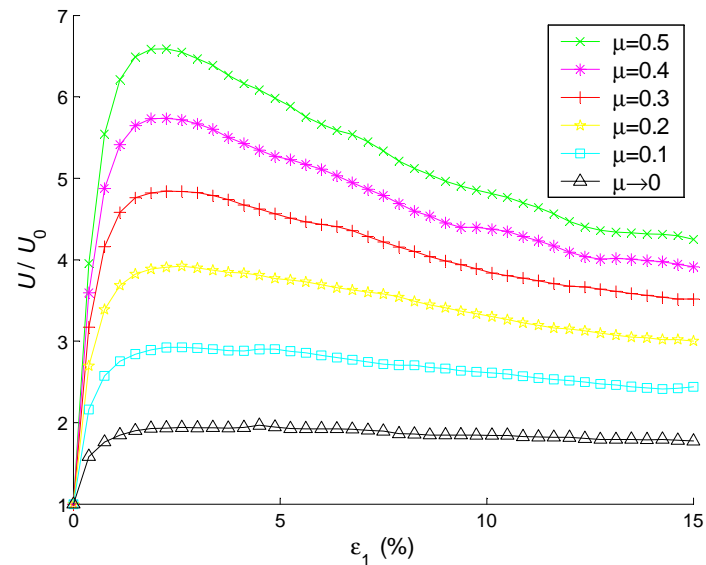


Energy

$$U_n = \frac{1}{V} \sum_{c \in C} \frac{1}{2k_n} [f_n^c]^2$$

$$U_t = \frac{1}{V} \sum_{c \in C} \frac{1}{2k_t} [f_t^c]^2$$

$$U = U_n + U_t$$



Dissipation

Dissipation

Work
input

Change
in energy

$$\begin{aligned}\delta D &\cong \delta W - dU \\ &= \sigma_{ij} d\varepsilon_{ij} - dU\end{aligned}$$

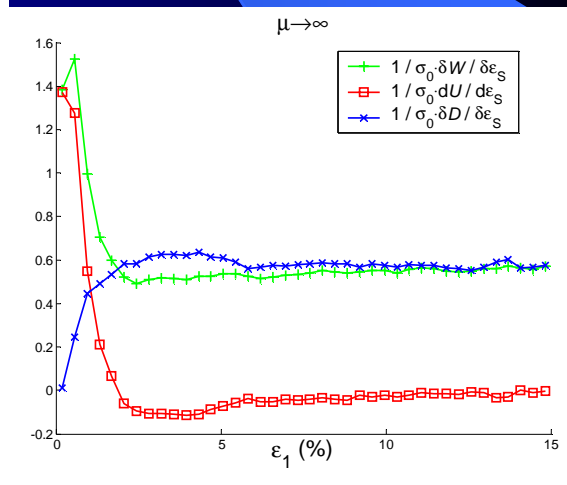
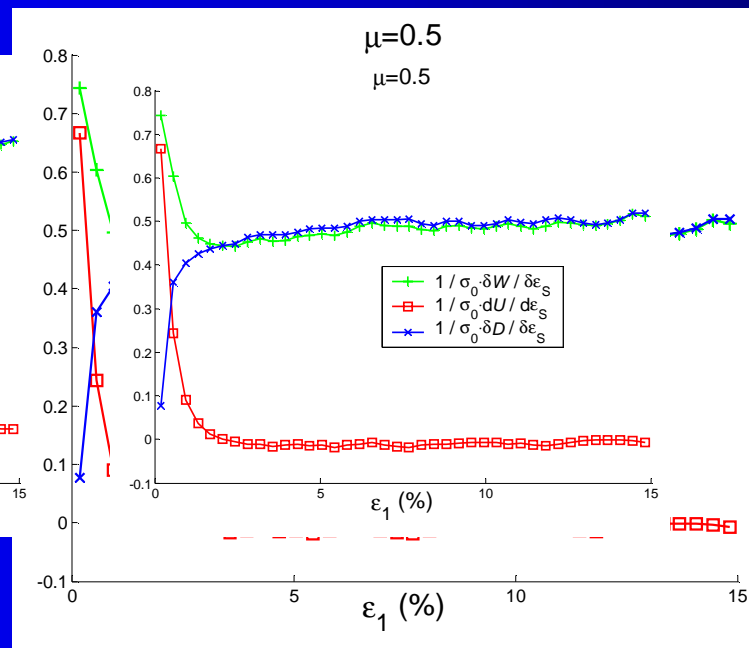
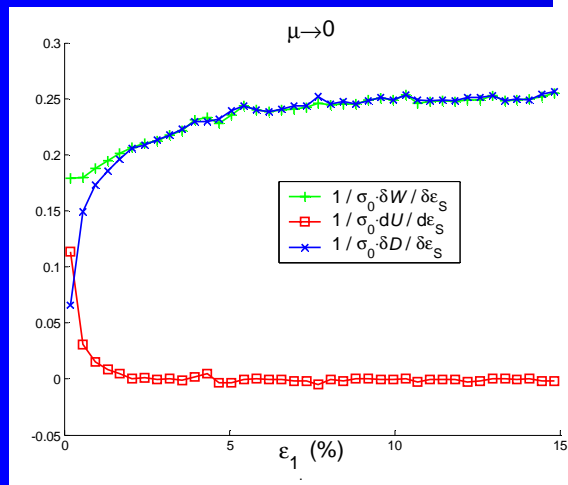
Dissipation

Dissipation

Work
input

Change
in energy

$$\delta D \cong \delta W - dU$$

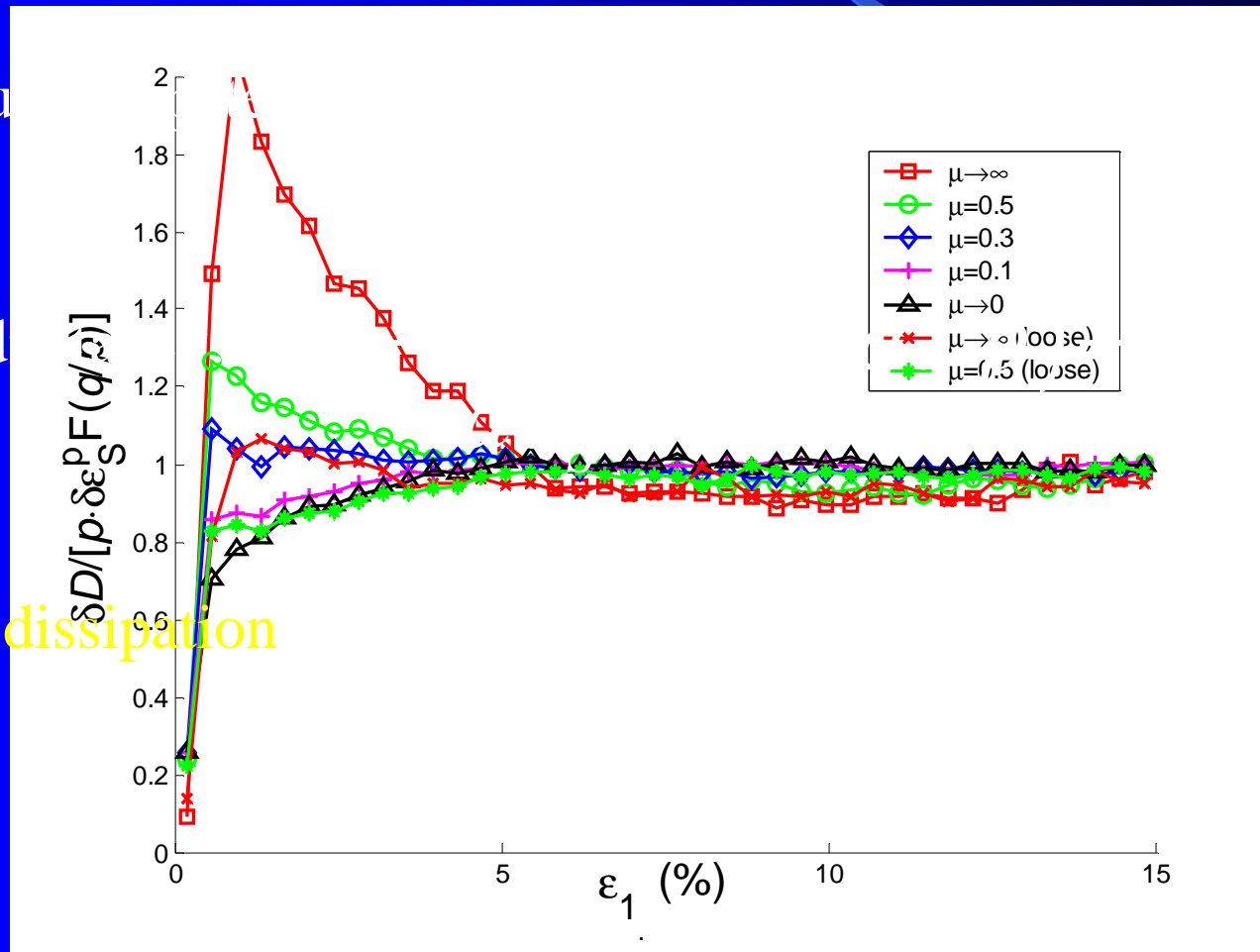


Dissipation function

Work input

Strength-d

Resulting dissipation function:



$p)_{\infty}$

Conclusions

- For all μ , frictional behaviour at macro-level
- Macro-level dissipation, even for $\mu \rightarrow 0$ and $\mu \rightarrow \infty$
- Strength-dilatancy relation
- Constant ratio of 'tangential' over 'normal' energy beyond initial range
- All work input is dissipated beyond initial range

Discussion

- Origin of macroscopic frictional behaviour:
 - Interparticle friction: NO
 - Contact disruption and creation: POSSIBLY
- Origin of dissipation if $\mu \rightarrow 0$ or $\mu \rightarrow \infty$:
 - Dynamics & restitution coefficient
 - Microscopic restitution coefficient \Rightarrow macroscopic plastic dissipation

Summary

- Slow flows
- Stress and strain
- Frictional nature
- Geometrical anisotropy
- Validity mean-field approximation



Mixing of granular materials in rotating cylinders

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Co-workers

- Gerard Finnie:
 - Mineral Processing Group, University of Witwatersrand, Johannesburg, South Africa
- Mao Ye & Christiaan Zeilstra & Hans Kuipers:
 - Department of Chemical Engineering, University of Twente

Mixing in rotating cylinders



Functions of rotary kilns

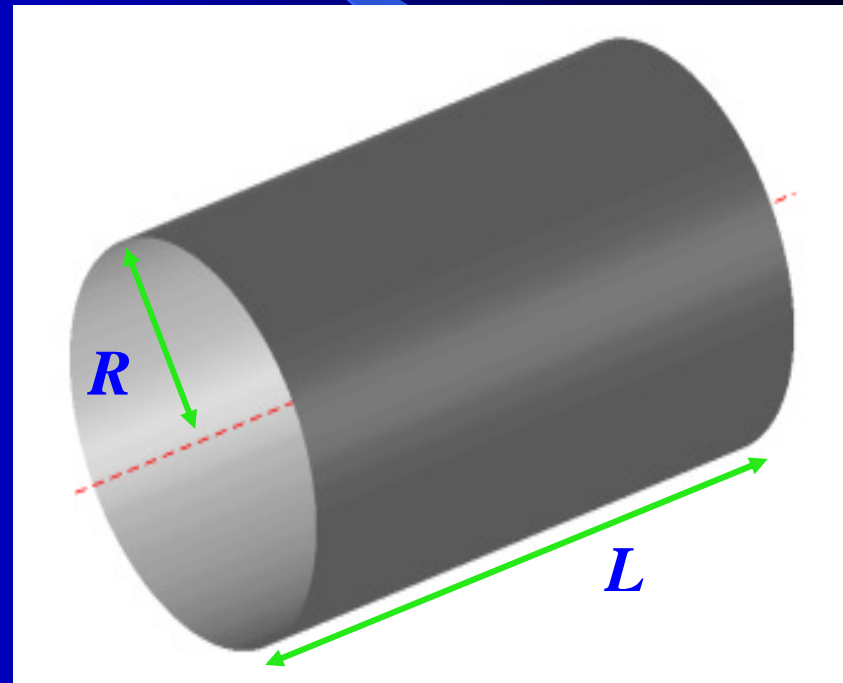
- Mixing
- Calcination
- Drying
- Waste incineration
- ...

Process parameters

- Speed of rotation, Ω
- Radius, R
- Filling degree, J
- Length, L

- Material properties
- Inclination
- Gas flow

- ...



Flow regimes

Increasing rotational speed

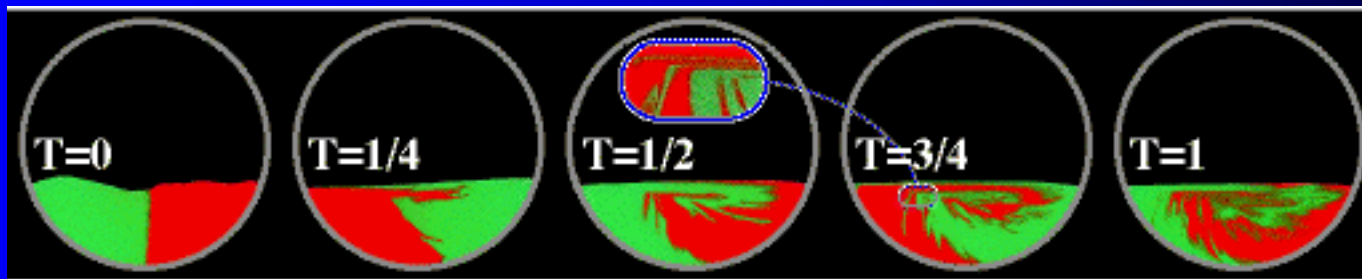


Basic form	Slipping motion		Cascading ("tumbling") motion			Cataracting motion	
Subtype	Sliding	Surging	Slumping	Rolling	Cascading	Cataracting	Centrifuging
Schematic							
Physical process	Slipping		Mixing			Crushing	Centrifuging

From: Mellmann, Powder Technology (2001)

Mixing in rotary kilns

- Transverse → fast
- Longitudinal → slow
- Fascinating patterns



From: Shinbrot et al., Nature (1999)

Segregation

- Separation due to differences in:
 - Size
 - Density
- Transverse & longitudinal segregation
- Here *no* segregation:
 - Equal densities
 - Small size differences

Dependence of mixing on process parameters

- Non-dimensional parameters

- Froude number $Fr = \frac{\Omega^2 R}{g}$

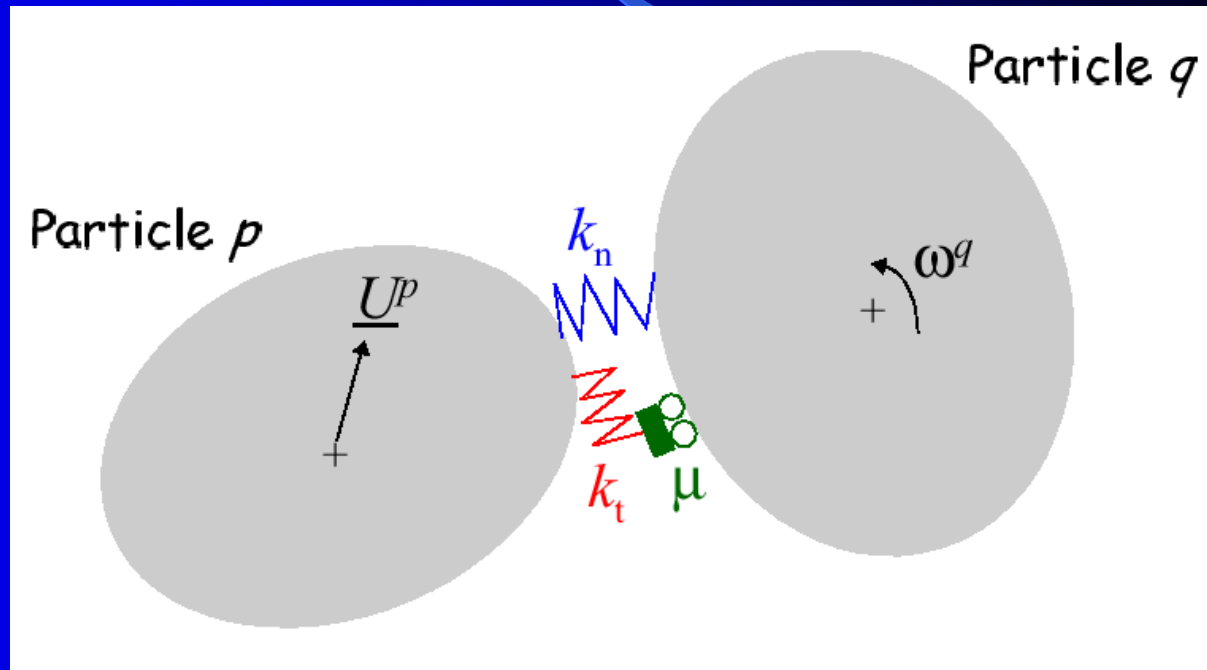
- Filling degree J

Approach: Discrete Element Method

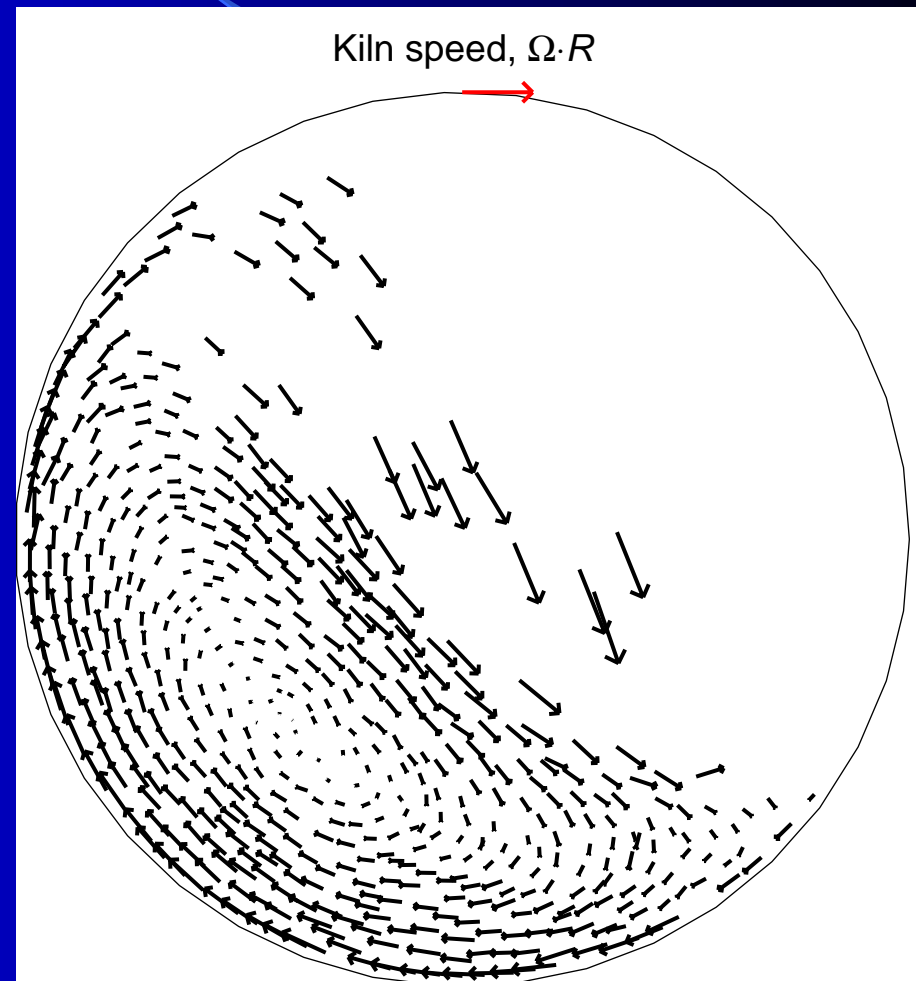
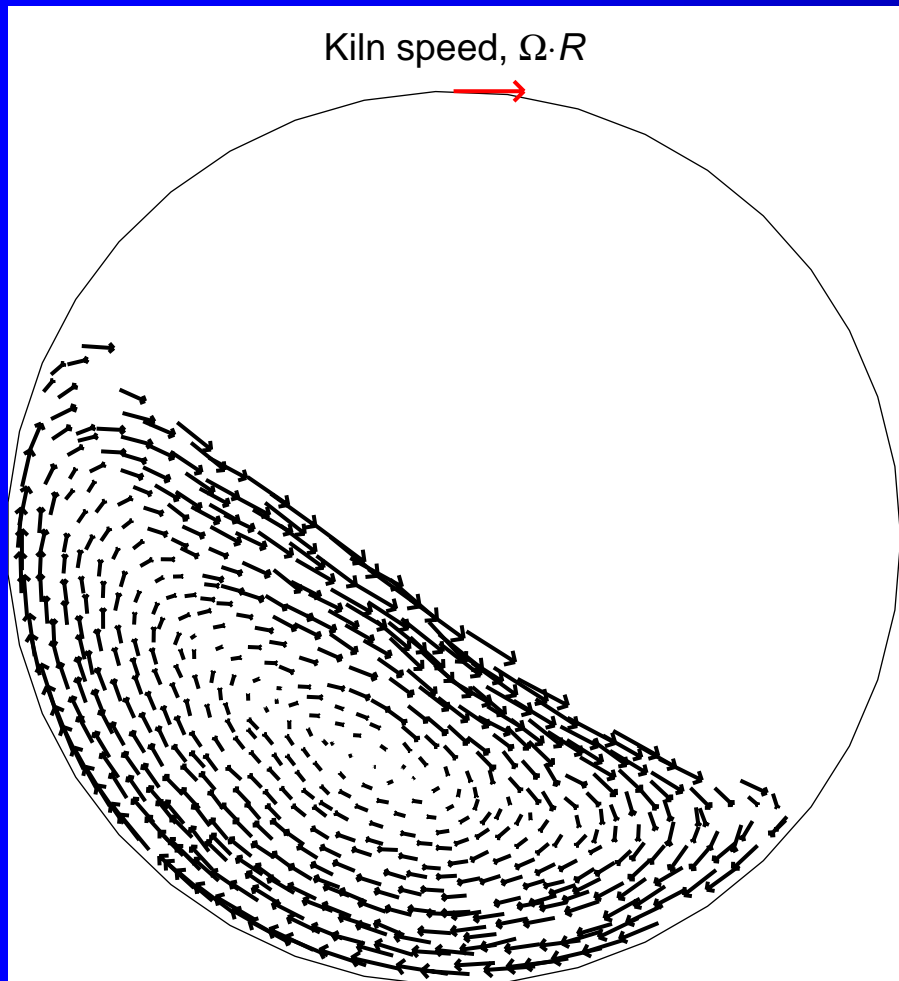
- Many-particle simulation method
- Numerics: explicit time-stepping of equations of motion
 - displacements
 - rotations
- simple models at micro level → complex behaviour at macro level

Contact constitutive relation

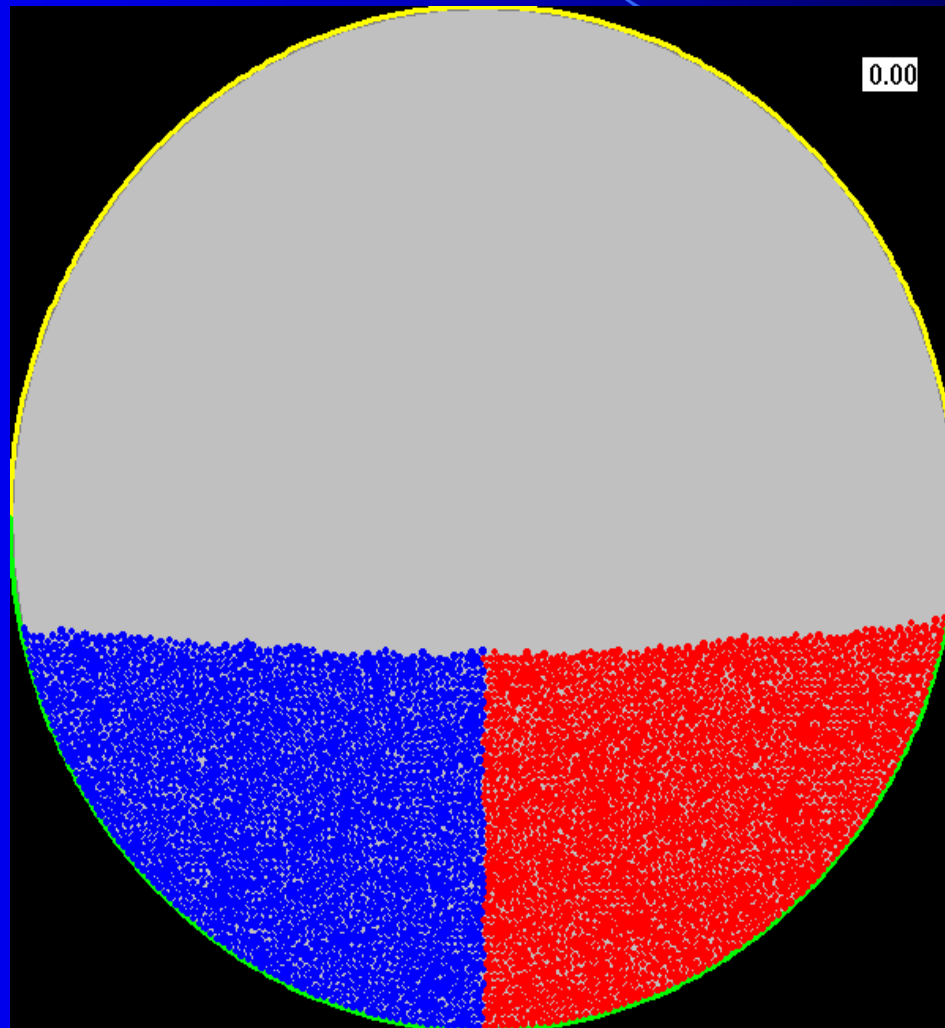
- Elastic
- Frictional
- Damping



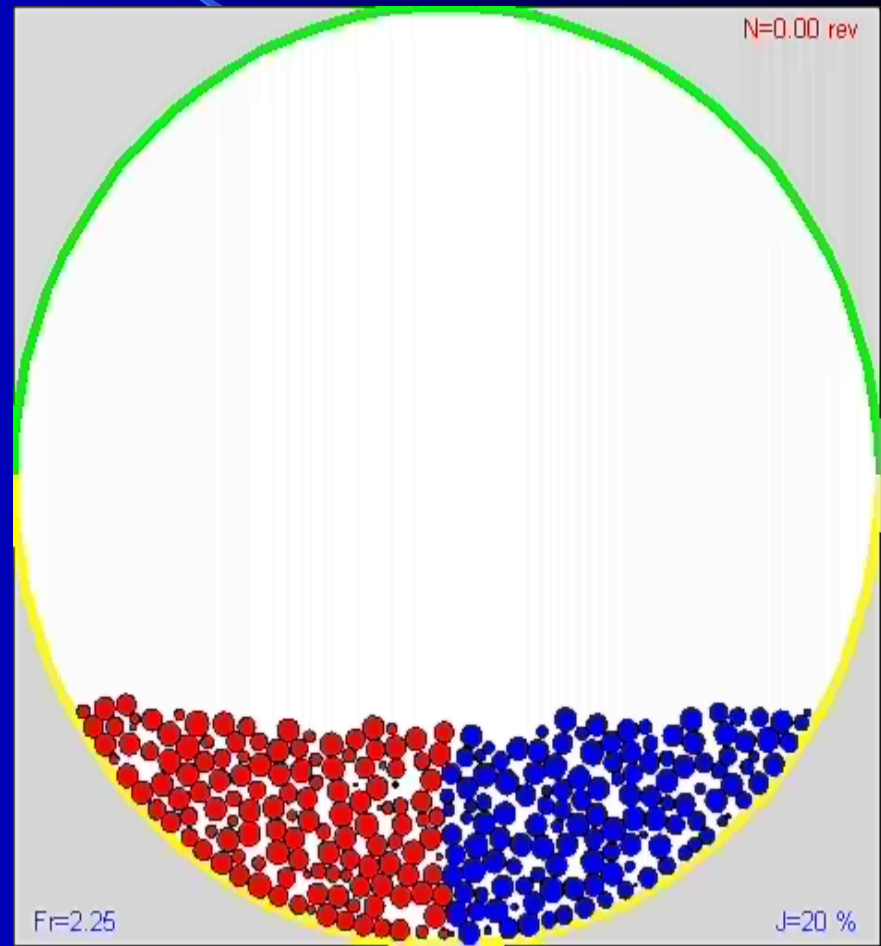
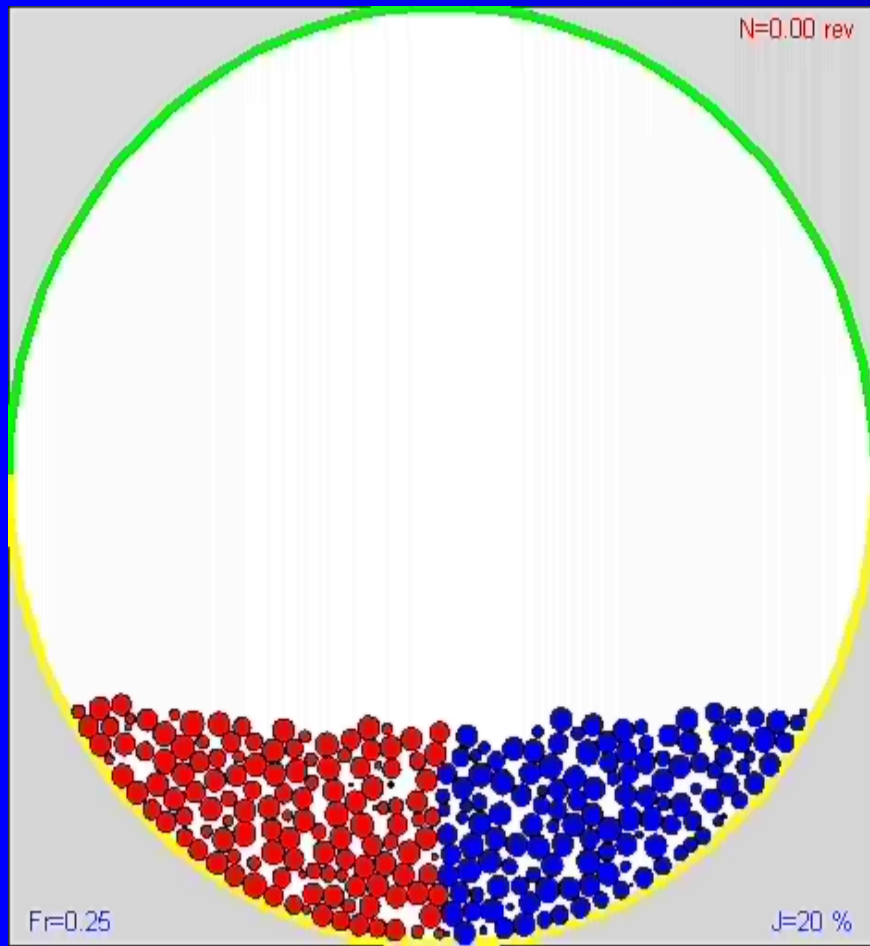
Velocities



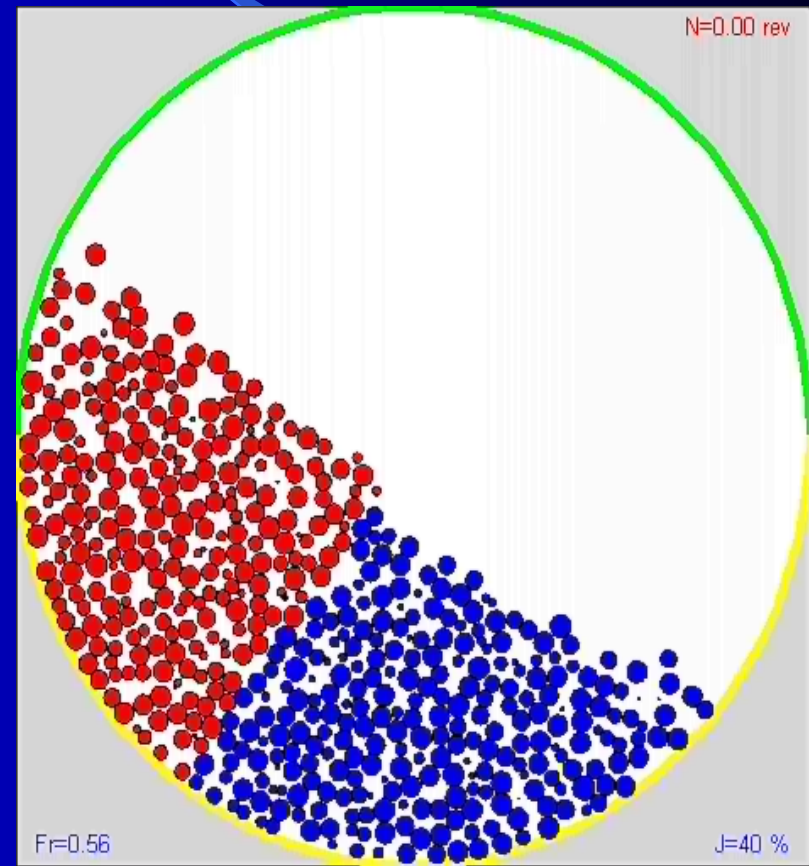
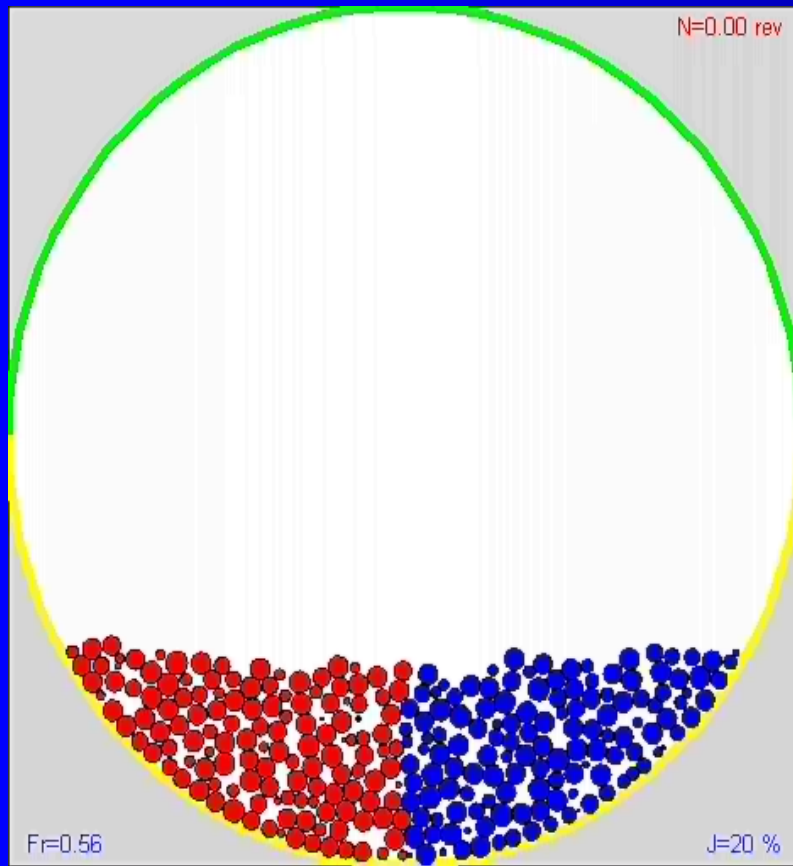
Visualization: 2D



Visualizations: effect of Fr



Visualizations: effect of J



Longitudinal mixing

- Diffusion process; no throughflow

$$\frac{\partial c}{\partial n} = D \frac{\partial^2 c}{\partial x^2}$$

$$\frac{\partial c}{\partial t} = D^* \frac{\partial^2 c}{\partial x^2}$$

$$D^* = \frac{D\Omega}{2\pi}$$

1 Solution

$$c(x, n) = \frac{1}{2} + \sum_{j=1}^{\infty} \frac{1}{2j-1} \exp\left(-\frac{(2j-1)^2 \pi^2 D n}{L^2}\right) \sin \frac{(2j-1)\pi n}{L}$$

Determination of diffusion coefficient (1)

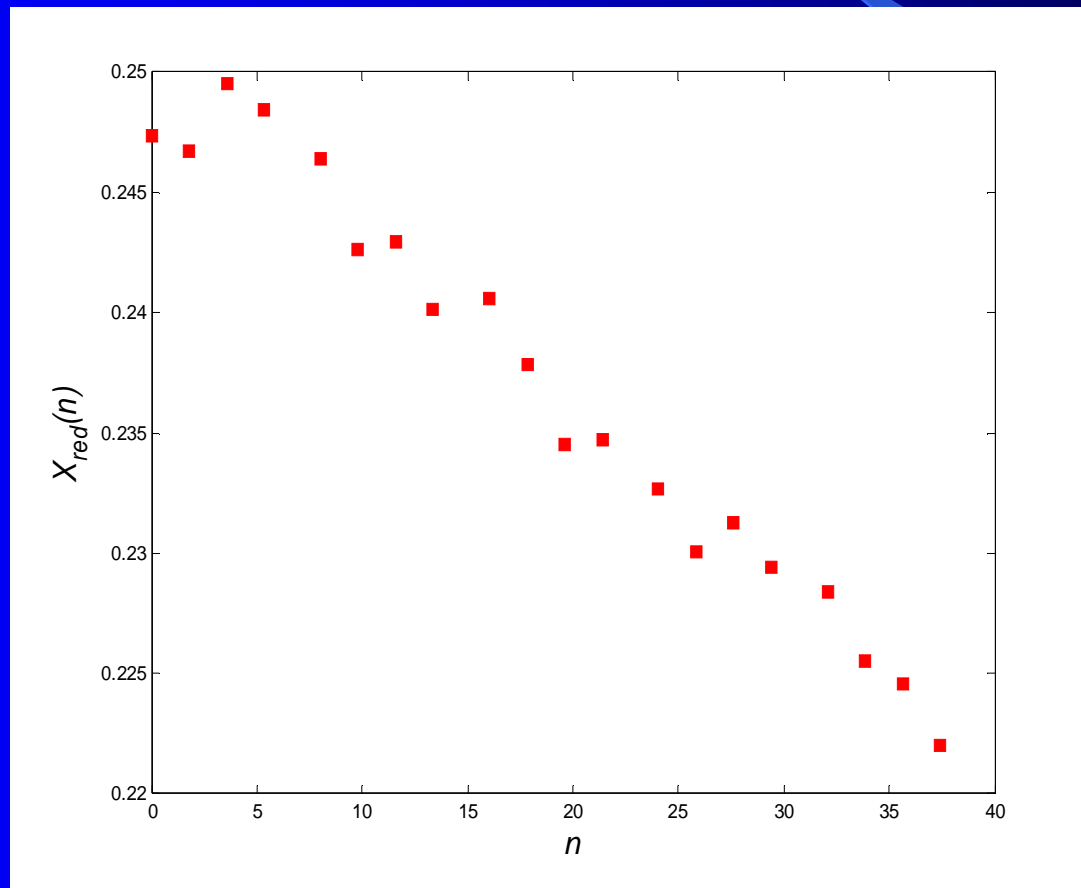
- Mean position of “red” particles

$$X_R(n) = \frac{1}{L} \int_{-L/2}^{+L/2} xc(x, n) dx$$

- 1 For small “Fourier” number

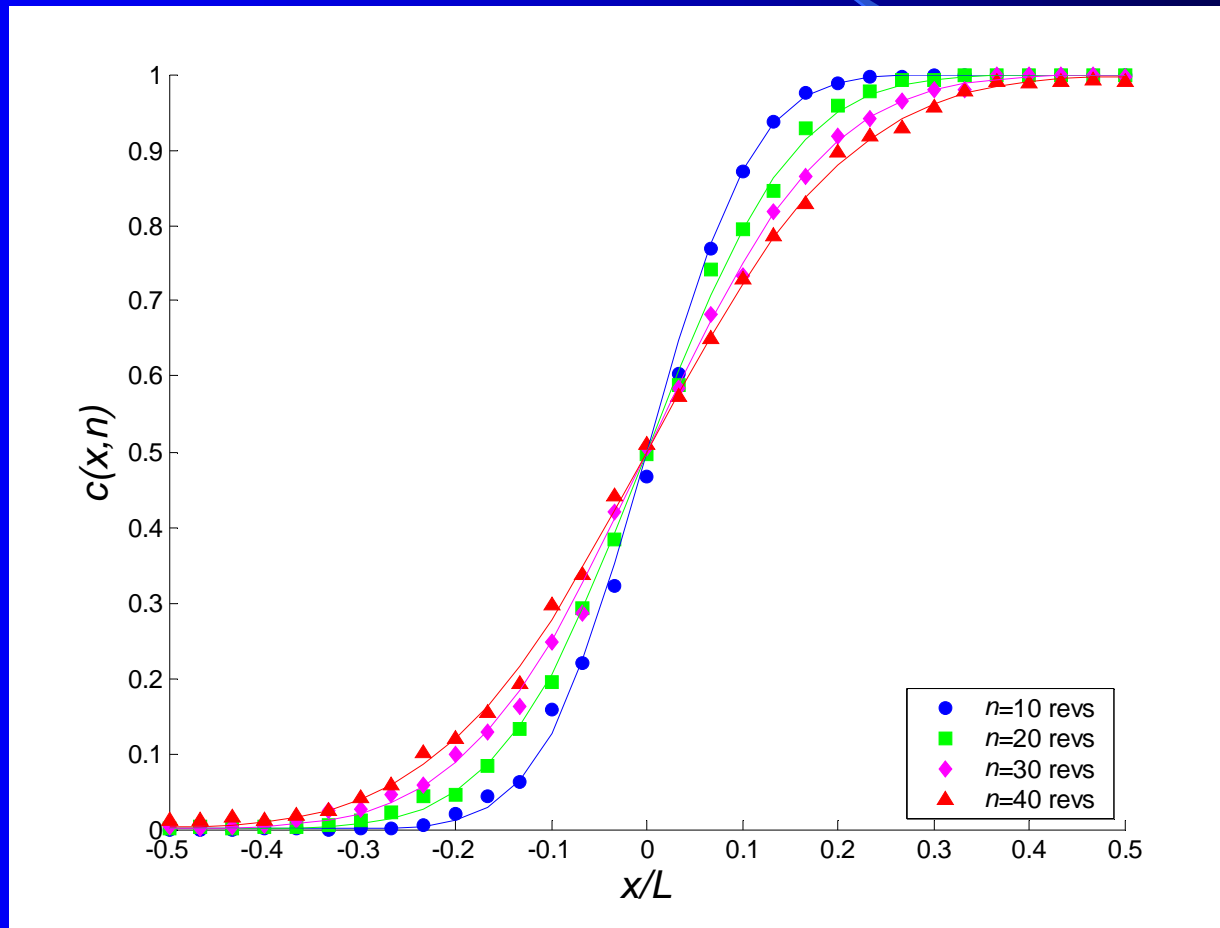
$$X_R(n) \cong \frac{1}{4} - 2 \left(\frac{Dn}{L^2} \right)$$

Determination of diffusion coefficient (2)

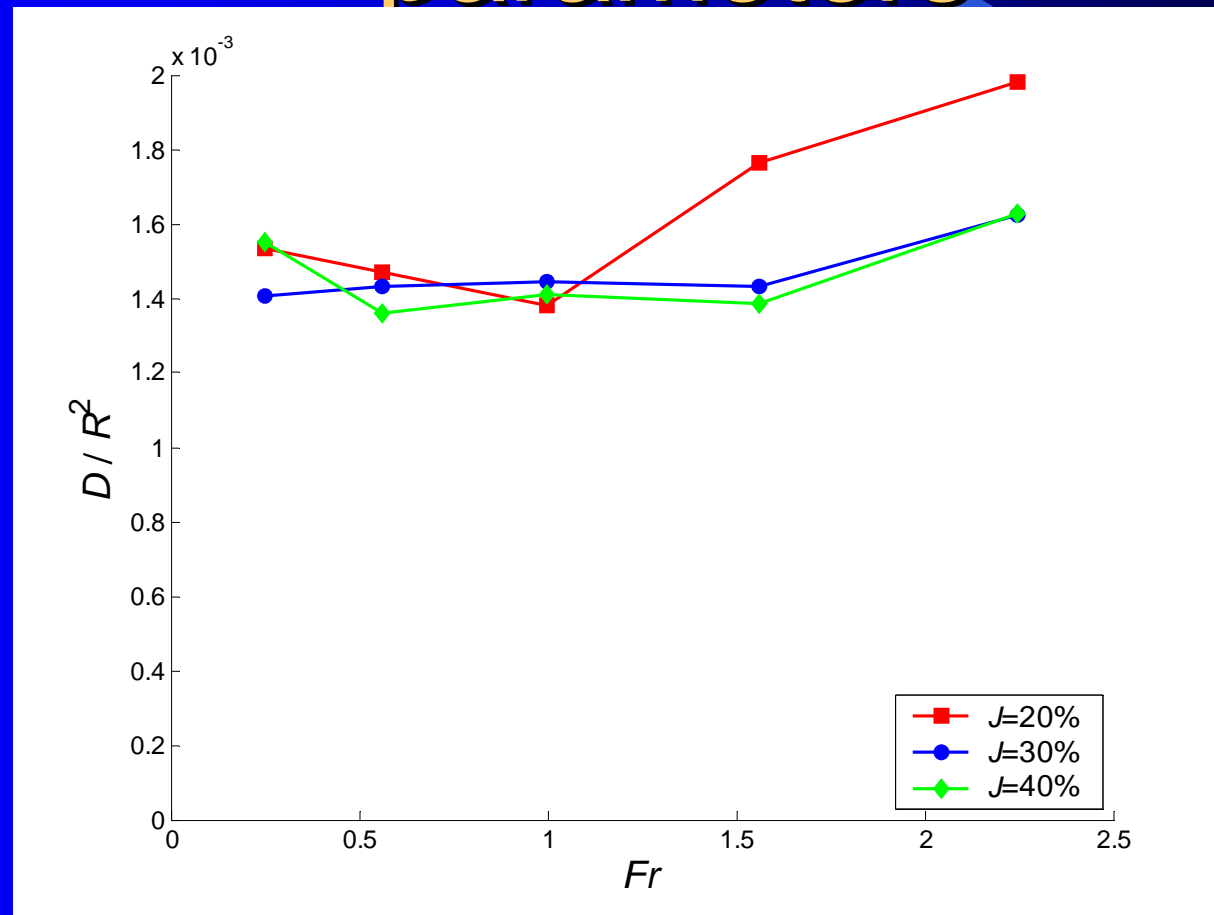


Linear relation is indeed observed!

Concentration profiles



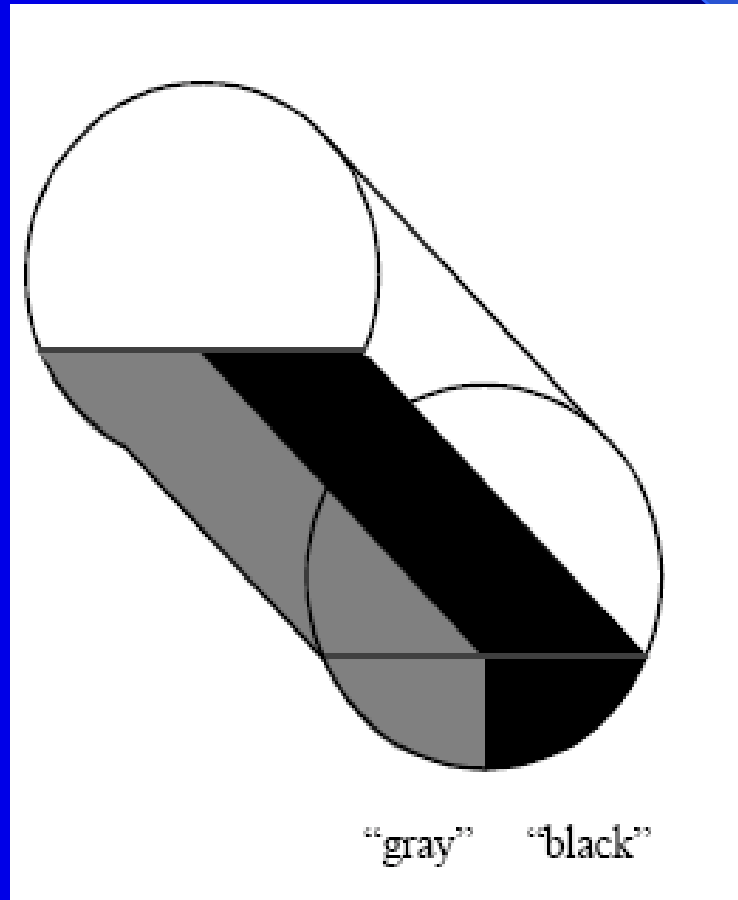
Dependence of diffusion coefficient on process parameters



Comparison with other studies

- Present $D^* \propto \Omega^{1.0}$ $D = \text{const}$
- Dury & Ristow (1999) $D^* \propto \Omega^{2.0}$ $D^* = \frac{D\Omega}{2\pi}$
- Rao et al. (1991) $D^* \propto \Omega^{1.0}$
- Rutgers (1965) $D^* \propto \Omega^{0.5}$
- Sheritt et al. (2003) $D^* \propto \Omega^{0.4}$

Transverse mixing: initial configuration



Transverse mixing

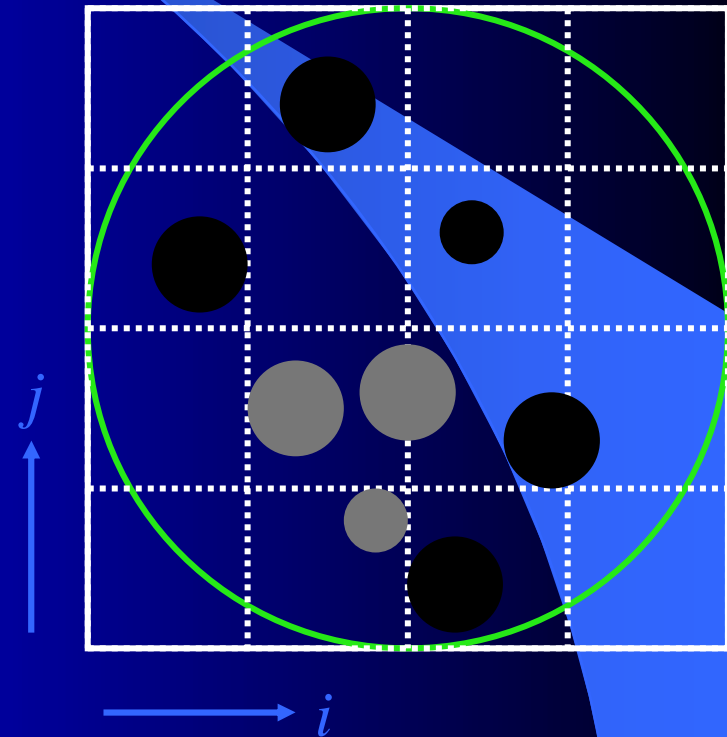
- Entropy-like mixing index

$p_{i,j}$: fraction of "black" particles

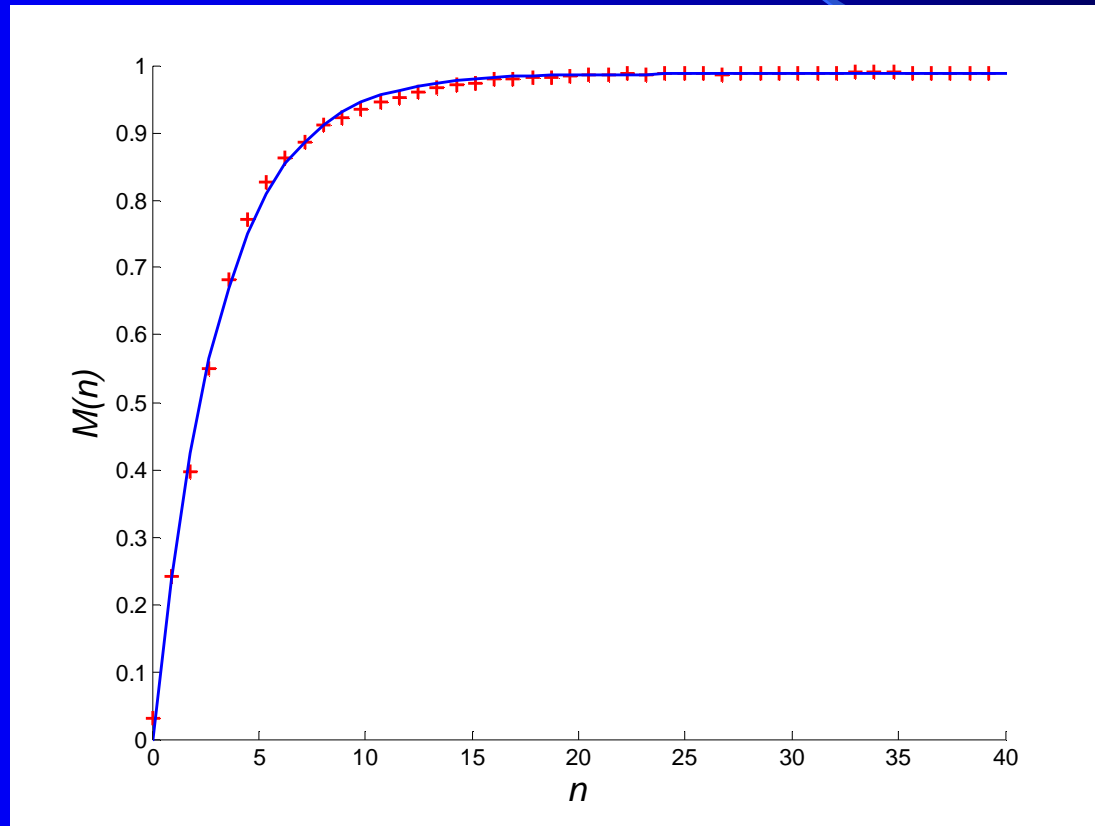
$q_{i,j}$: fraction of "gray" particles

$$I_{i,j} = -kV_{i,j} (p_{i,j} \ln p_{i,j} + q_{i,j} \ln q_{i,j})$$

$$M(n) = \sum_{i,j} \frac{I_{i,j}(n)}{I(n \rightarrow \infty)}$$



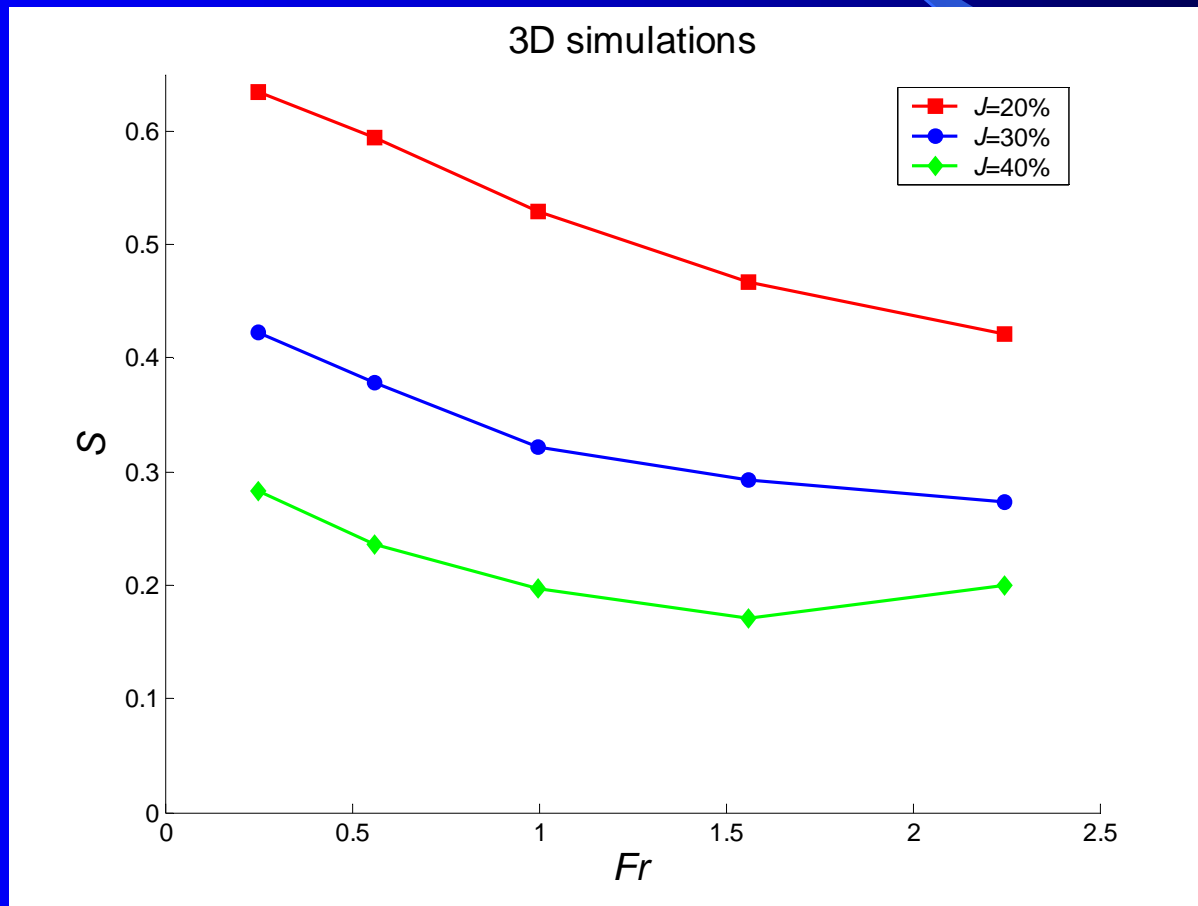
Evolution of mixing index



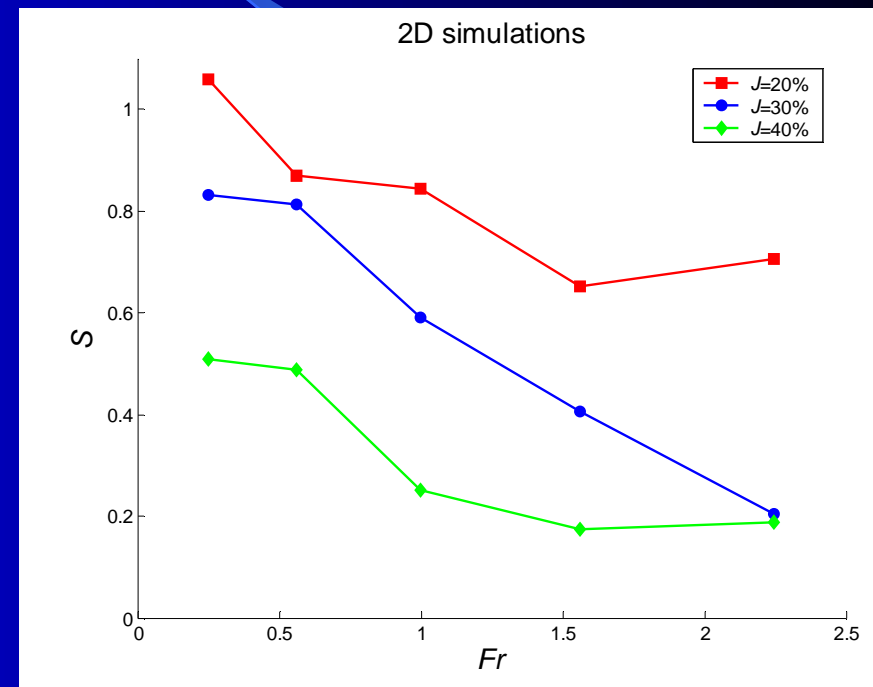
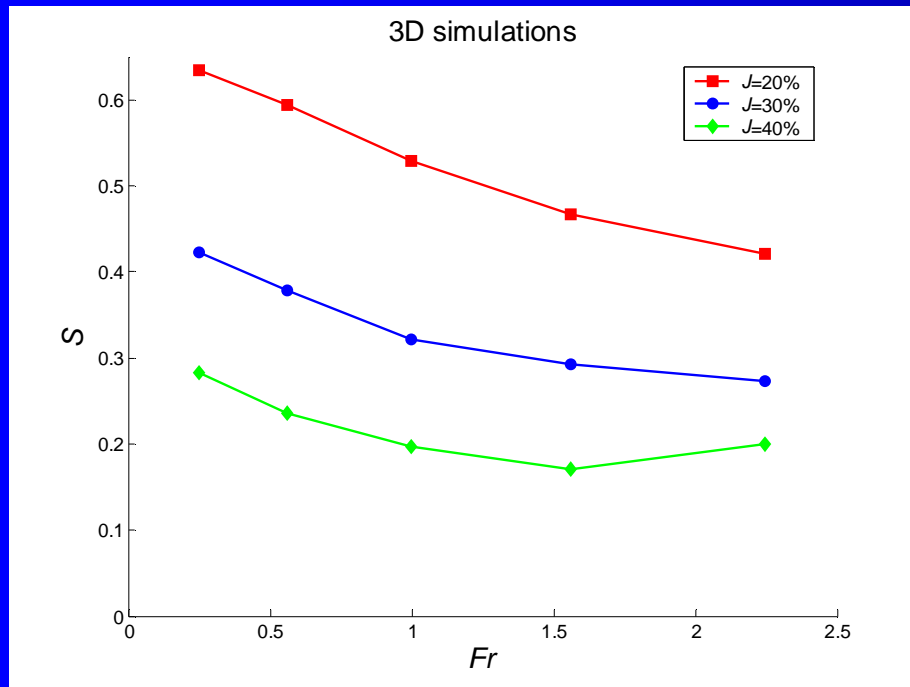
$$M(n) \cong 1 - \exp(-Sn)$$

↑
Mixing speed

Dependence of mixing speed on process parameters



2D vs. 3D simulations



Faster transverse mixing in 2D than in 3D

Conclusions

- Longitudinal mixing
 - Diffusion equation
 - Diffusion coefficient
 - Proportional to rotational speed
 - Weak dependence filling degree
- Transverse mixing
 - Entropy-like mixing index
 - Mixing speed S
 - $\Omega \uparrow: S \downarrow$
 - $J \uparrow: S \downarrow$

Further research

- Effect of particle properties on mixing
- Non-spherical particles
- Inclined rotary kilns
- Velocity profile in active layer
- Inclusion of gas flow
- Axial segregation