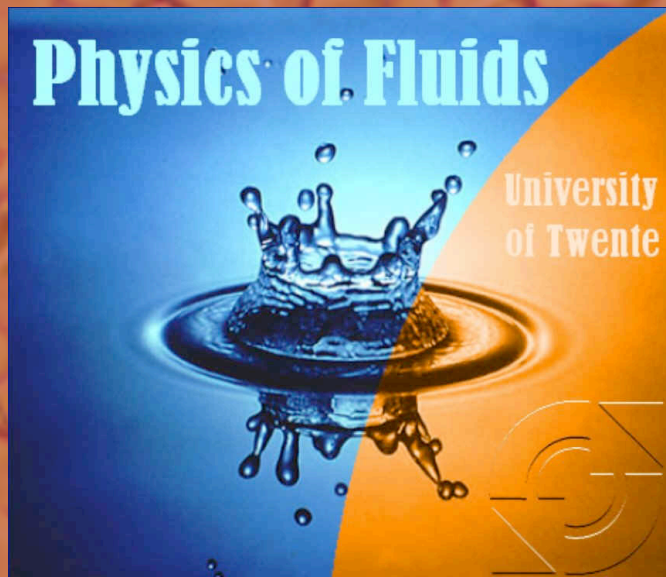


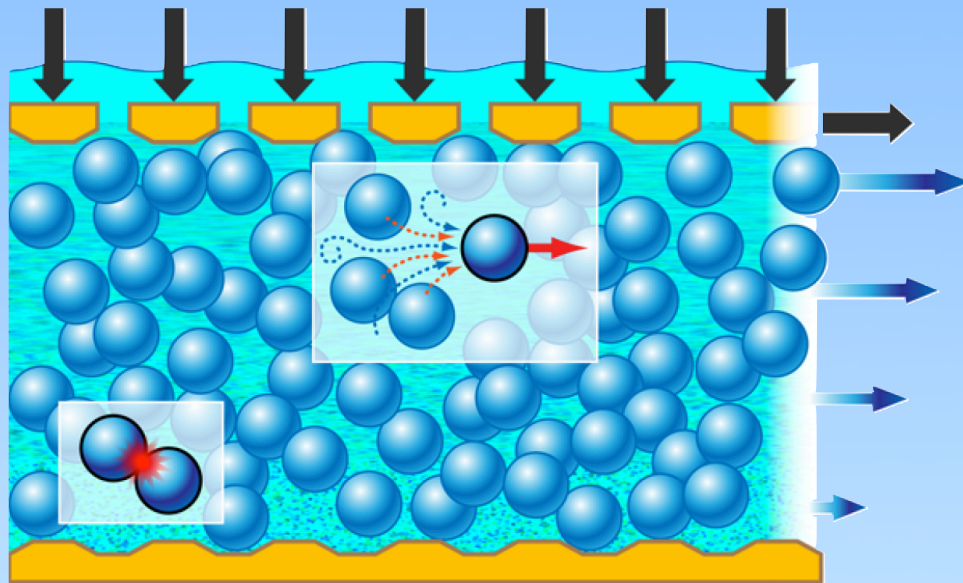
Cornstarch and other suspensions from a different perspective



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Stefan von Kann
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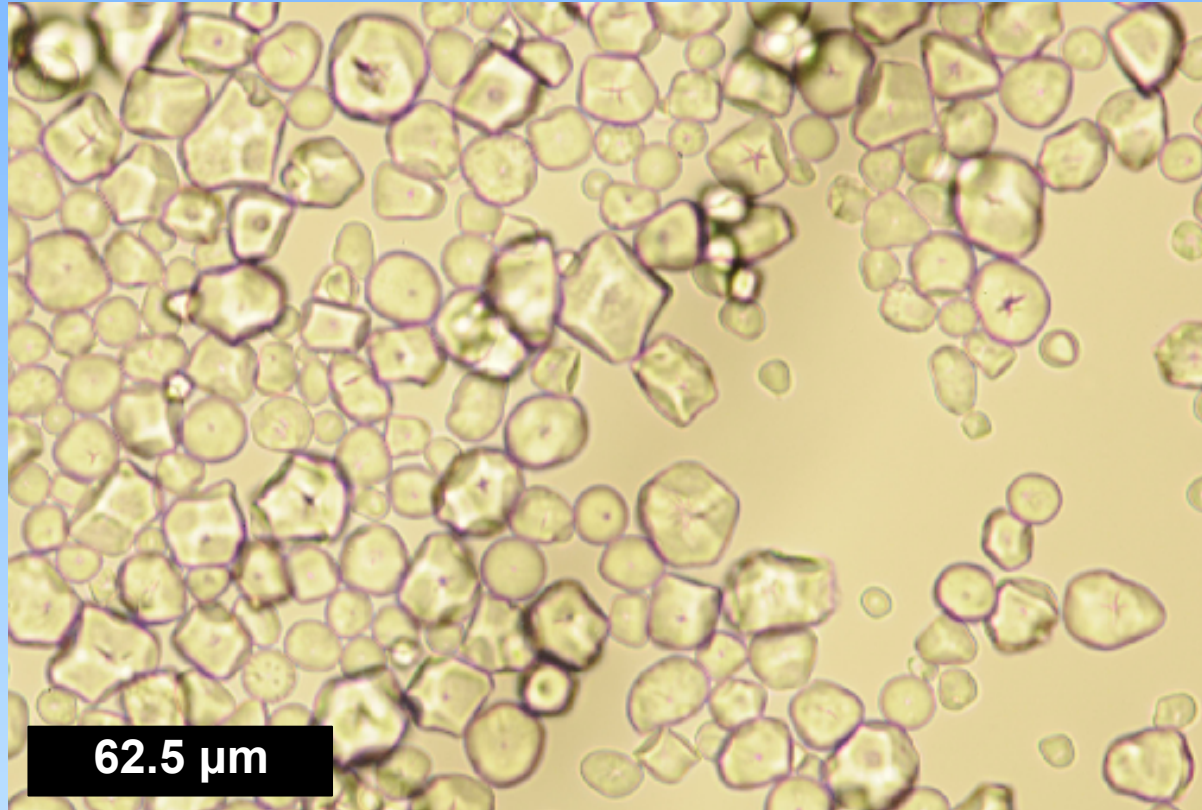
Suspensions: A rheologist's view versus ?



What if we took the same materials for a completely different experiment?

typical rheological experiment:
well defined geometry, with
optimally controlled γ , σ_t , σ_n

Cornstarch

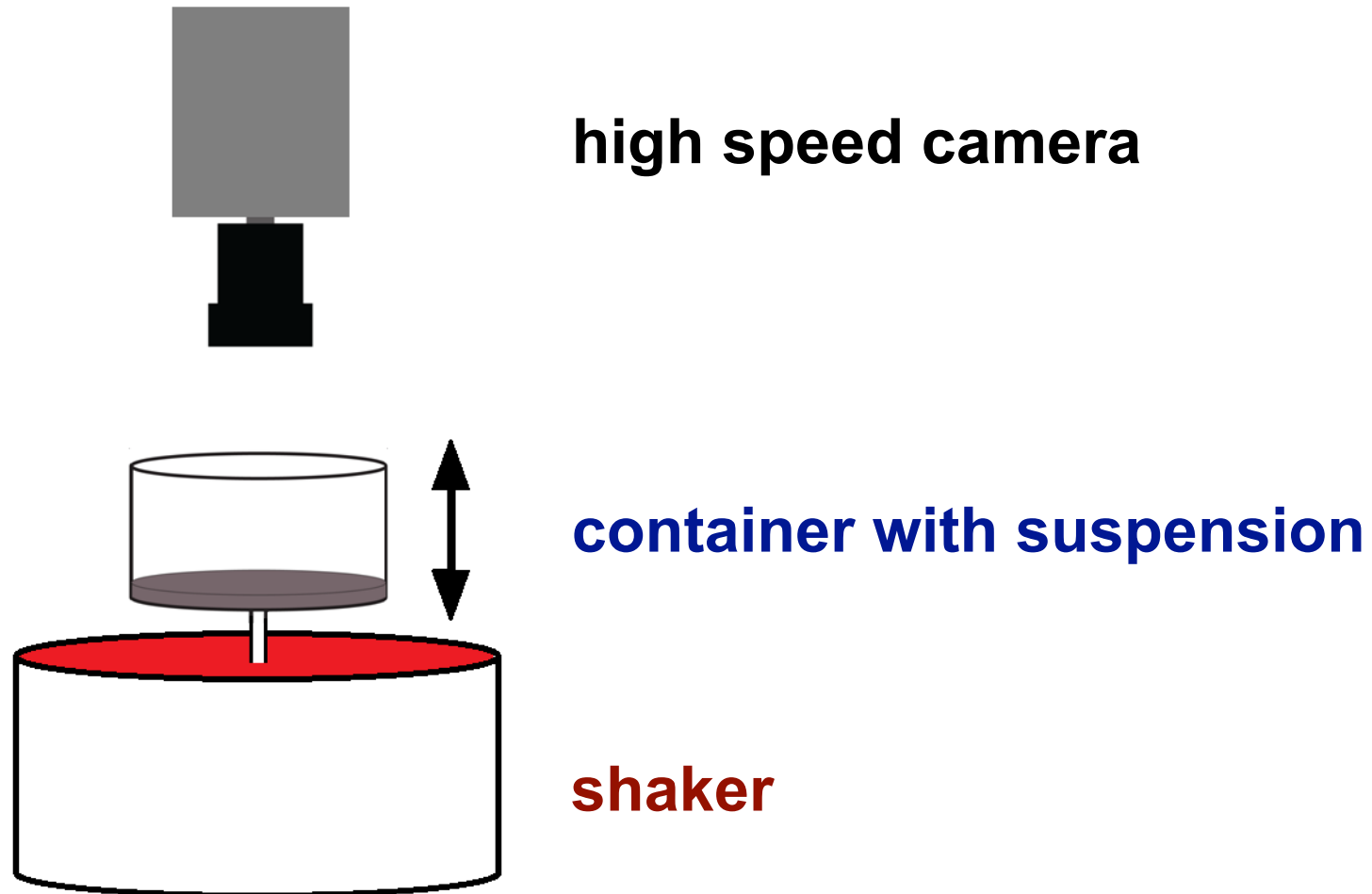


62.5 μm

diameter: 5-20 μm ,
flat distribution of sizes (numbers)
Irregular shapes
 $\rho = 1.5 \text{ g/cm}^3$

“shear thickening suspension”

First experiment



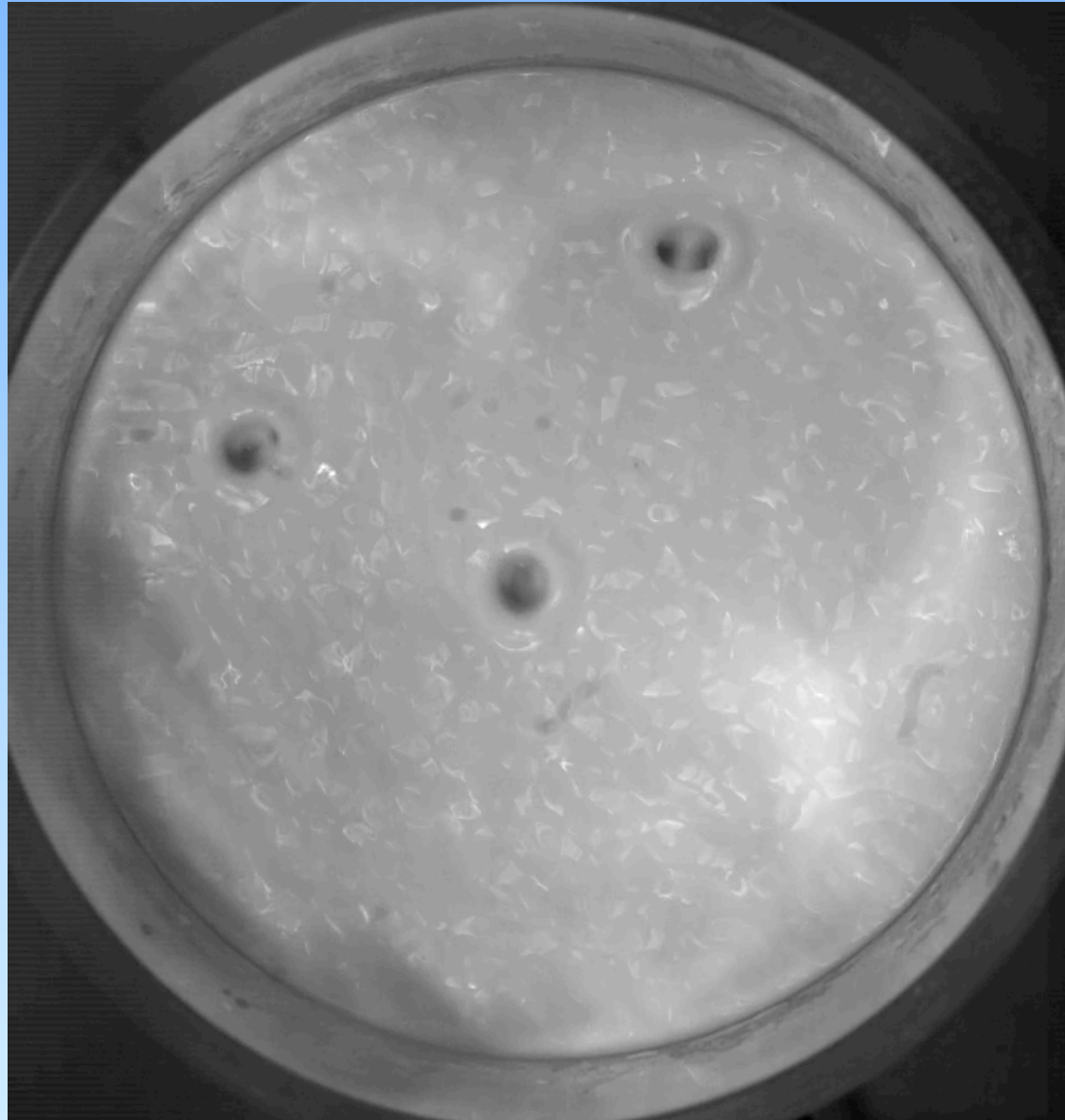
Shaken cornstarch 1



**jumping
liquid**

40 Hz
30 g

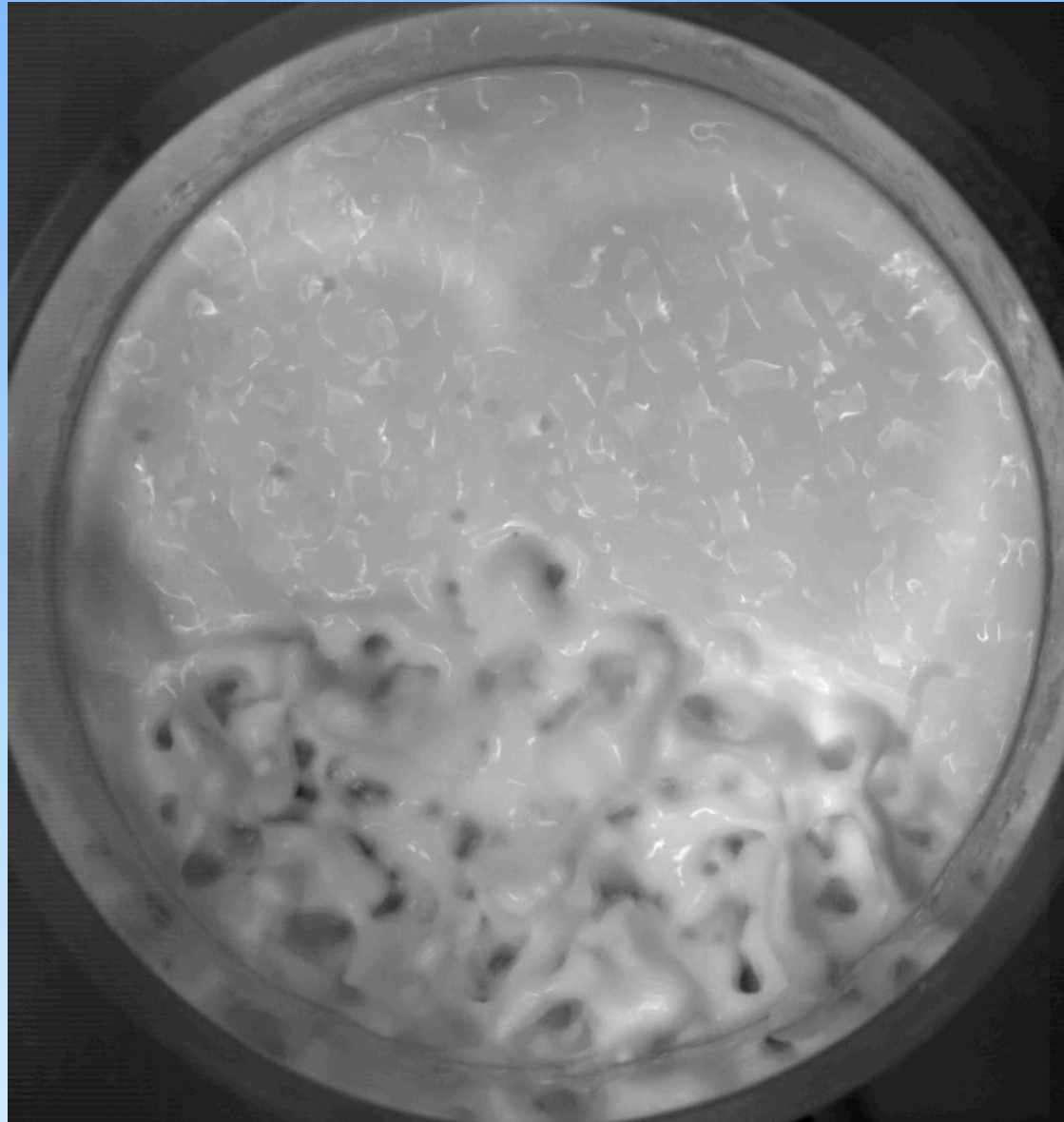
Shaken cornstarch 2



**stable
holes**

80 Hz
20 g

Shaken cornstarch 3

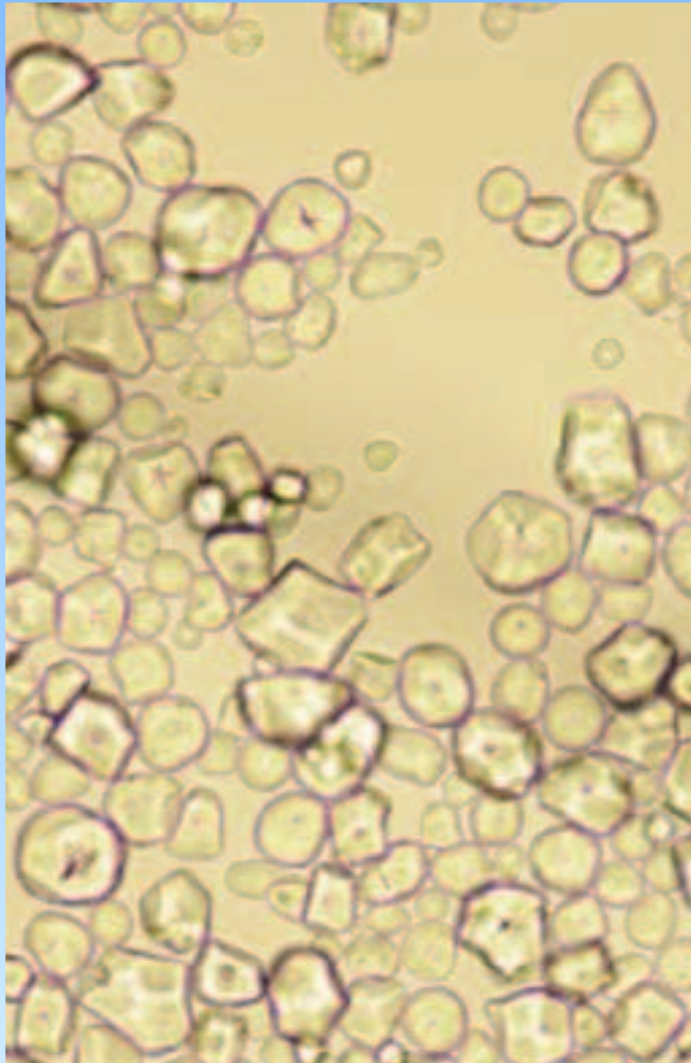


fingers

80 Hz
30 g

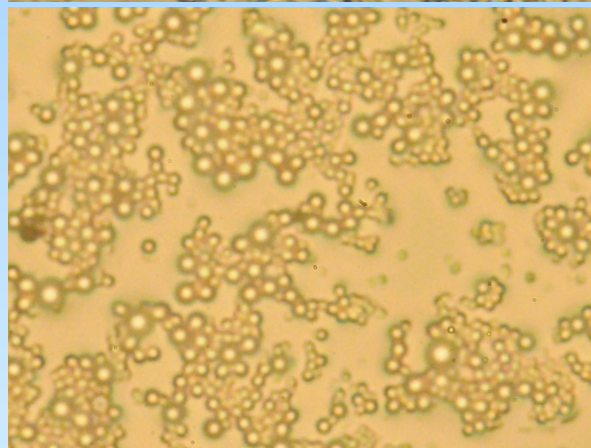
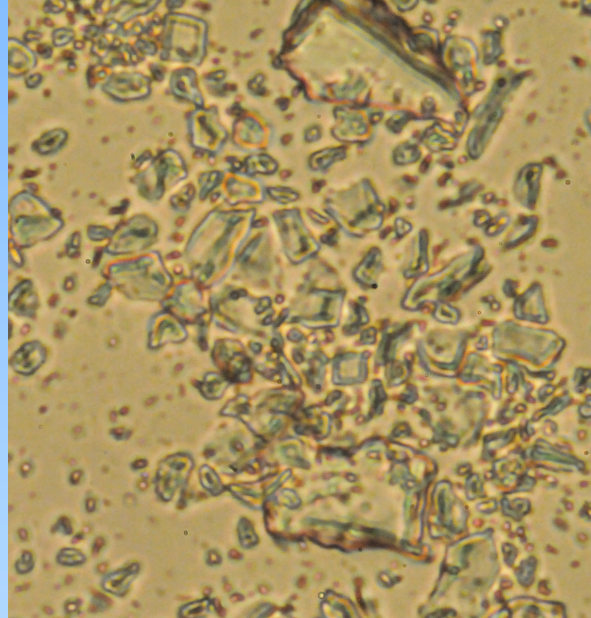
Other suspensions

cornstarch



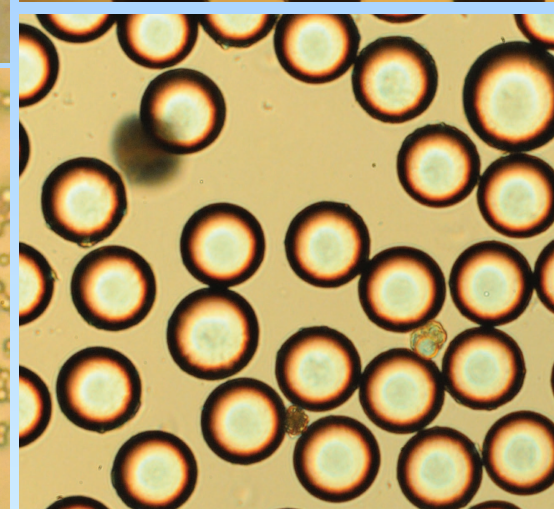
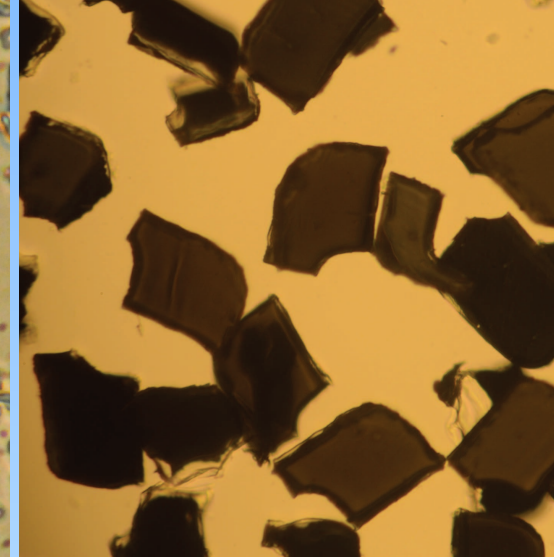
cornstarch

quartz flour



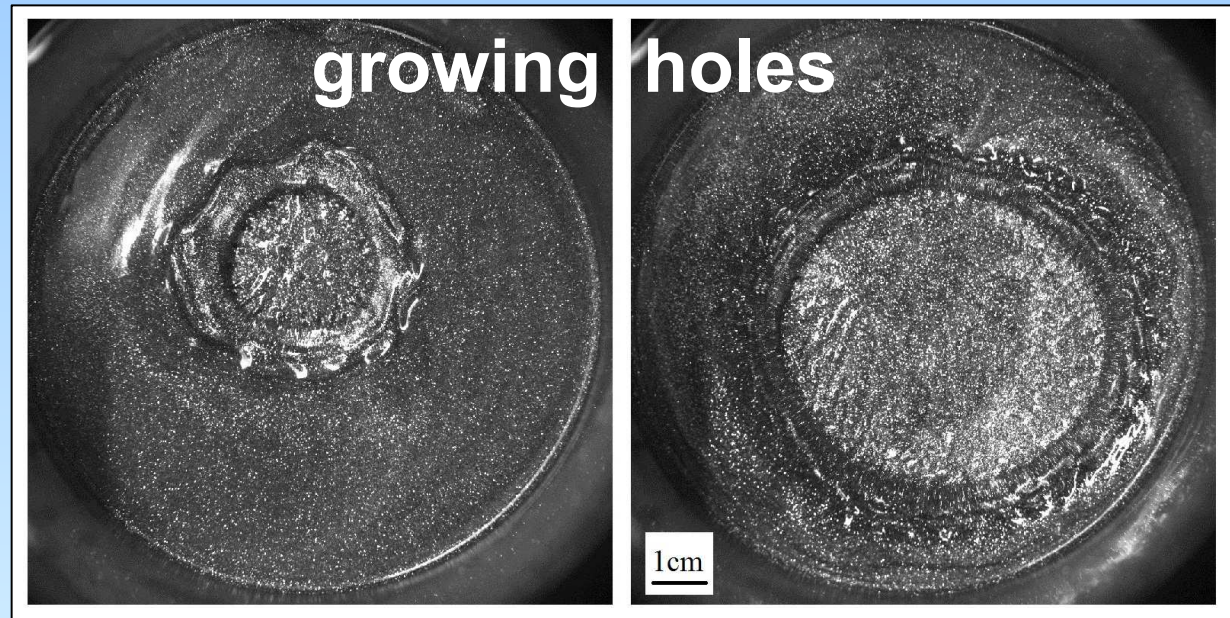
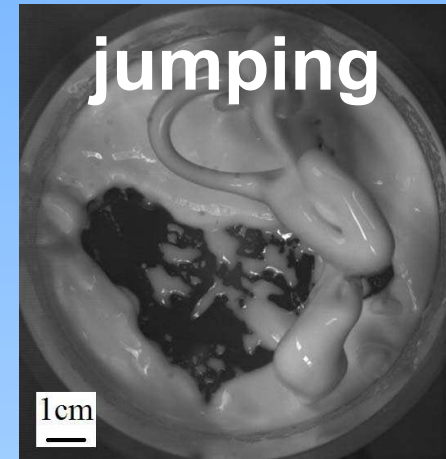
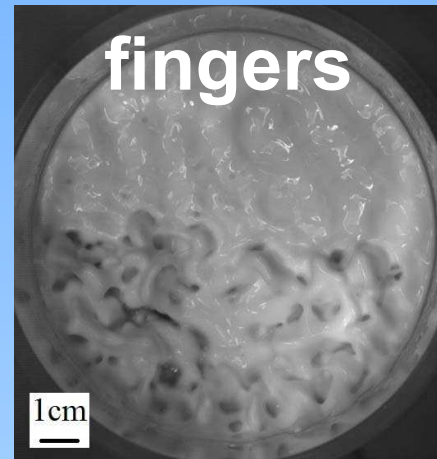
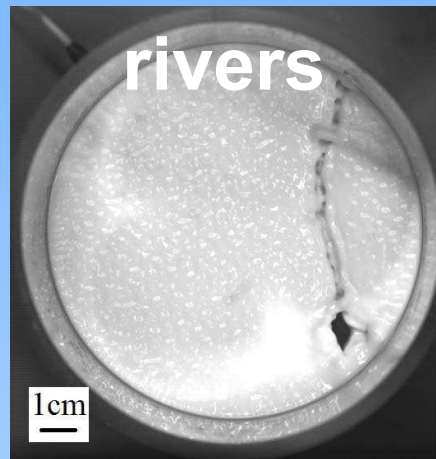
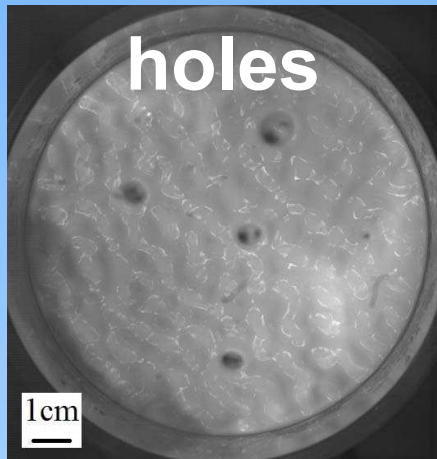
polydisperse silica

glitter platelets



monodisp. silica

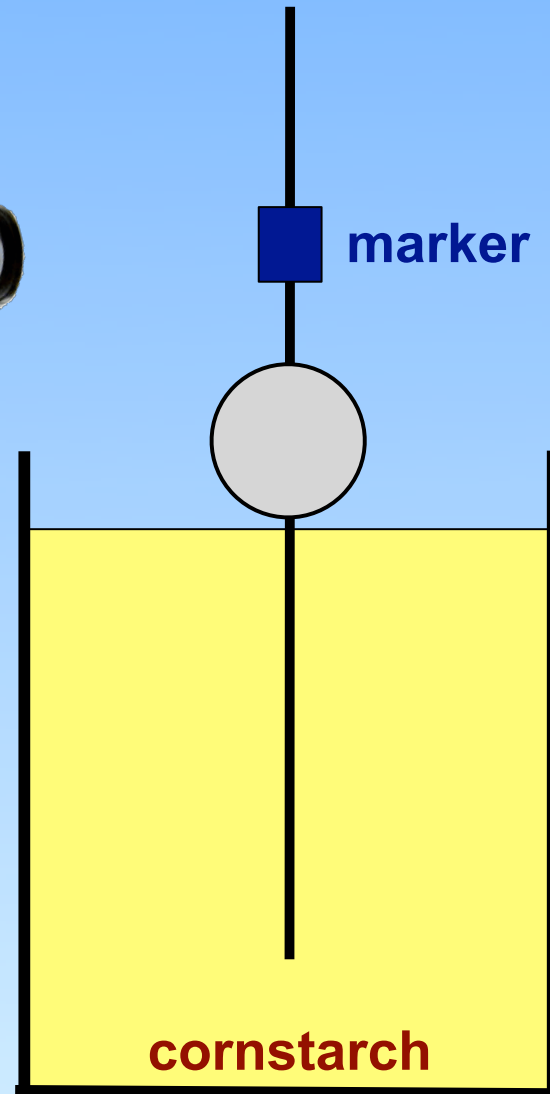
Shaken suspensions



Second experiment



high-speed
camera

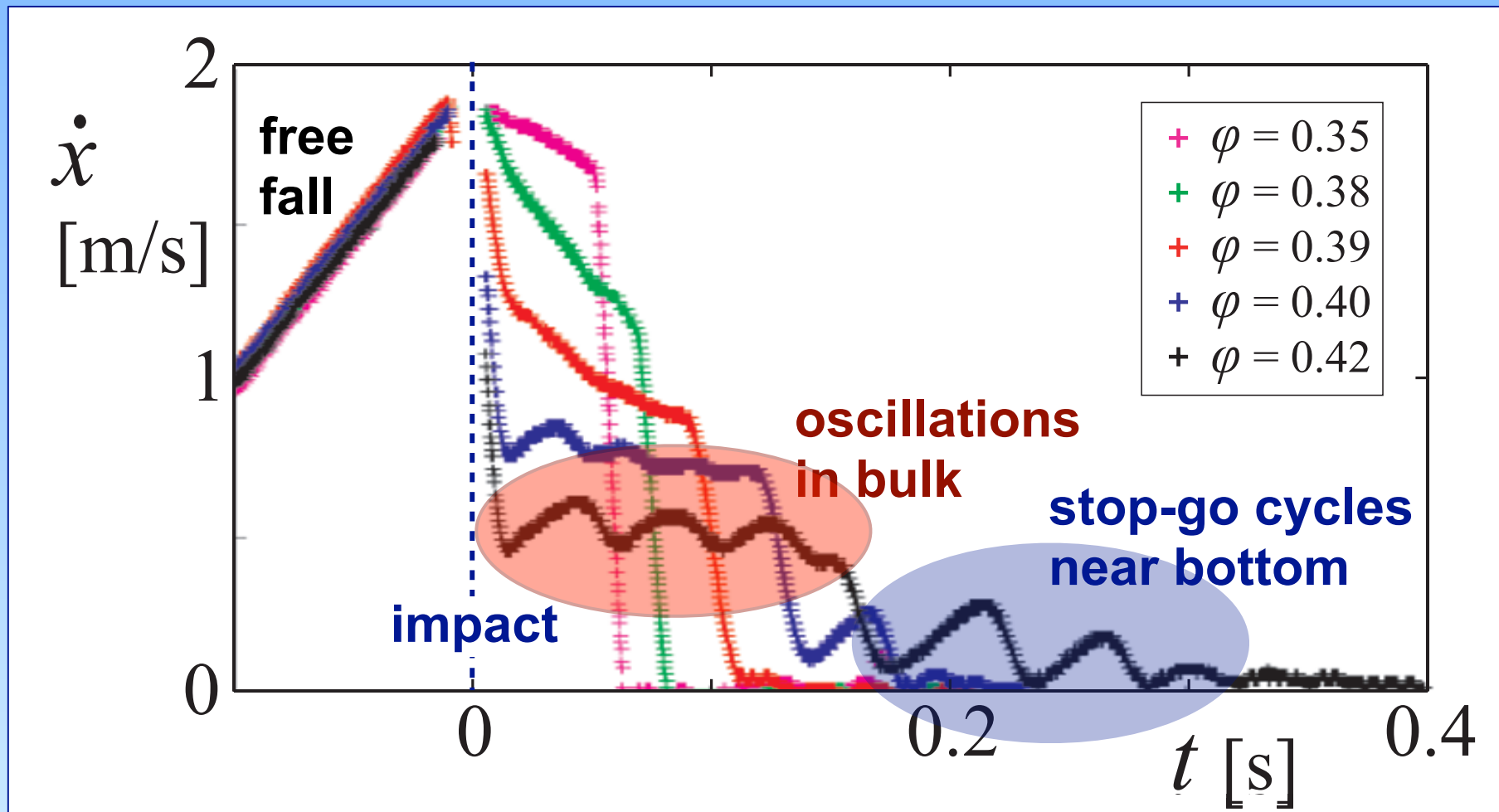


$x(t)$ (depth sphere
inside suspension)

Control parameters:

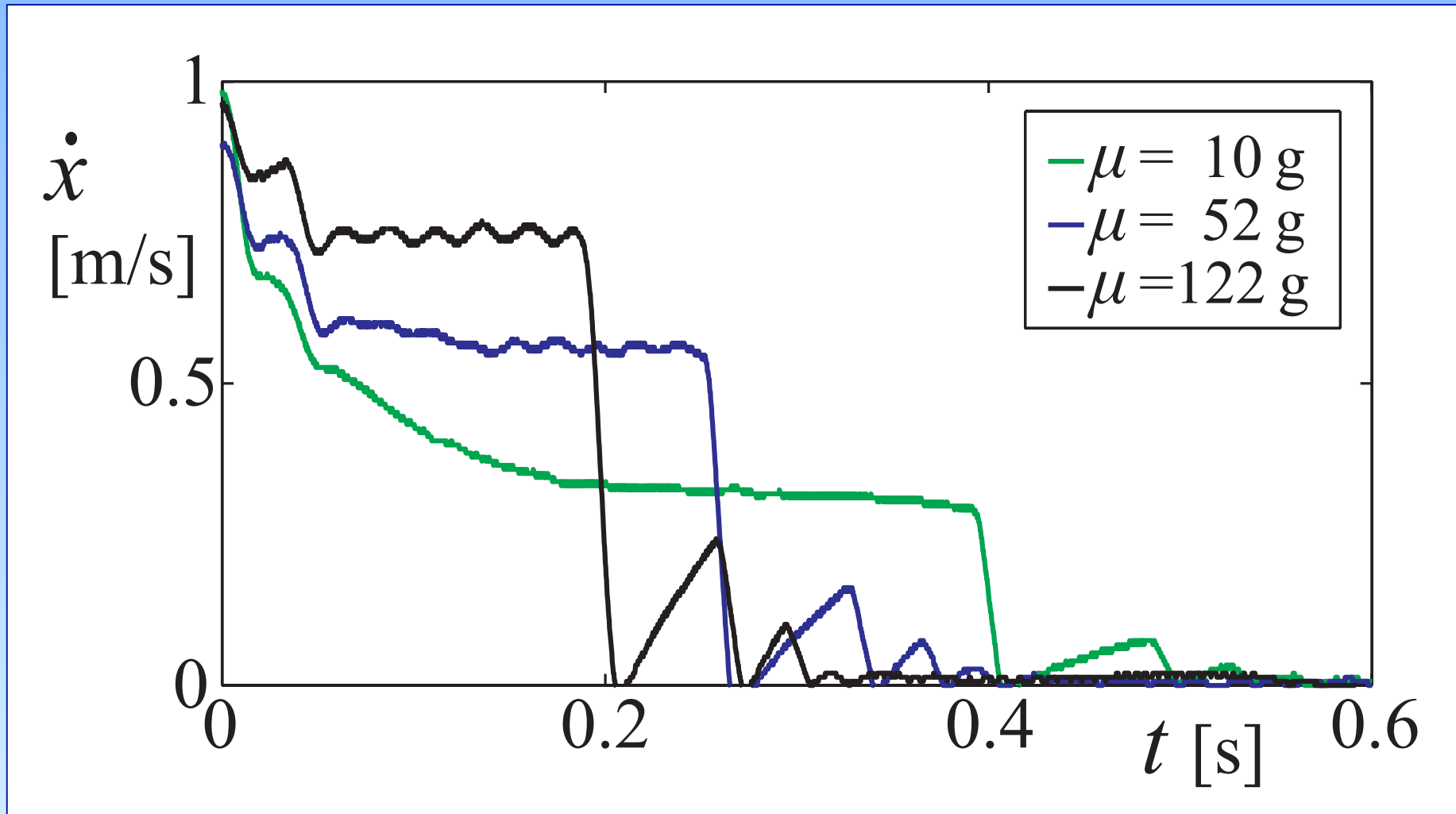
- ▶ packing fraction φ
- ▶ object mass

Increasing packing fraction ϕ



Increasing sphere mass μ

$$\varphi = 0.44$$



Equation of motion

$$m\ddot{x} = \mu g + D$$

Added mass corrected mass:

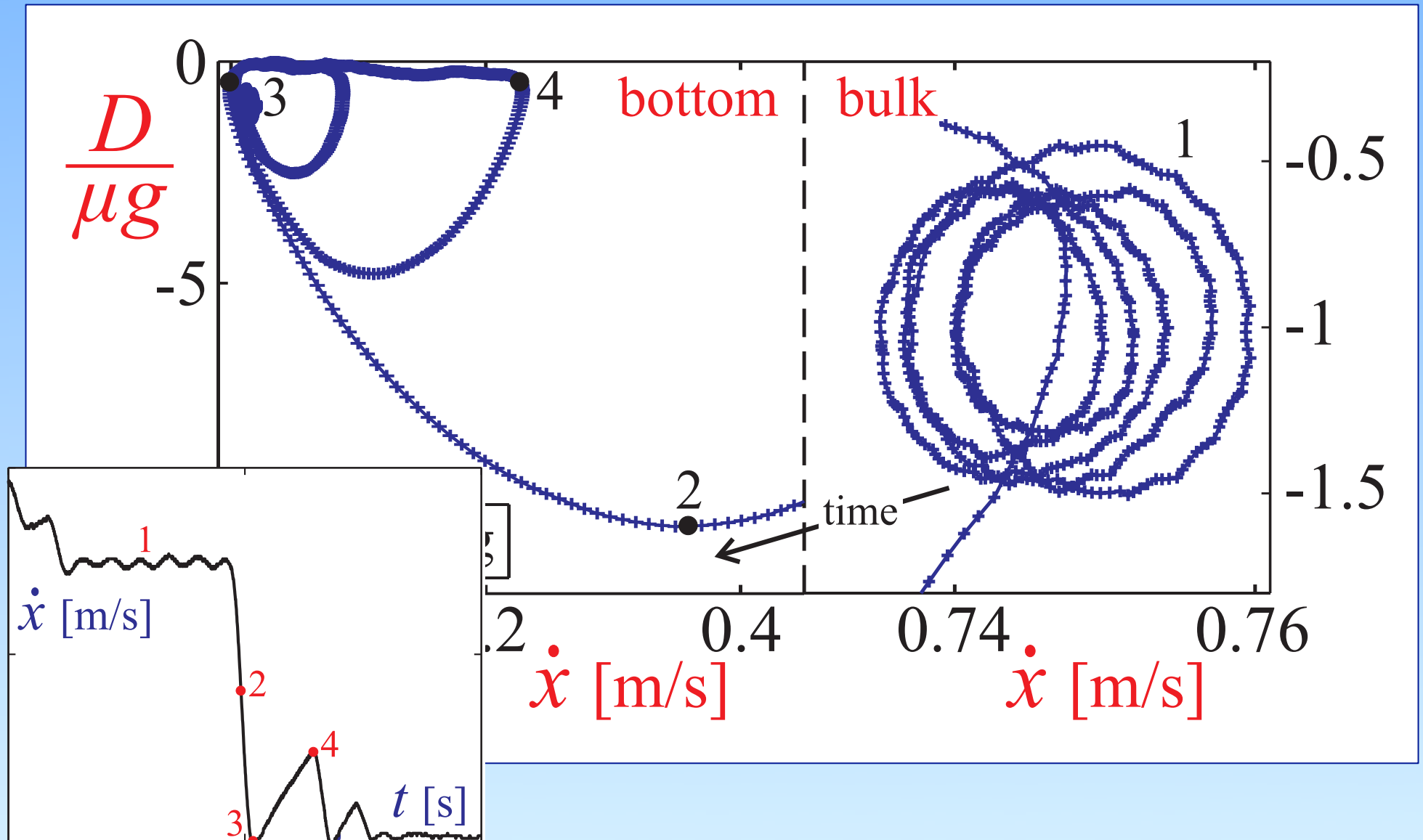
$$m = m_{sphere} + m_{added} = m_{sphere} + \frac{1}{12}\pi d^3 \rho_{susp}$$

Buoyancy corrected mass:

$$\mu = m_{sphere} - m_{buoy} = m_{sphere} - \frac{1}{6}\pi d^3 \rho_{susp}$$

use this equation to calculate drag D vs velocity \dot{x}

Drag D vs velocity \dot{x}



Bulk oscillations

What type of model could describe the bulk oscillations?

Shear thickening or other stress-strain rheology?

No. Leads to monotonic D vs $\dot{\gamma}$ -curve

Visco-elastic liquid models?

No. Leads to damped oscillations

Hysteretic drag model? [R.D. Deegan, *Phys. Rev. E* 81, 036319 (2010).]

Works reasonably well

Modeling bulk oscillations

Hysteretic drag model

Inspired by:

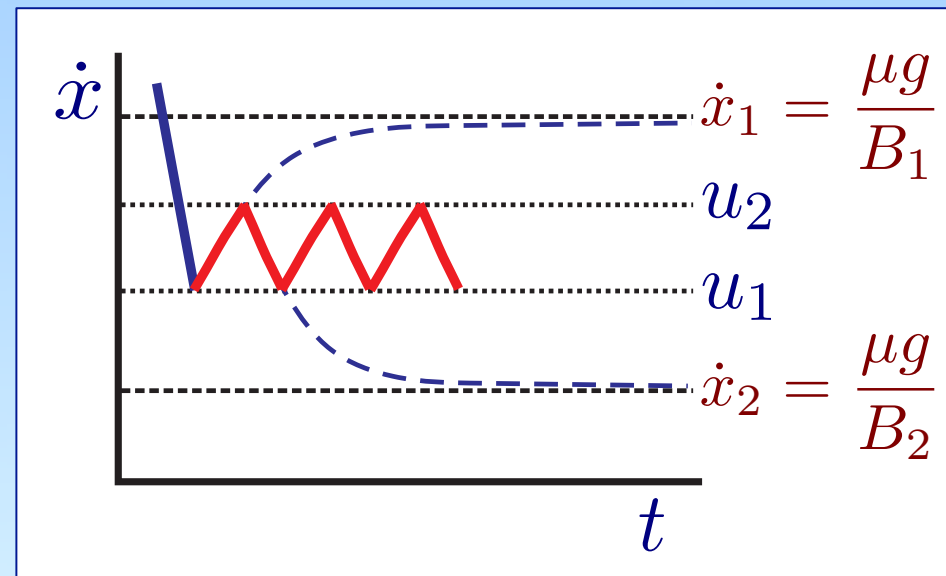
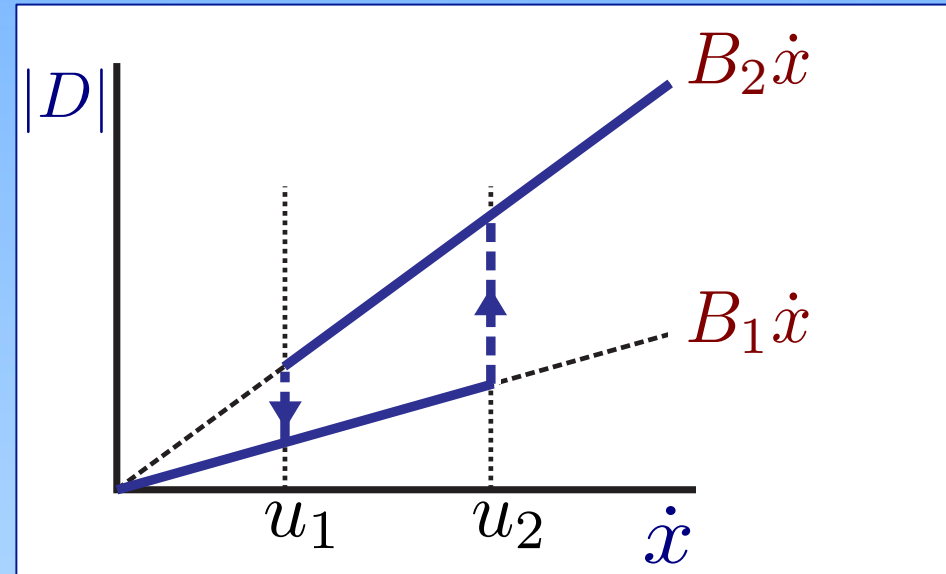
R.D. Deegan,

Phys. Rev. E 81, 036319 (2010).

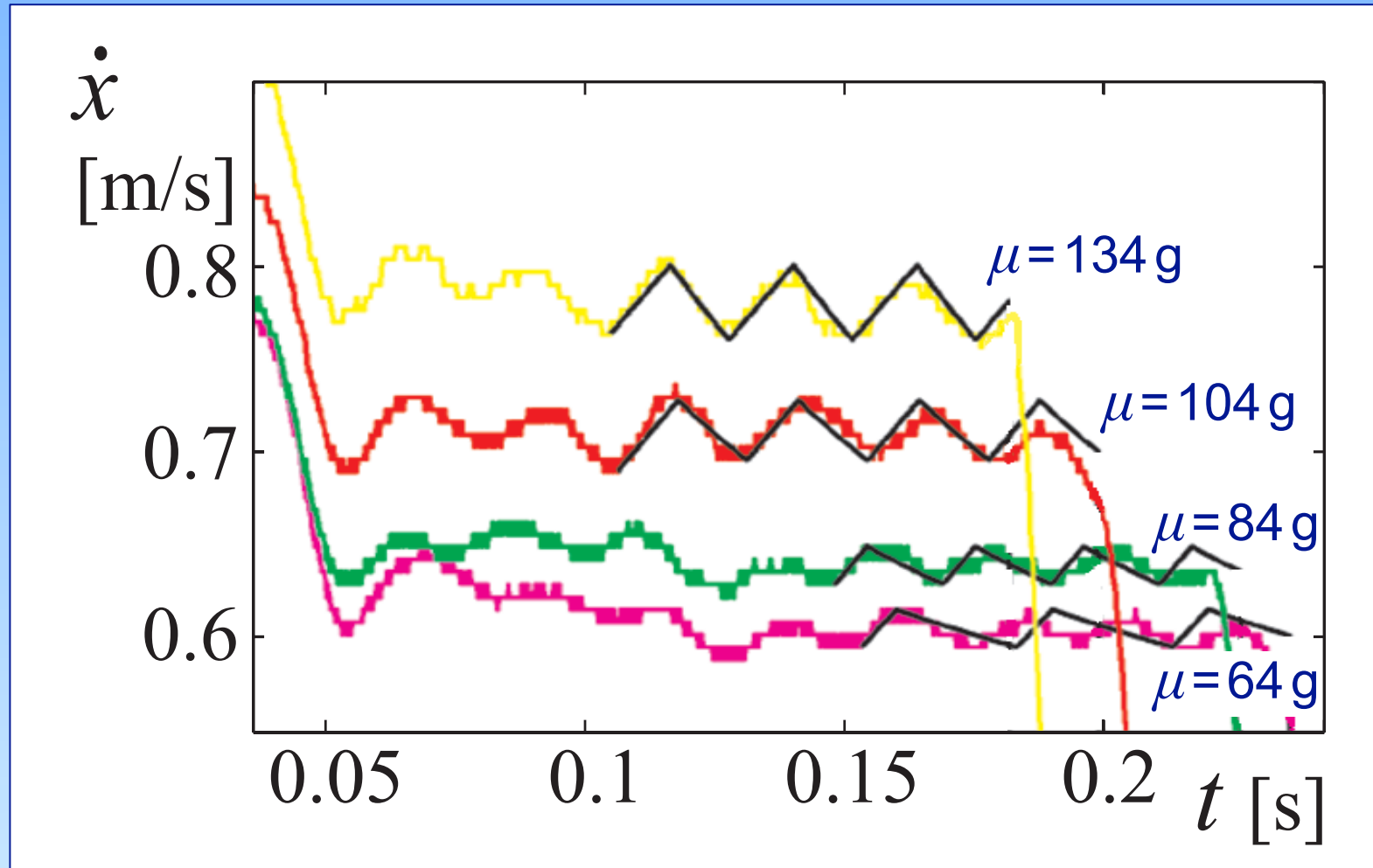
$$m\ddot{x} = \mu g + D$$

with:

$$D = \begin{cases} -B_1\dot{x} & \text{when } \dot{x} \text{ falls below } u_1 \\ -B_2\dot{x} & \text{when } \dot{x} \text{ rises above } u_2 \end{cases}$$

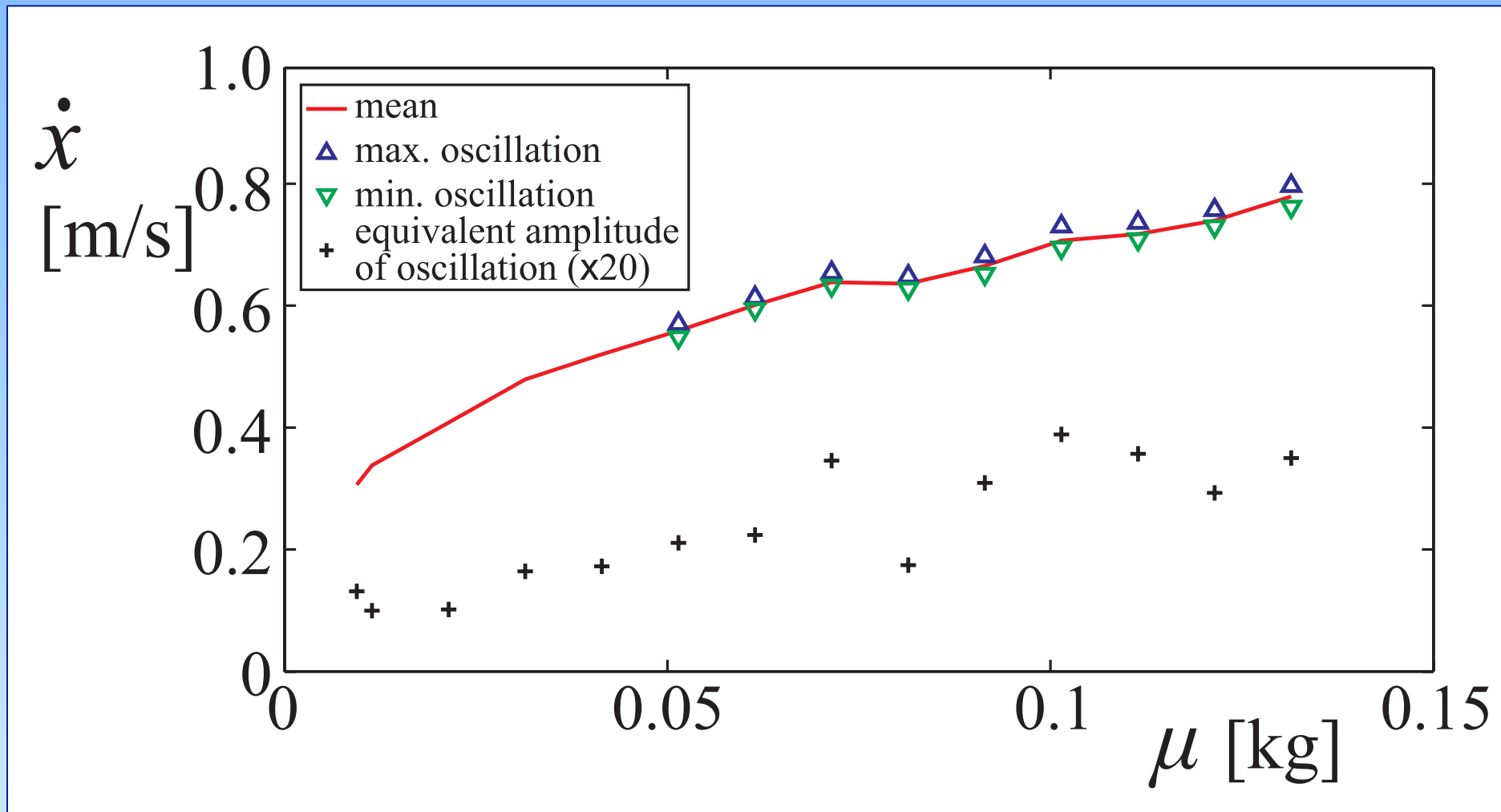


Results for fixed B_1, B_2

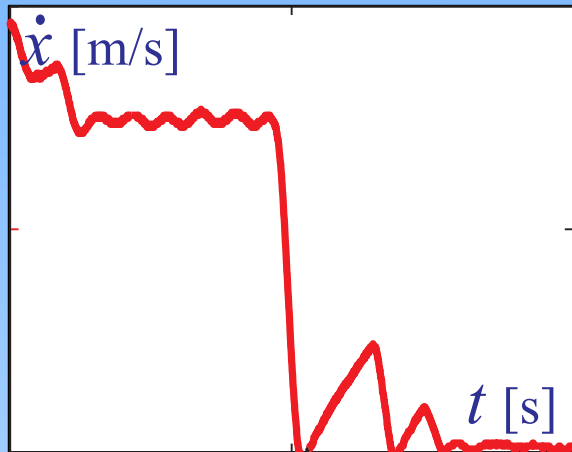


Drawback: u_1, u_2 need to be redefined for each μ

Velocities u_1, u_2 vs mass μ

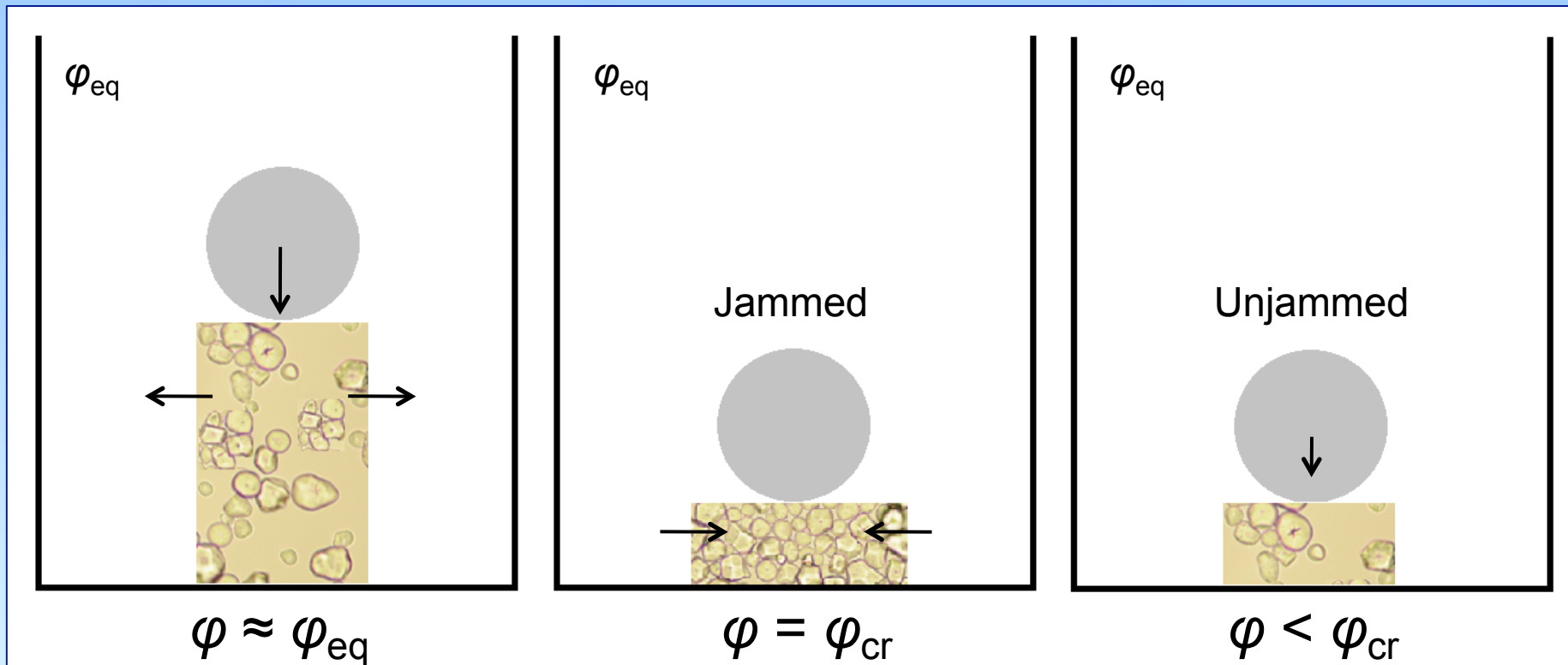


Stop-go cycles at the bottom



Fast deceleration points to jamming:

- ▶ $\dot{x} > 0$, liquid squeezed out
- ▶ ϕ increases
- ▶ jamming by compaction, $\phi = \phi_{cr}$, $\dot{x} = 0$
- ▶ particles rearrange on fluid time scale
- ▶ ϕ decreases, relaxation, $\dot{x} > 0$



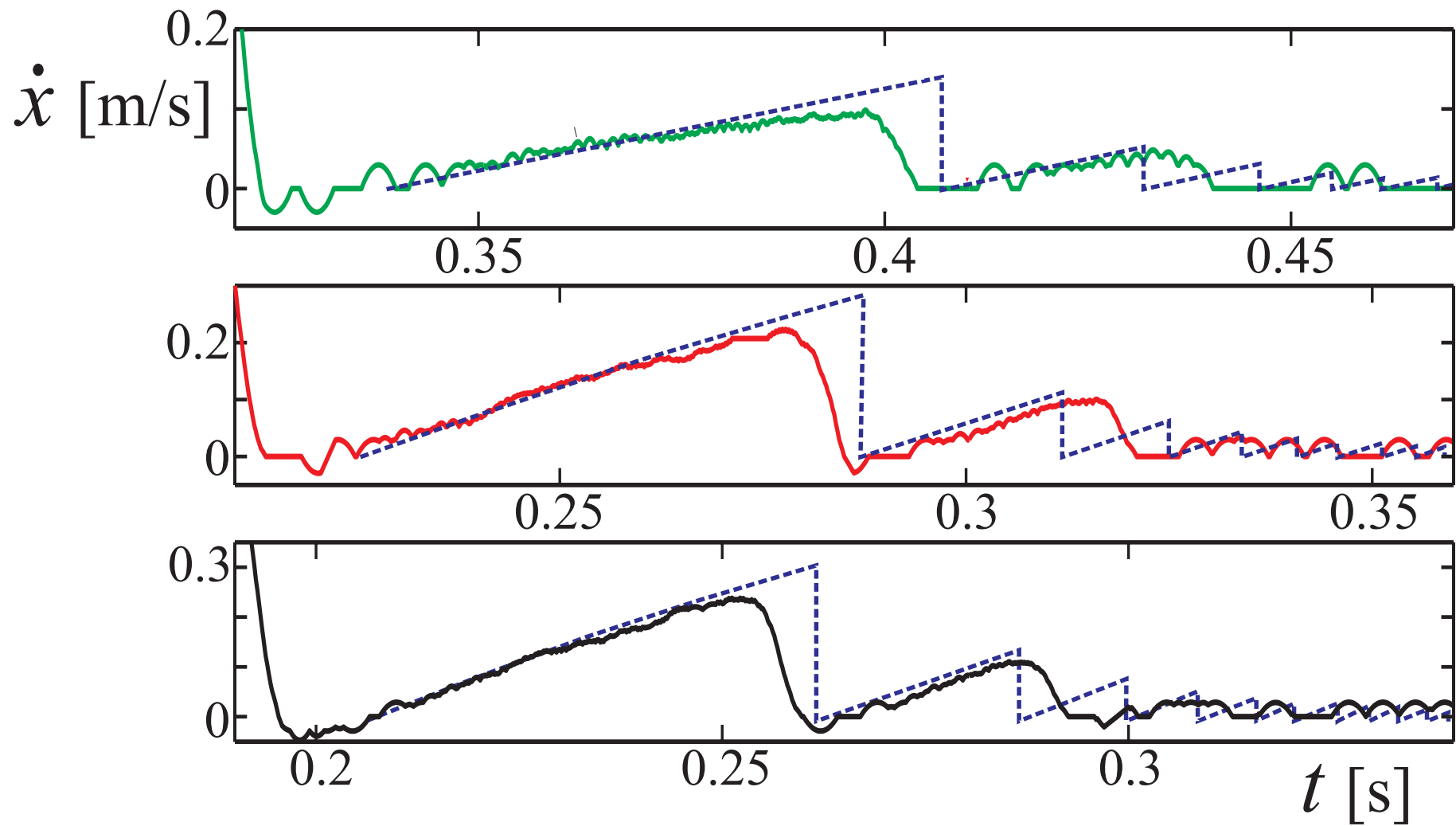
A minimal model

$$\begin{cases} m\ddot{x} = \mu g + D & \text{when } \phi < \phi_{cr} \\ \dot{x} = 0 & \text{when } \phi \geq \phi_{cr} \end{cases}$$

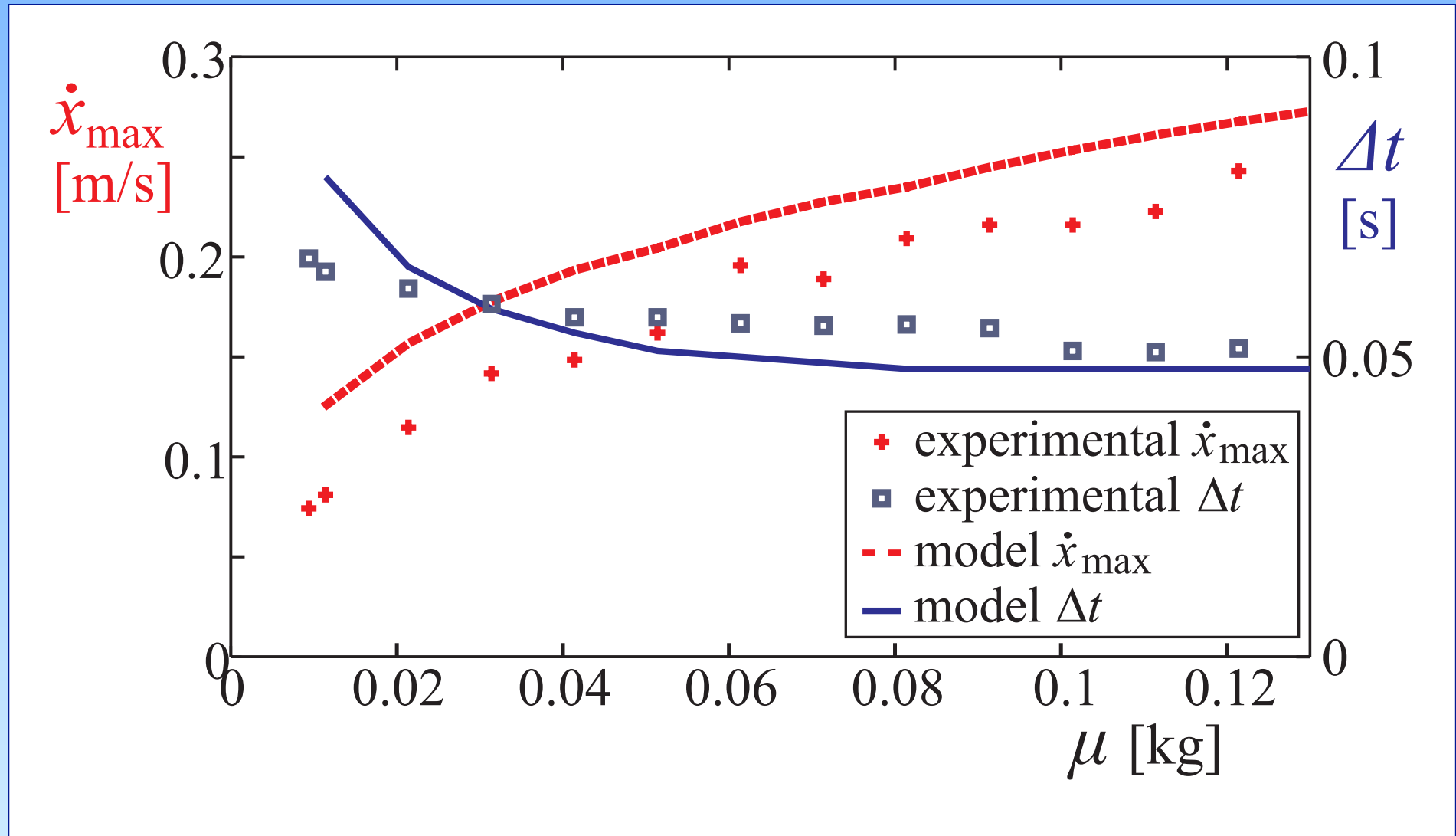
$$\dot{\phi} = -c \frac{\dot{x}}{x} - \kappa(\phi - \phi_{eq})$$

increases ϕ **decreases ϕ**
due to compression **due to relaxation**
($-\dot{x}/x$ = compression rate)

Comparing to experiment

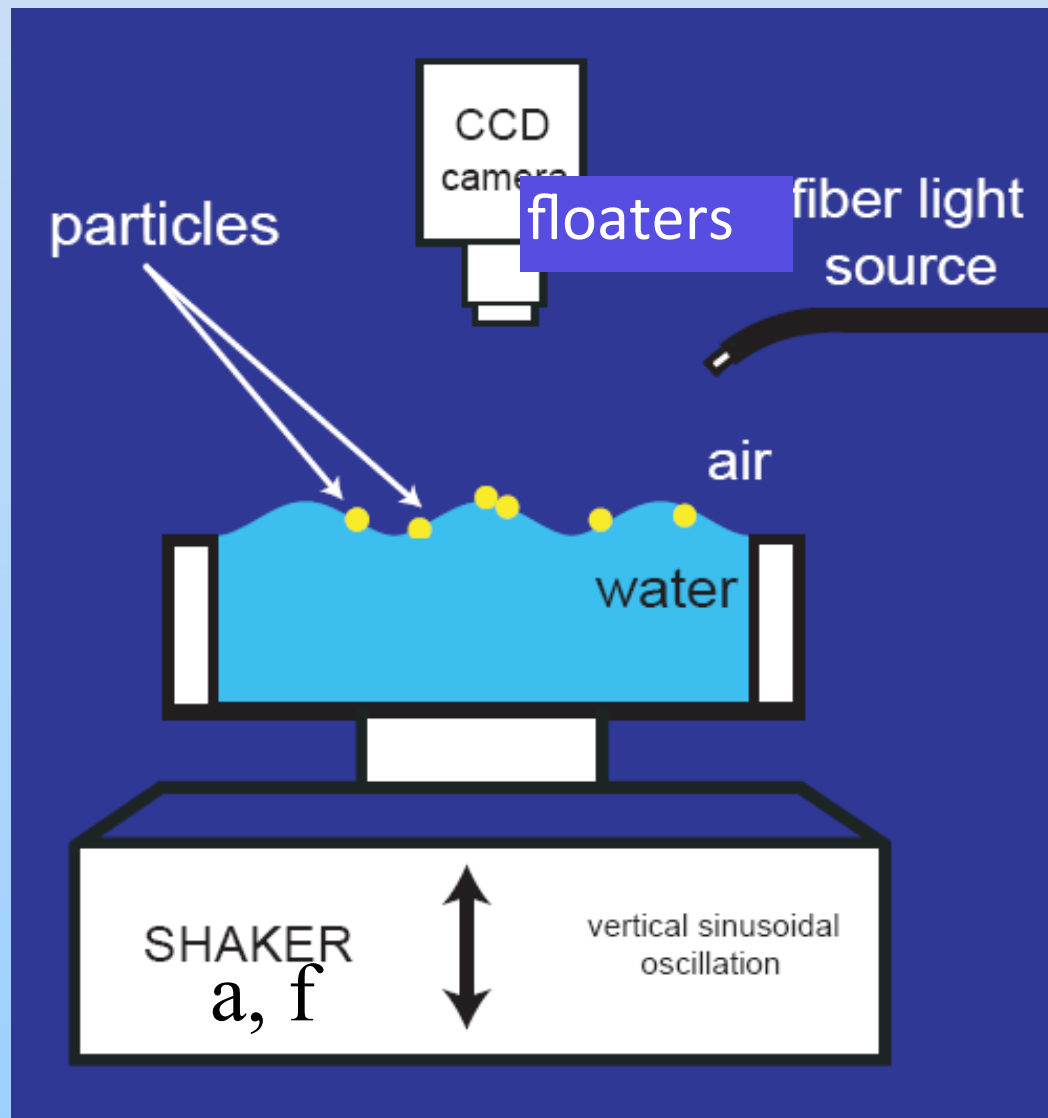


Comparing to experiment



Floating particles on Faraday waves

Floating particles on Faraday waves



Control Parameters:

- D = floater size
- θ = wetting angle
- a = amplitude
- f = frequency
- ϕ = concentration

$$\phi = \text{Area}_{\text{floater}} / \text{Area}_{\text{total}}$$

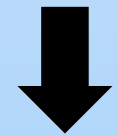
low ϕ

5 mm



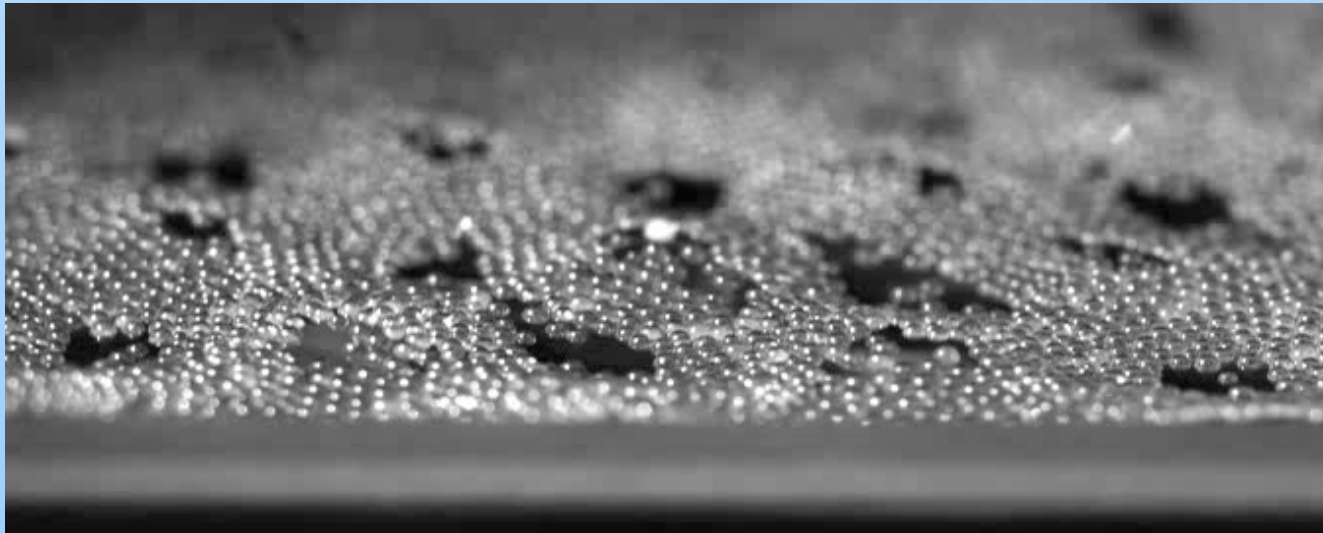
antinode
clusters

$f = 19$ Hz
 $a = 2$ mm



adding more
floaters

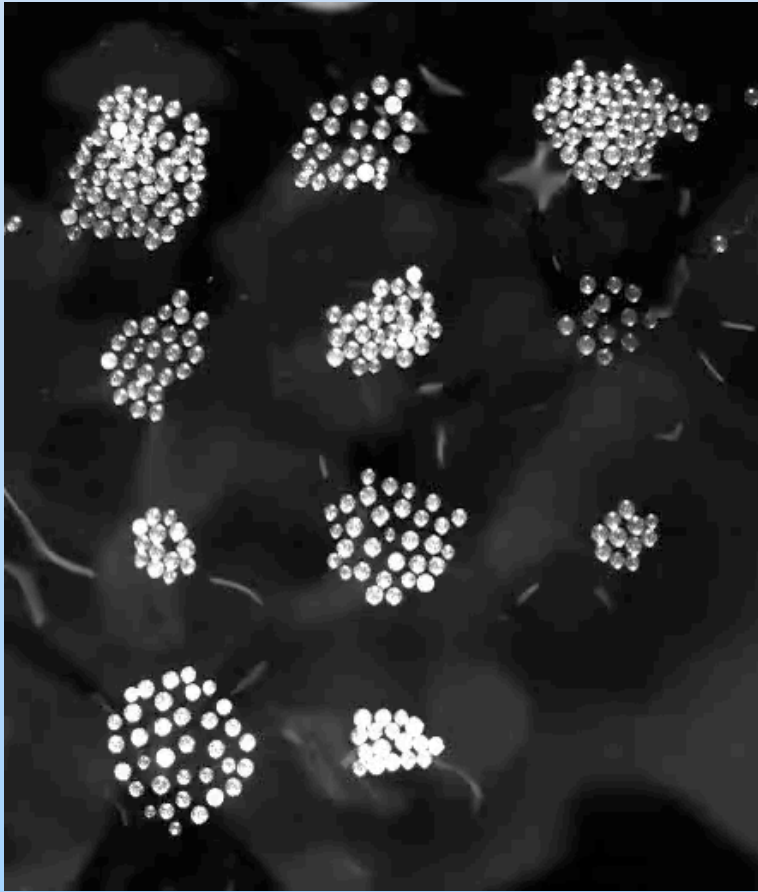
high ϕ



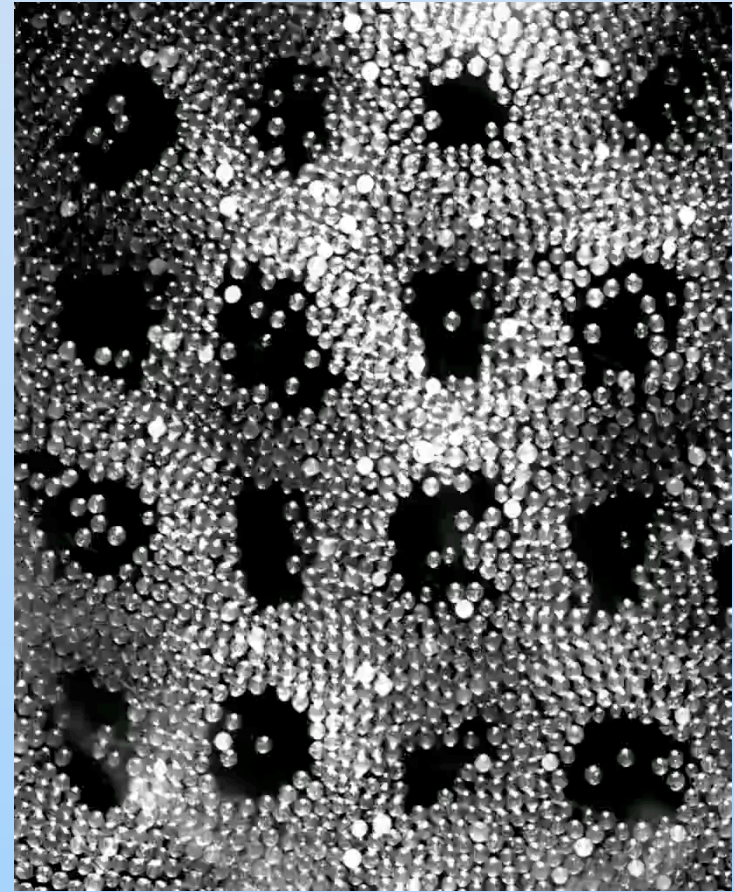
node
clusters

$f = 20$ Hz
 $a = 2.2$ mm

10 mm



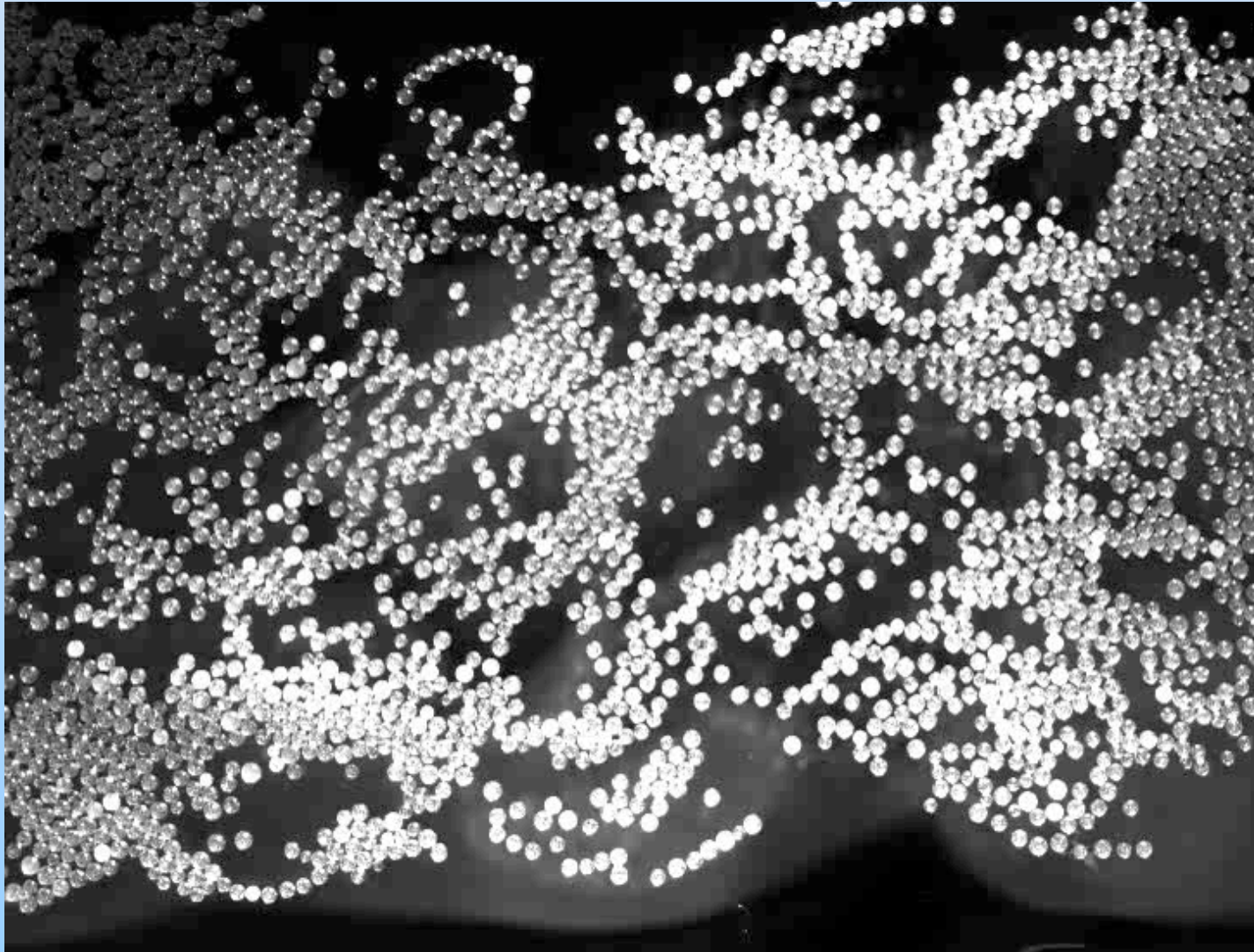
low ϕ : antinode clusters



high ϕ : node clusters

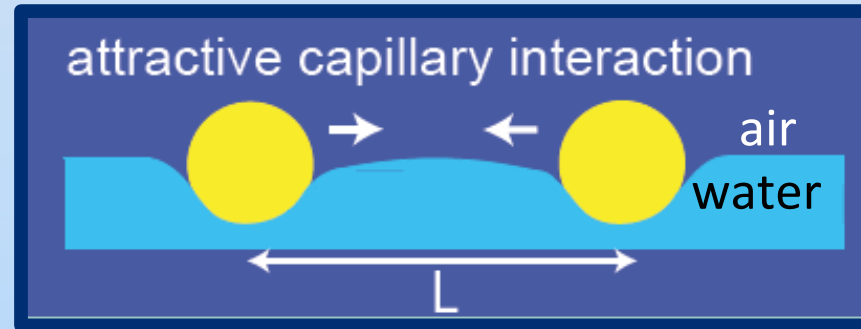
- What is the physical origin of the clustering?
- What happens at intermediate ϕ ?

Structures at intermediate ϕ



Competition between forces

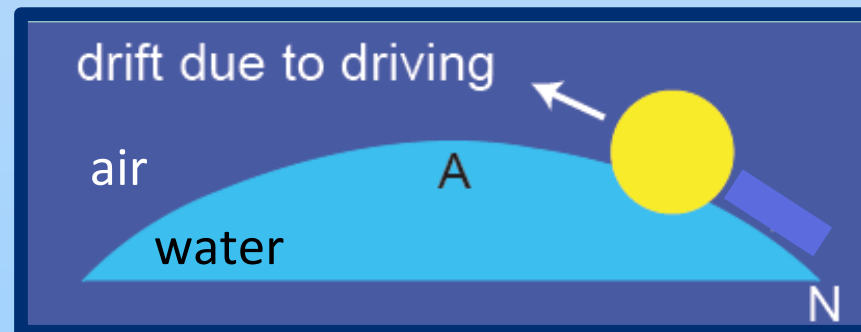
capillarity
(weak)



$$F \sim 1.2 \text{ nN at } L \sim D \text{ (experiment)}$$

+

drift force
(strong)



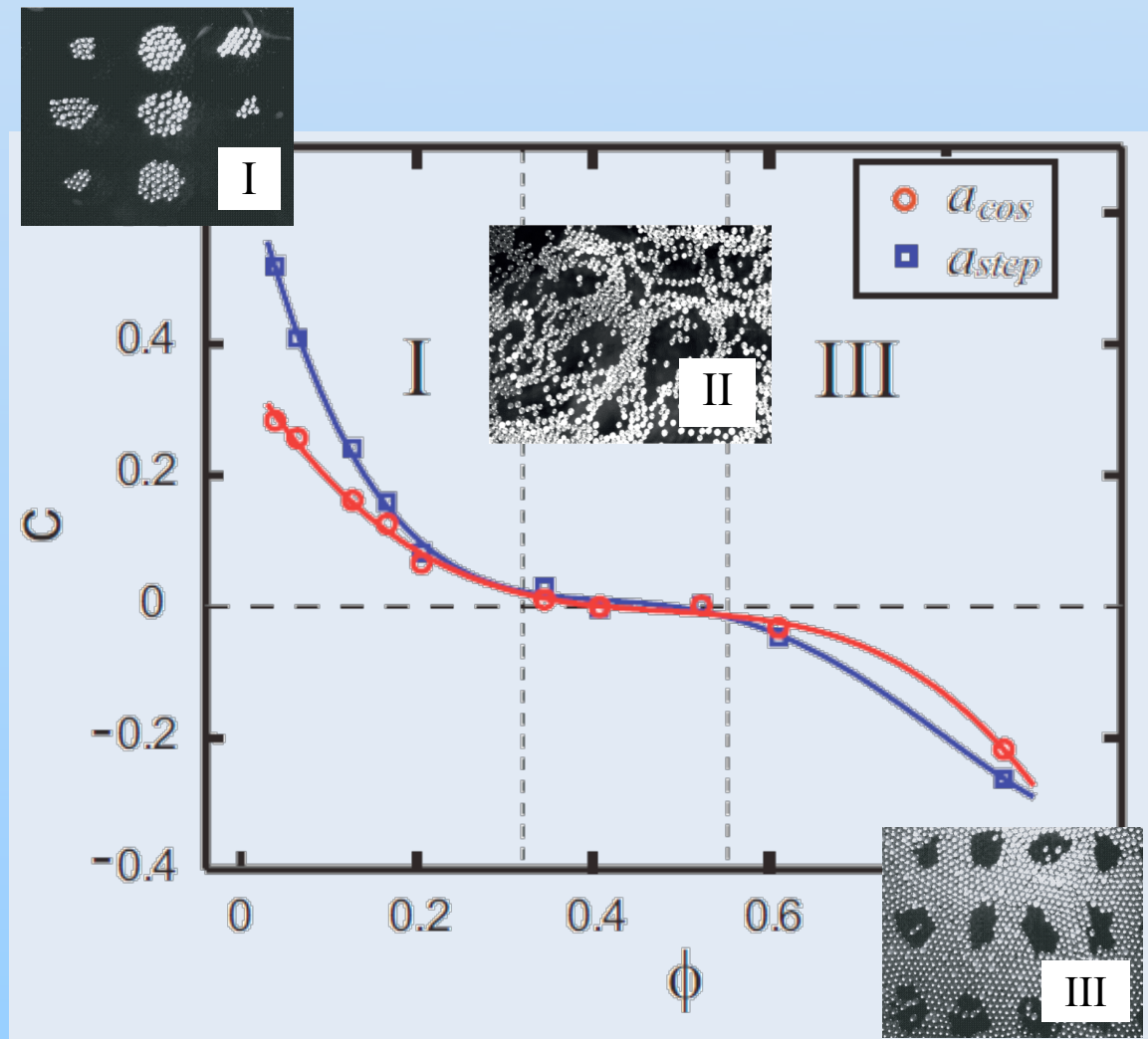
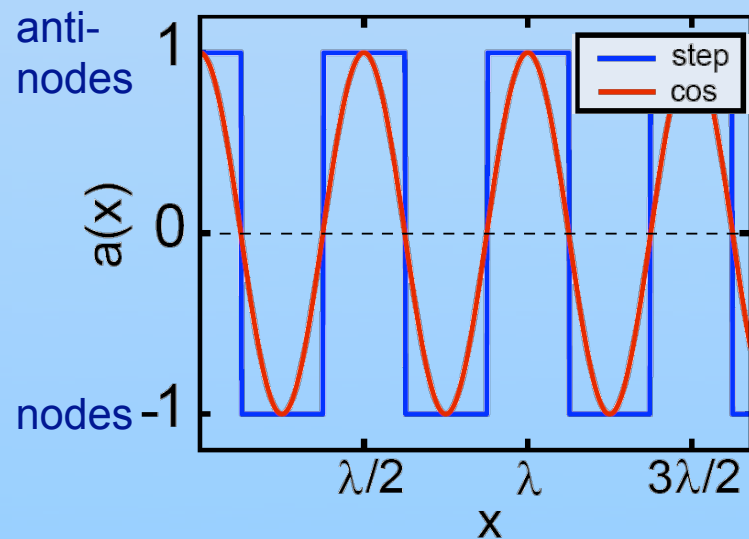
$$F \sim 2000 \text{ nN (theory* - one particle model)}$$

* G. Falkovich *et al.* Nature 435, 1045 (2005).

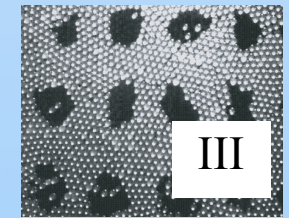
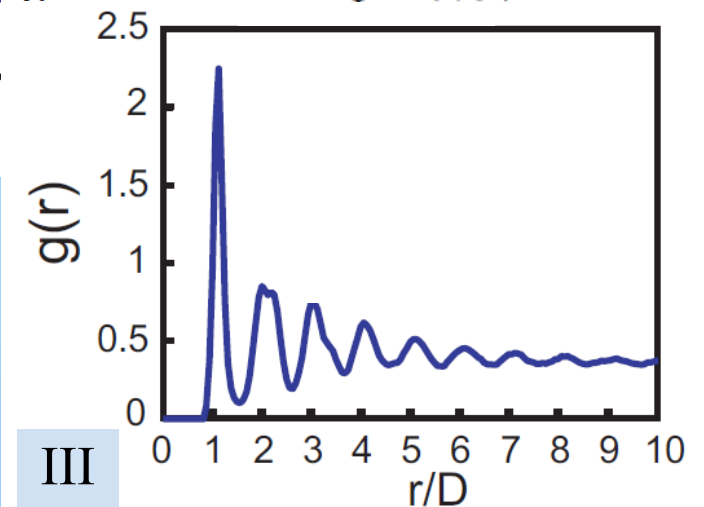
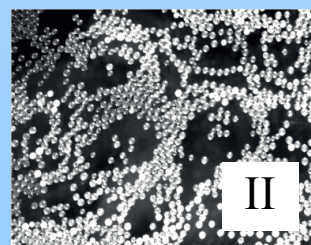
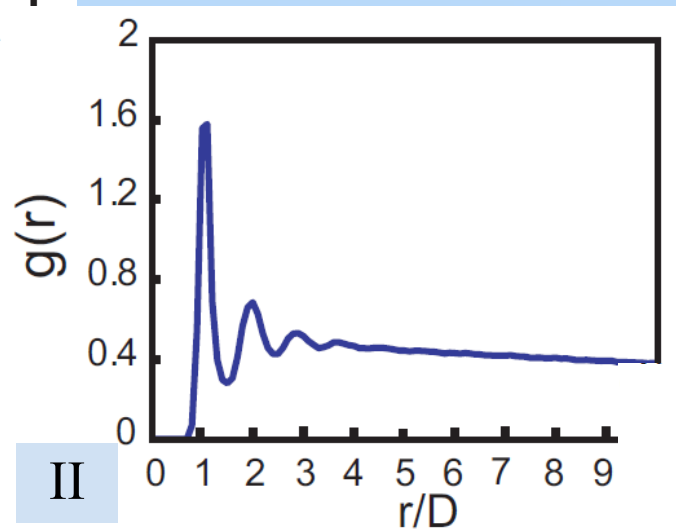
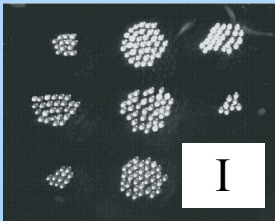
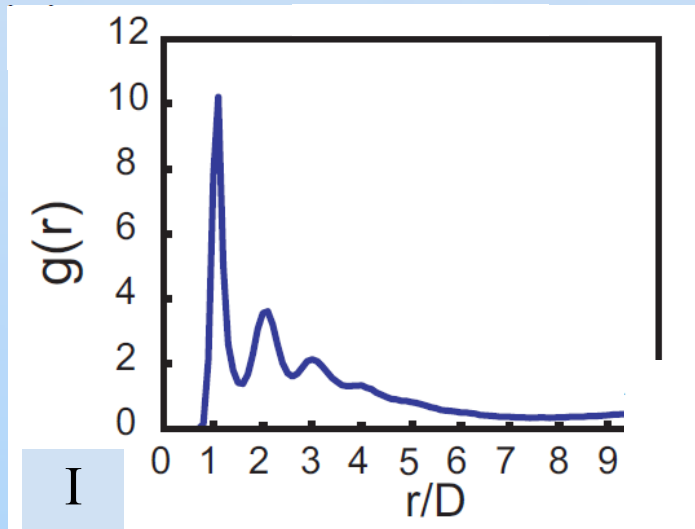
Experimental analysis:
Characterizing the antinode –
node cluster transition

Global characterization: Correlation number c

$$c = \frac{\langle \phi(\mathbf{r}, t) a(\mathbf{r}) \rangle_{\mathbf{r}, t}}{\langle \phi(\mathbf{r}, t) \rangle_{\mathbf{r}, t}}$$

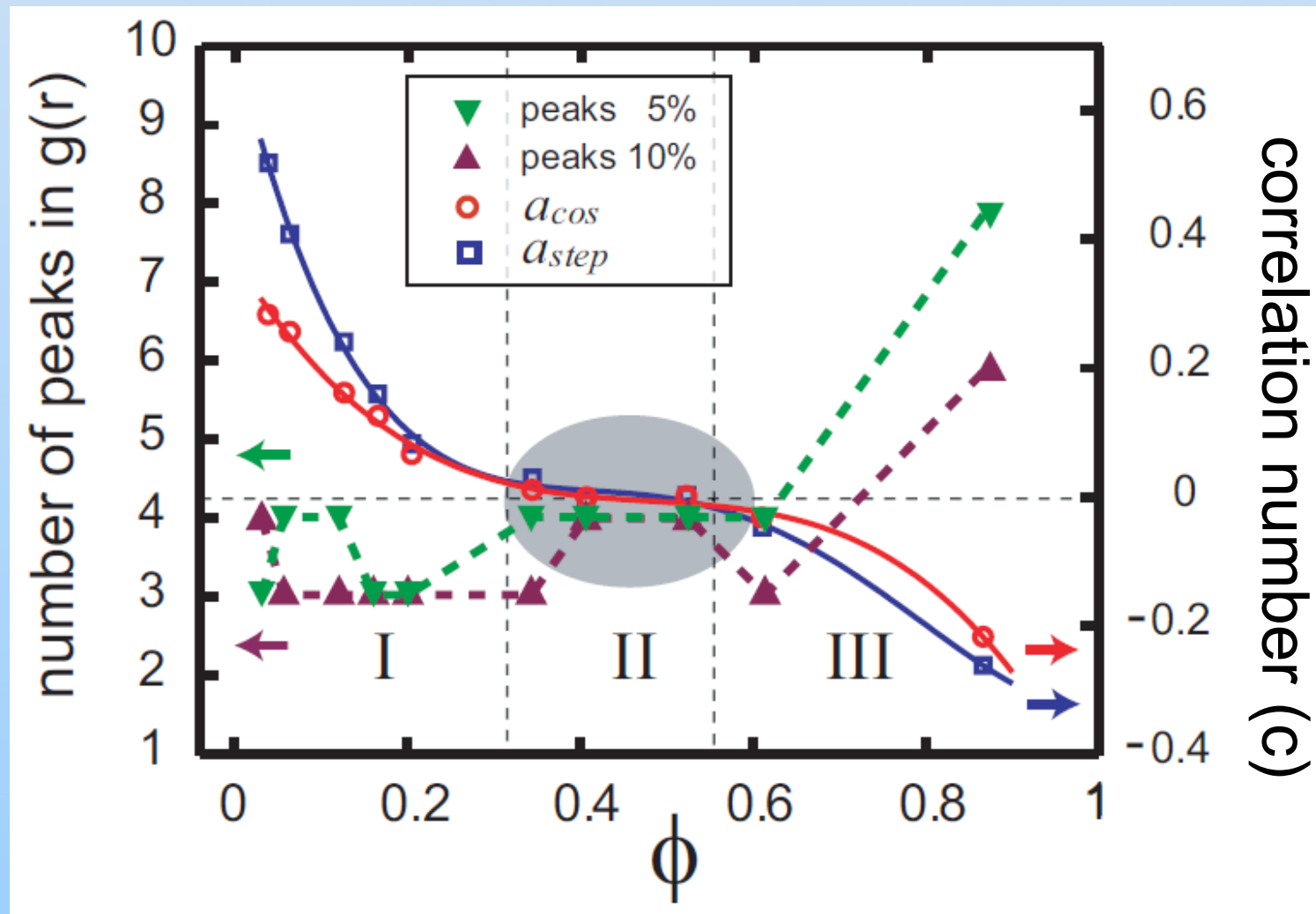


Local characterization: Pair correlation function $g(r)$



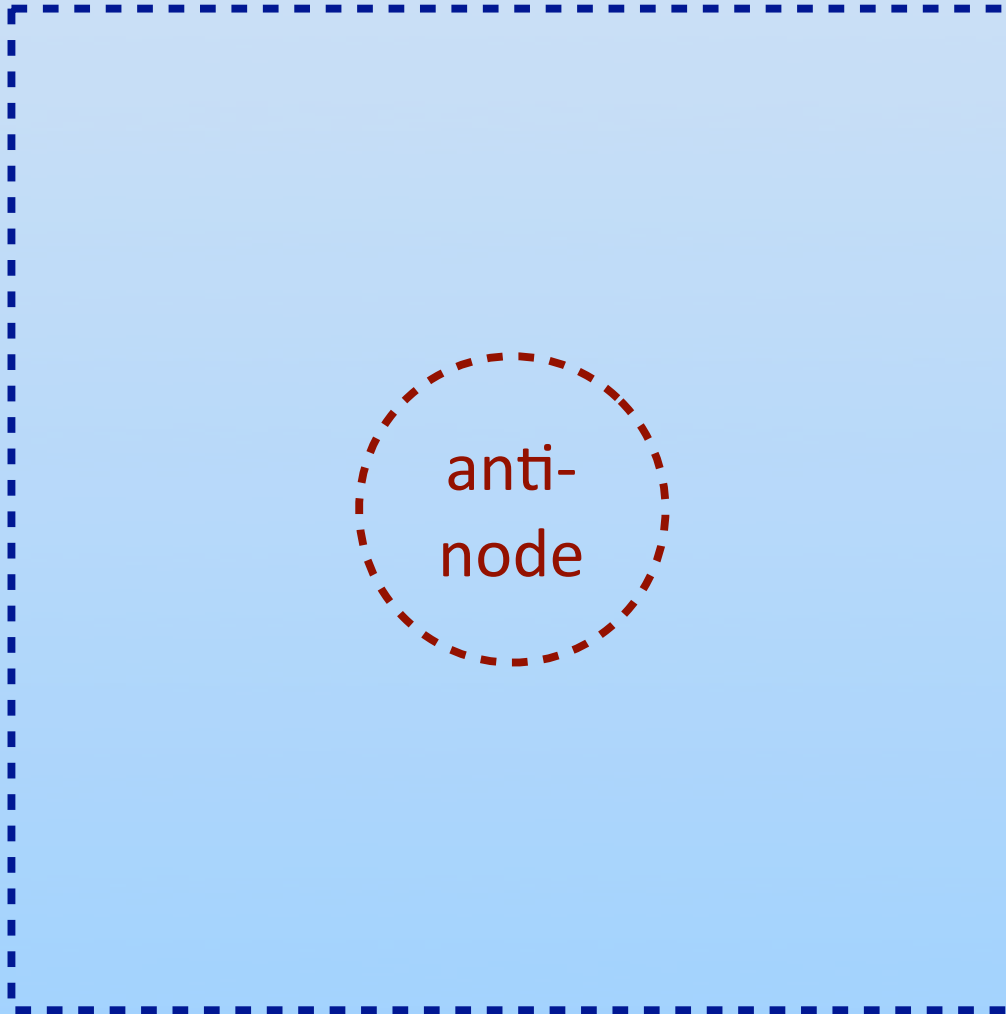
(D = floater diameter)

Global vs local characterization



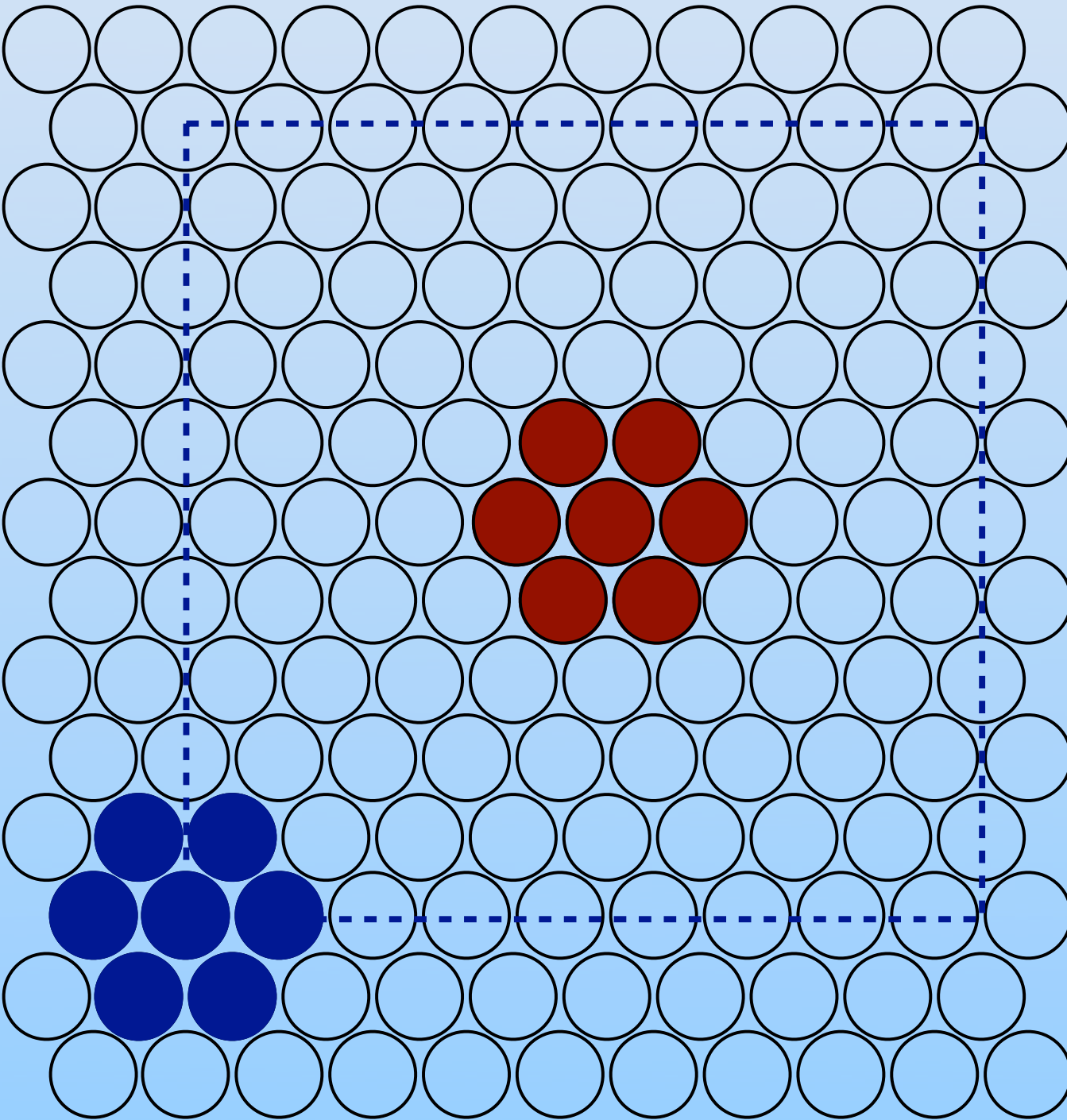
What is the origin of the antinode-node cluster transition?

wave pattern



anti-
node

nodal lines



wave pattern

add particles:

▶ at antinode

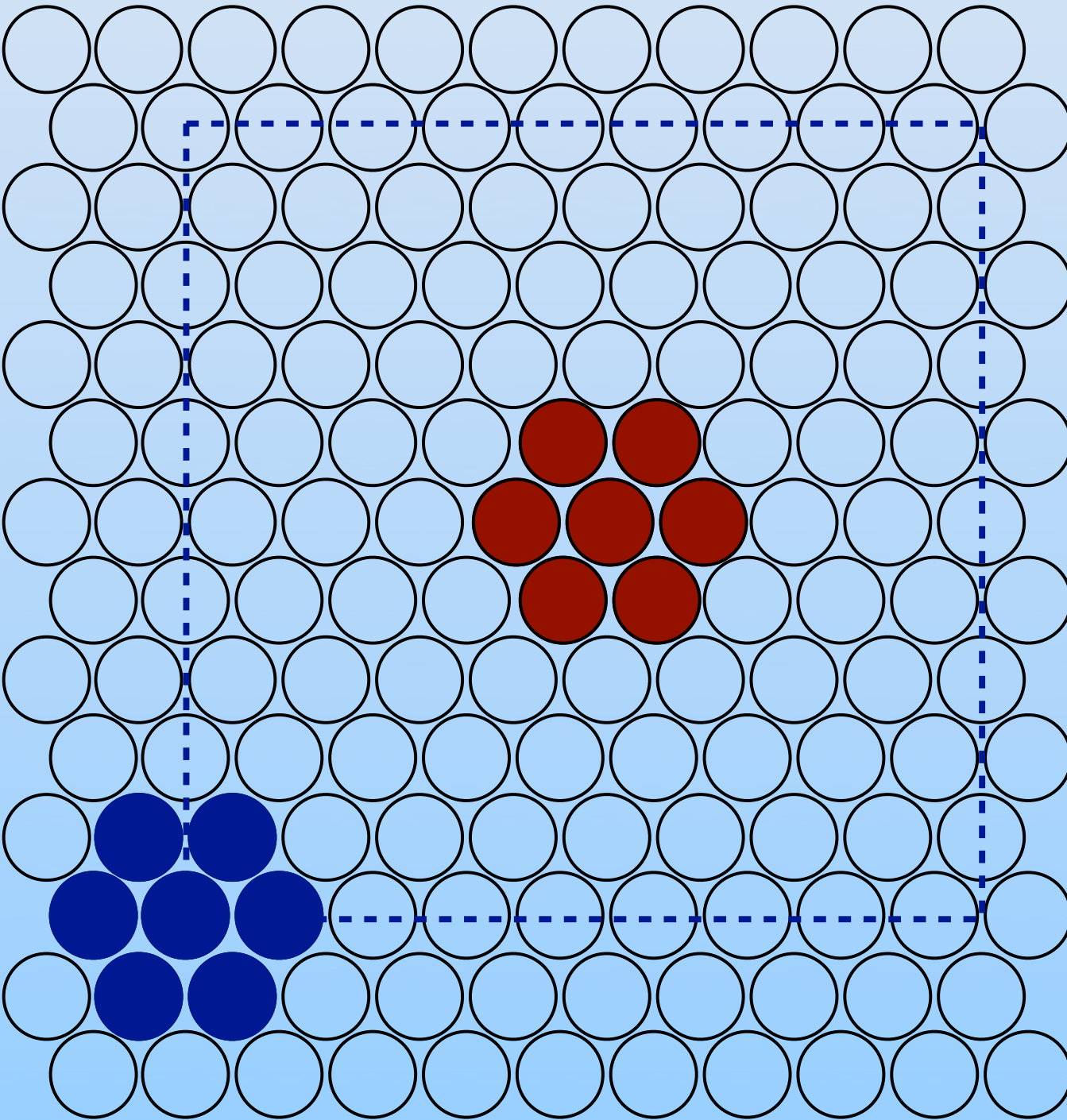
▶ at node

energy:

(capillary & drift)

$$U_{\text{cap,anti}} = U_{\text{cap,node}}$$

$$U_{\text{drift,anti}} < U_{\text{drift,node}}$$



wave pattern

add particles:

▶ at antinode

▶ at node

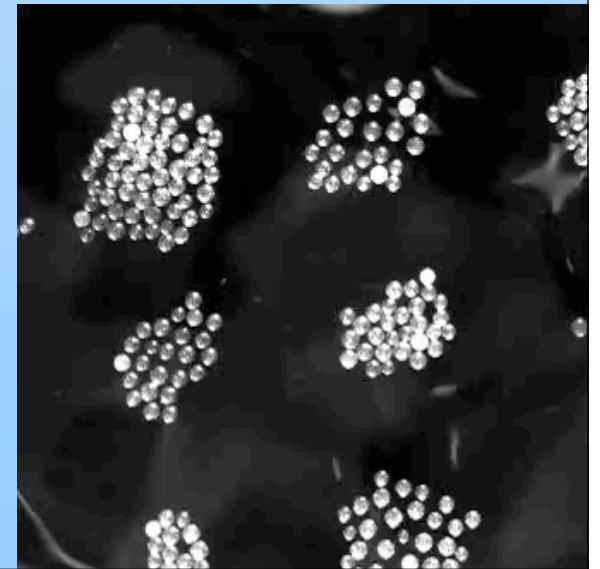
~~energy:~~

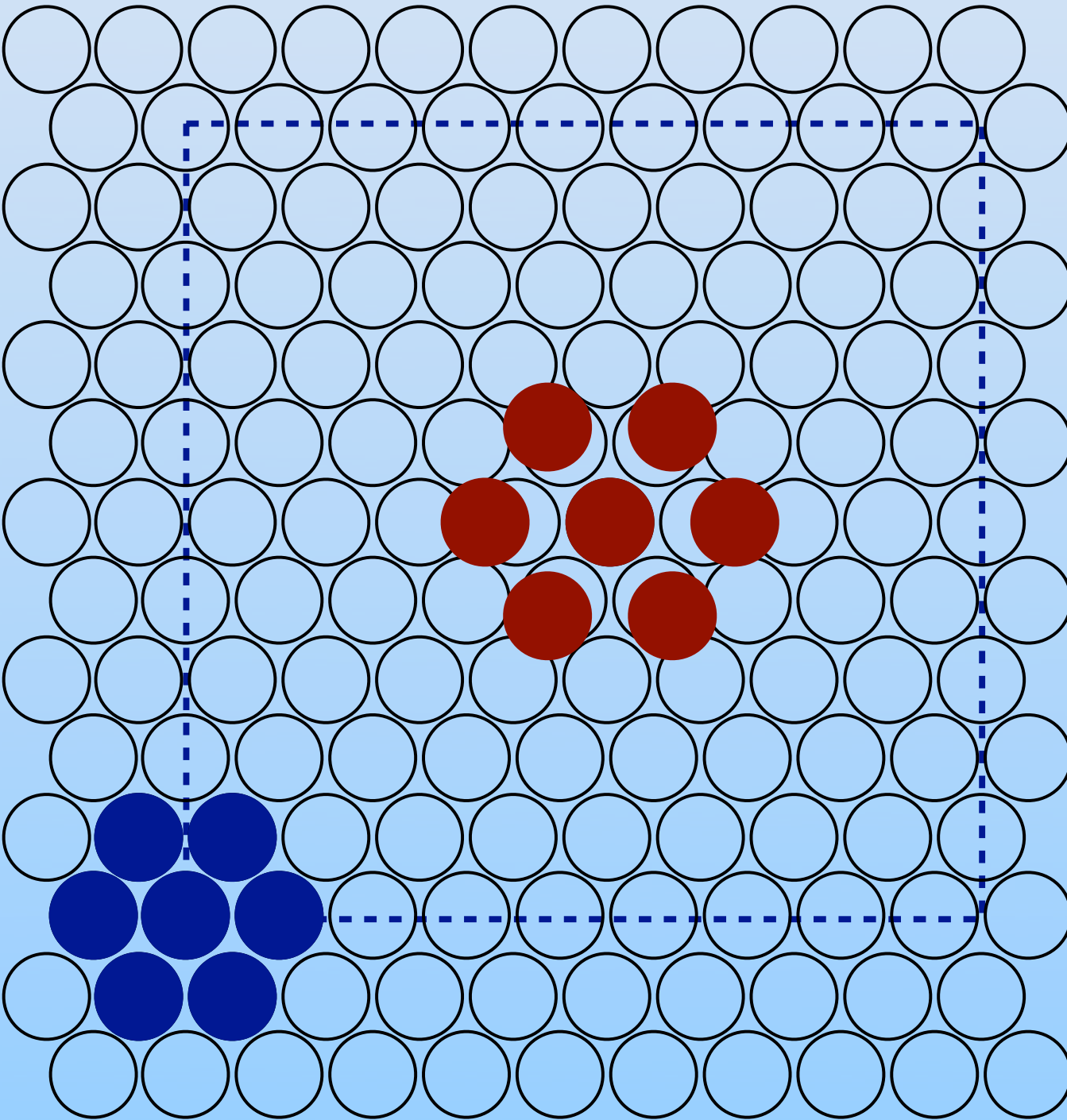
~~(capillary & drift)~~

~~$U_{\text{cap,anti}} = U_{\text{cap,node}}$~~

~~$U_{\text{drift,anti}} < U_{\text{drift,node}}$~~

add breathing:





wave pattern

add particles:

▶ at antinode

▶ at node

~~energy:~~

~~(capillary & drift)~~

~~$U_{\text{cap,anti}} = U_{\text{cap,node}}$~~

~~$U_{\text{drift,anti}} < U_{\text{drift,node}}$~~

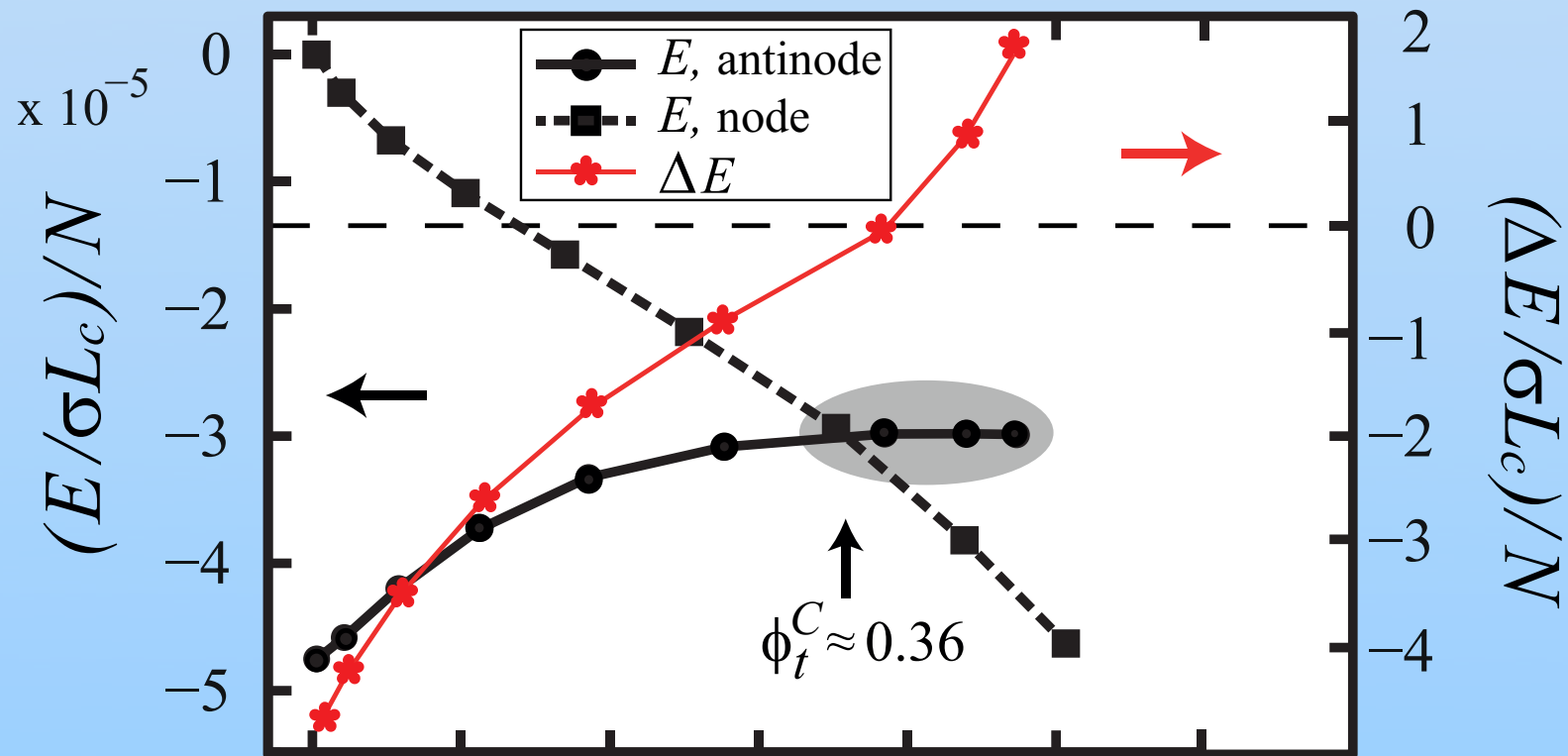
add breathing:

$U_{\text{cap,anti}} > U_{\text{cap,node}}$

$U_{\text{drift,anti}} < U_{\text{drift,node}}$

Competition between capillary and drift energy

- ▶ antinode: U_{drift} favorable, U_{cap} unfavorable
- ▶ node: U_{drift} unfavorable, U_{cap} favorable



Competition between capillary and drift energy

- ▶ antinode: U_{drift} favorable, U_{cap} unfavorable
- ▶ node: U_{drift} unfavorable, U_{cap} favorable

