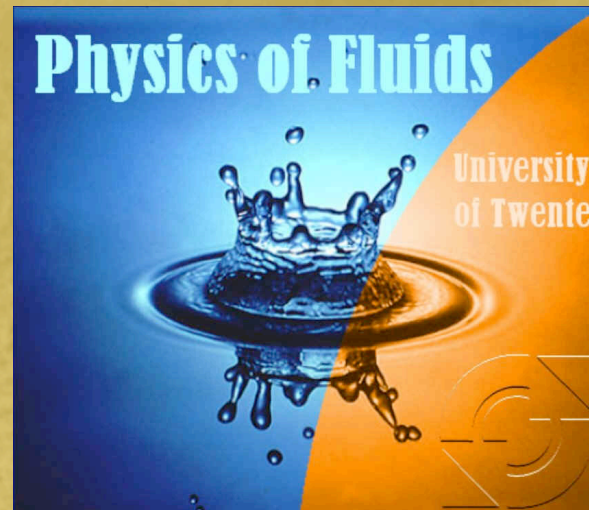


Granular matter and interstitial fluids

Devaraj van der Meer

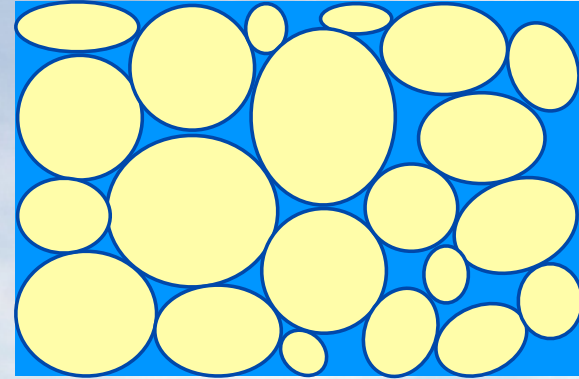
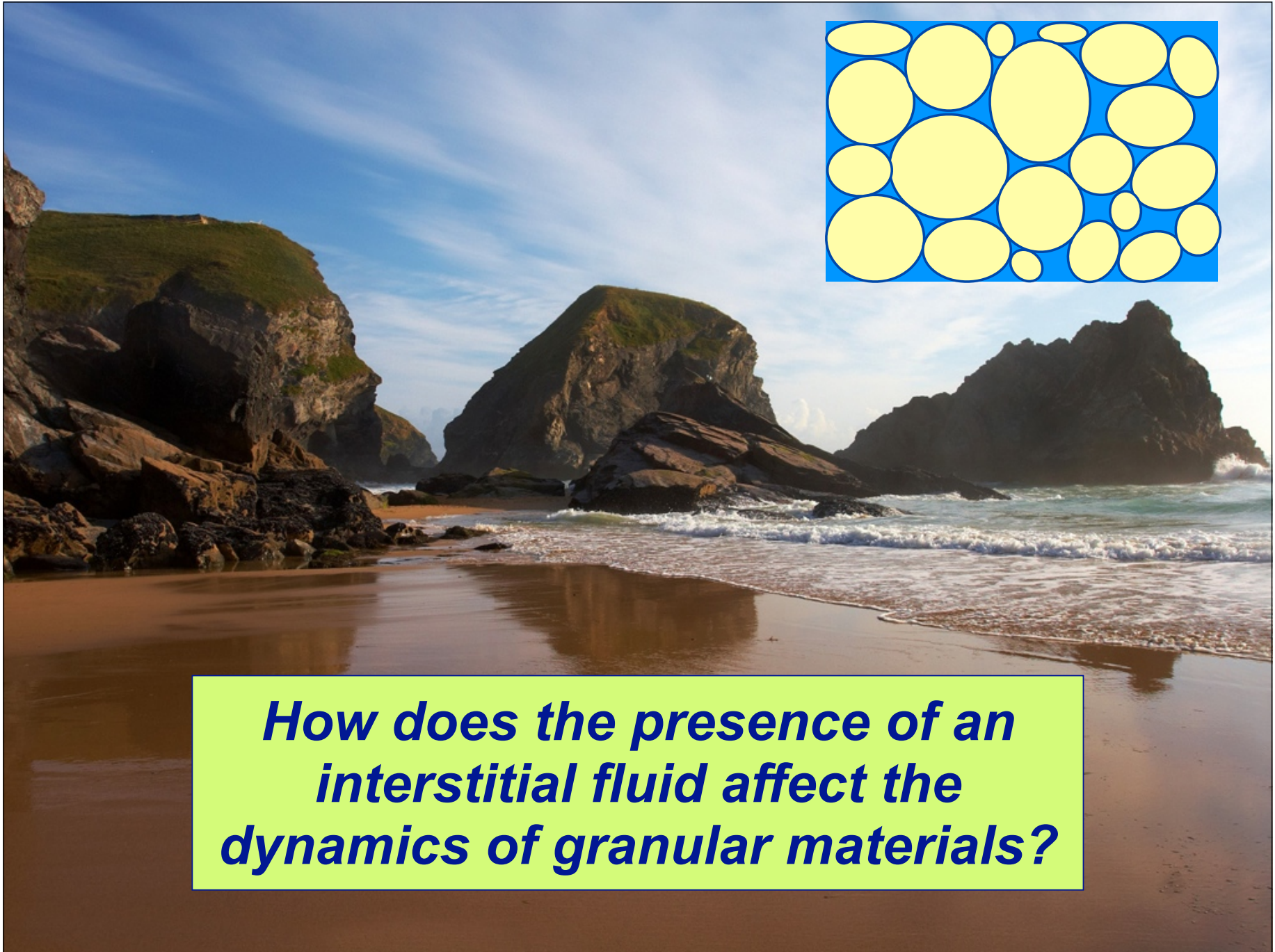


J.M. Burgerscentrum



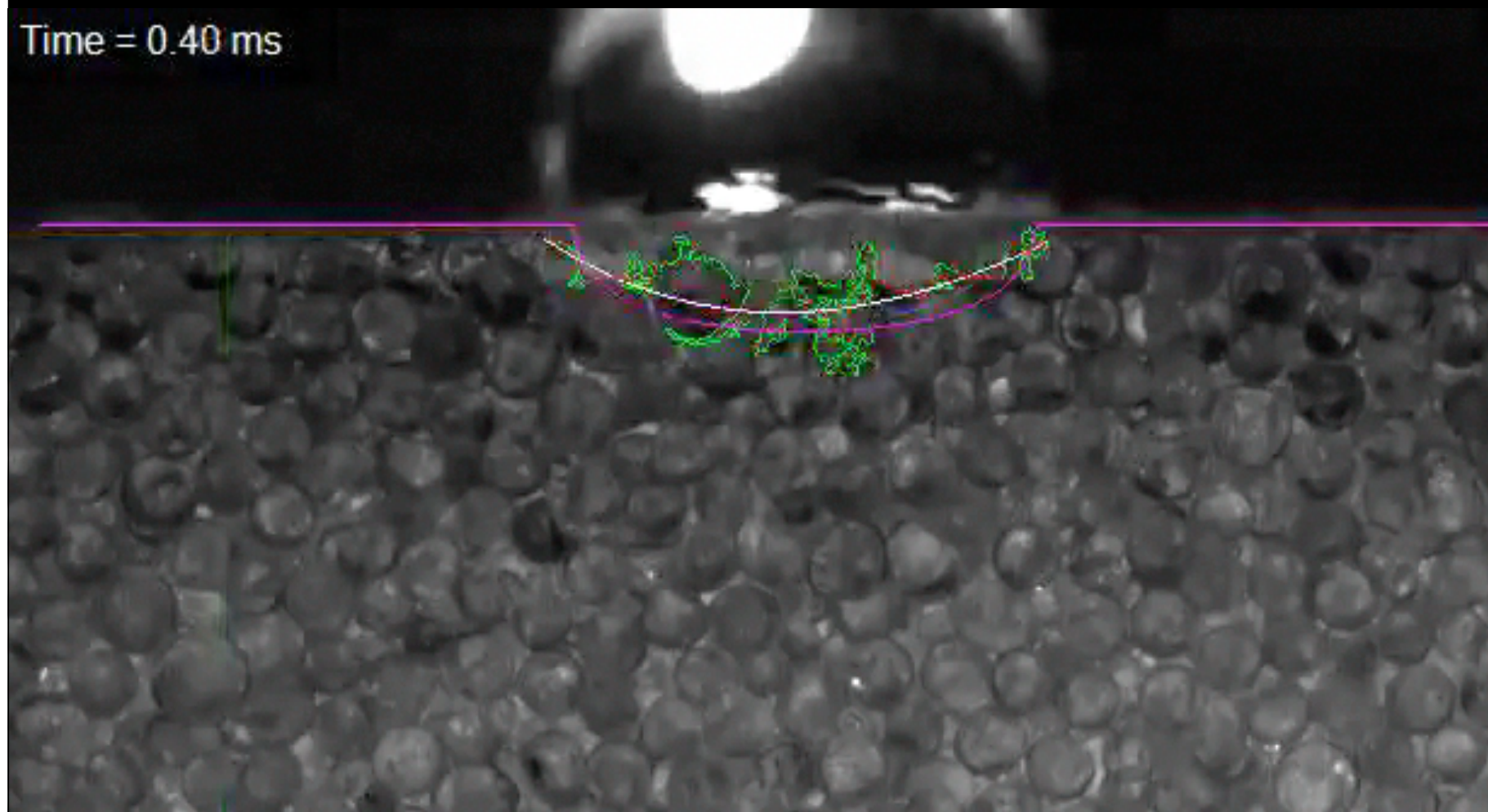
Physics of Fluids - University of Twente – The Netherlands



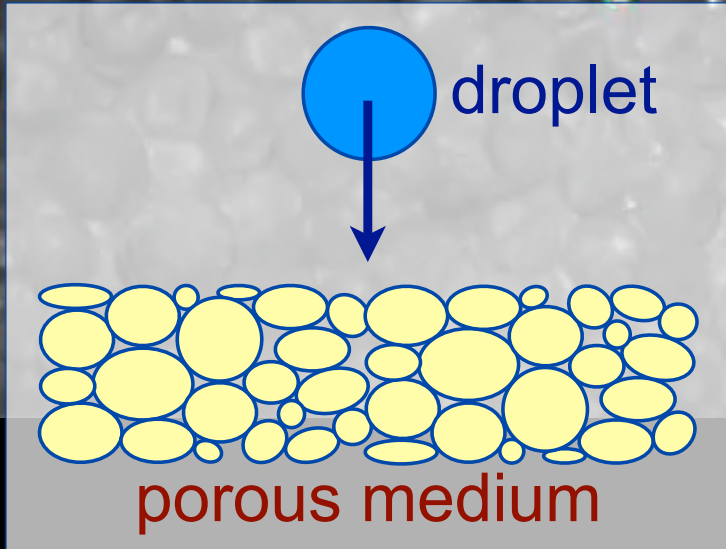
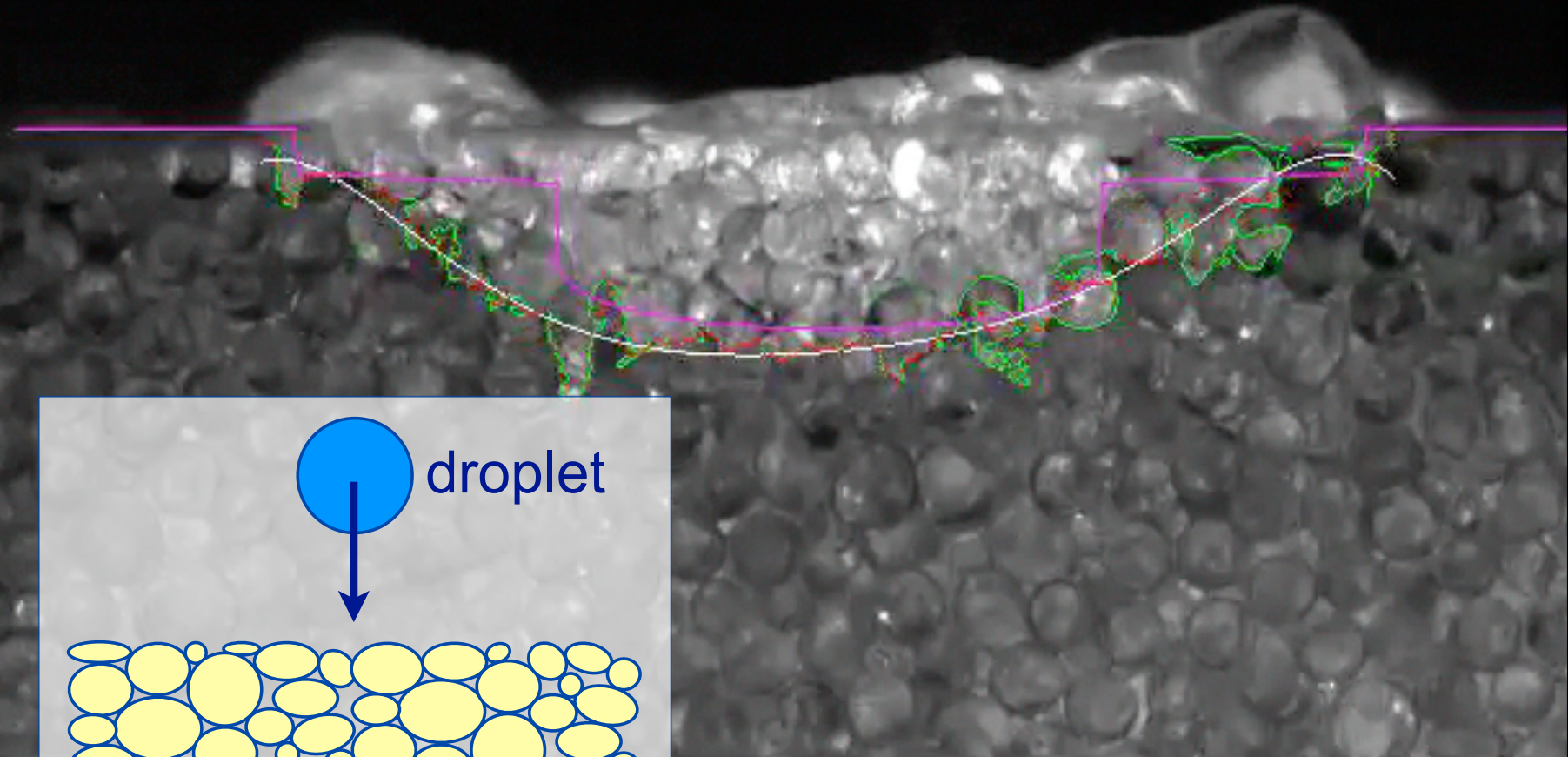


How does the presence of an interstitial fluid affect the dynamics of granular materials?

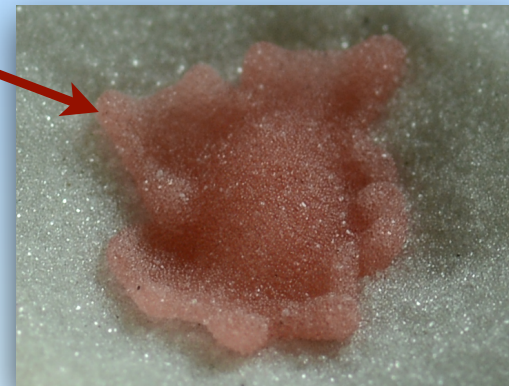
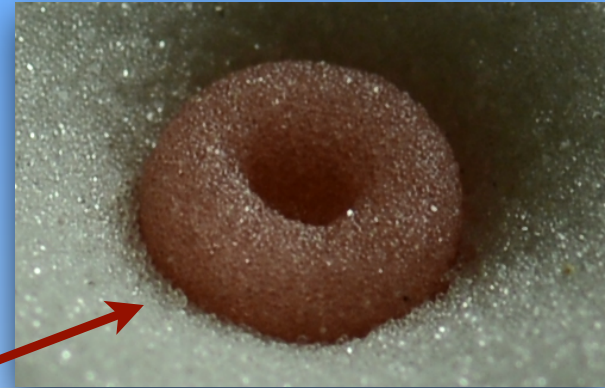
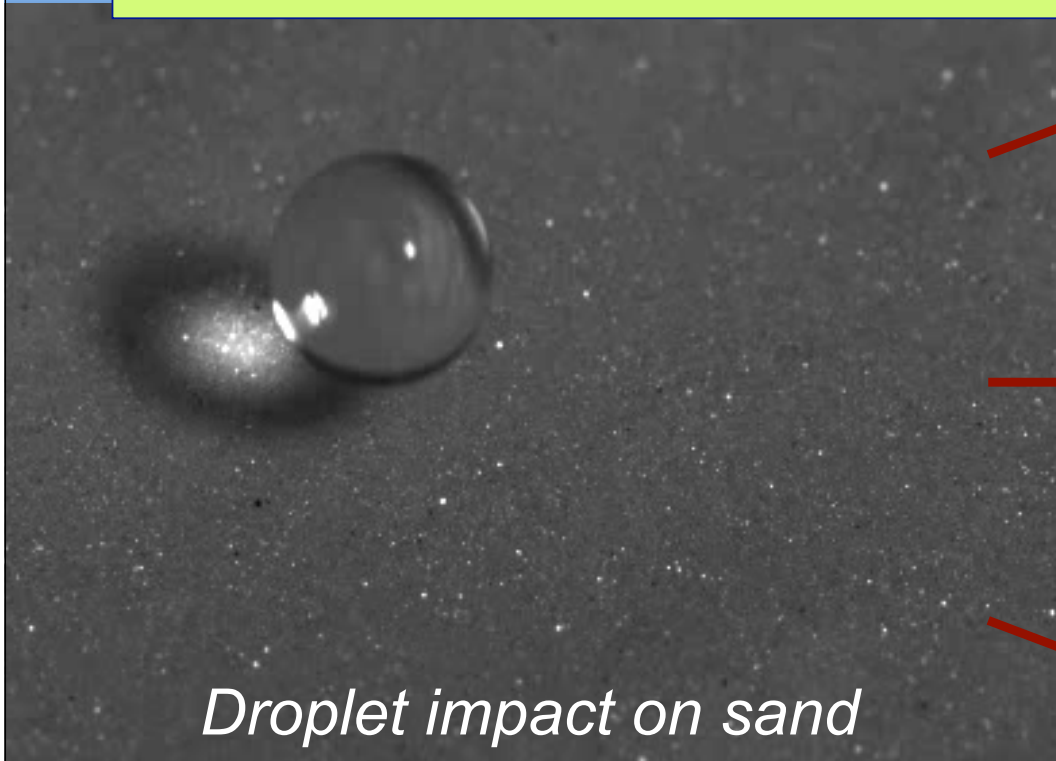
Time = 0.40 ms



Time = 3.07 ms

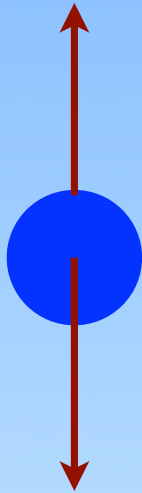


***residue shape depends
on mixing rate***



Role of interstitial fluid: single particle

$$F_{drag} = 3\pi\eta dV$$



$$F_g = \frac{1}{6}\pi d^3 \rho_p g$$

d = particle diameter

V = typical particle velocity

η = air viscosity ($2 \cdot 10^{-5}$ Pa·s)

ρ_p = part. density ($2.5 \cdot 10^3$ kg/m³)

g = grav. acceleration (10 m/s²)

$$B \equiv \frac{F_{drag}}{F_g} = \frac{18\eta V}{\rho_p g d^2}$$

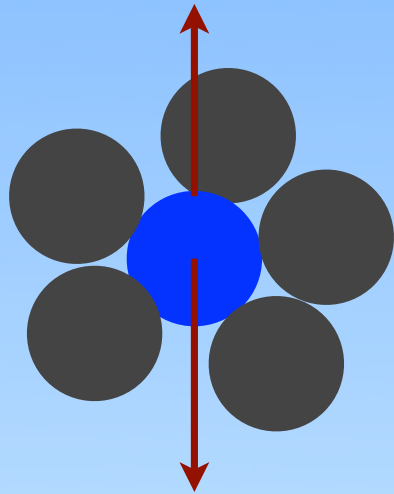
$$B \approx 1 \rightarrow d \approx \sqrt{\frac{18\eta V}{\rho_p g}}$$

$$V \approx 1 \text{ m/s} \rightarrow d \approx 120 \mu\text{m}$$

$$V \approx \sqrt{2gd} \rightarrow d \approx 16 \mu\text{m}$$

Role of interstitial fluid: packed particle

$$F_{f \rightarrow s} = 2k \frac{1 - \varepsilon}{\varepsilon^3} F_{drag}$$



$$F_g = \frac{1}{6} \pi d^3 \rho_p g$$

$\varepsilon = 1 - \phi = \text{porosity} (\approx 0.5)$

$k = \text{Kozeny constant} (\approx 5)$

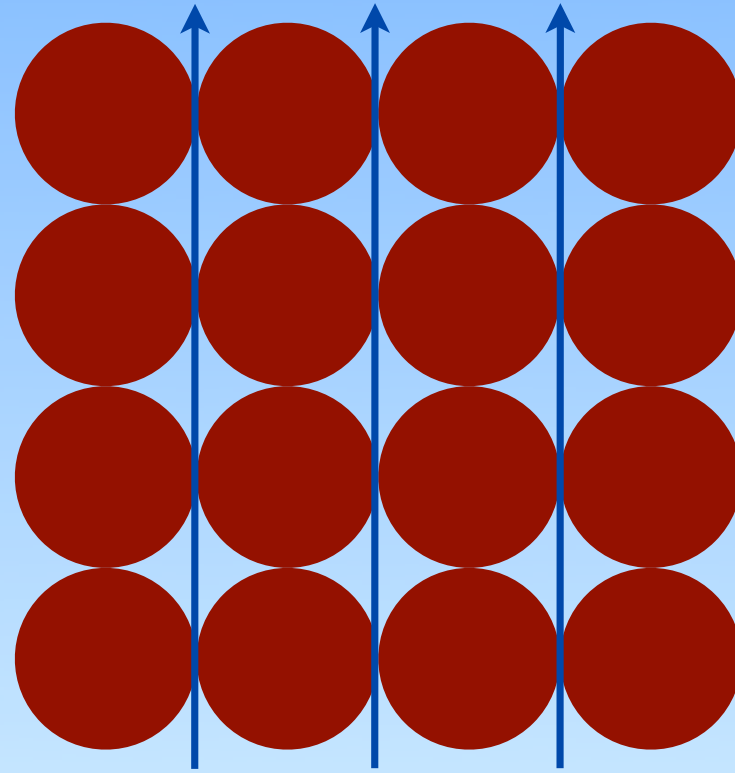
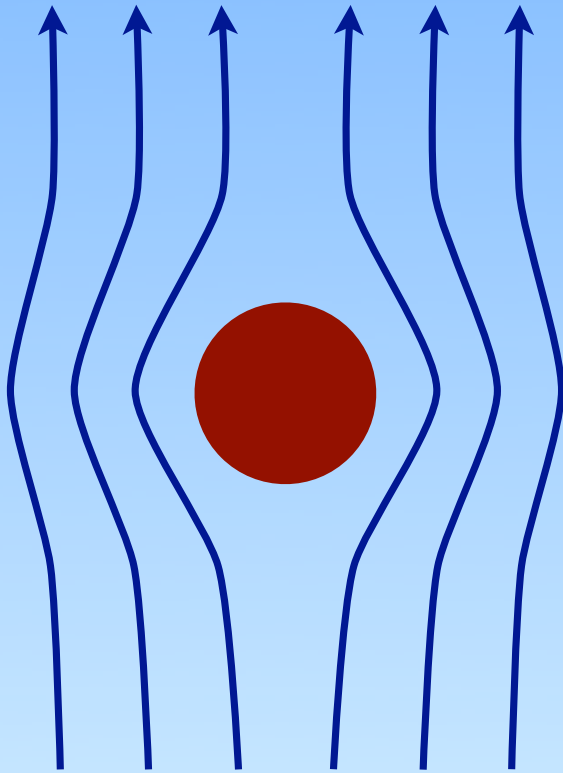
$$B_p \equiv \frac{F_{f \rightarrow s}}{F_g} \approx 40 \frac{18\eta V}{\rho_p g d^2}$$

$$B_p \approx 1 \rightarrow d \approx \sqrt{40} \sqrt{\frac{18\eta V}{\rho_p g}}$$

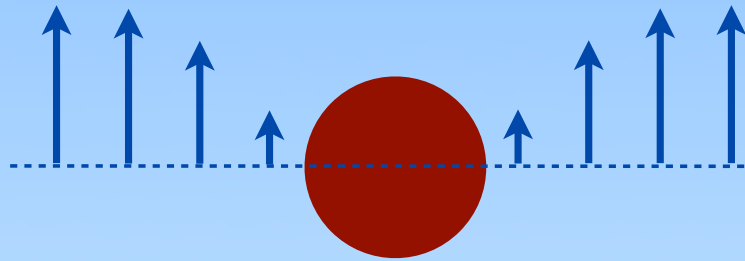
$$V \approx 1 \text{ m/s} \rightarrow d \approx 760 \text{ } \mu\text{m}$$

$$V \approx \sqrt{2gd} \rightarrow d \approx 190 \text{ } \mu\text{m}$$

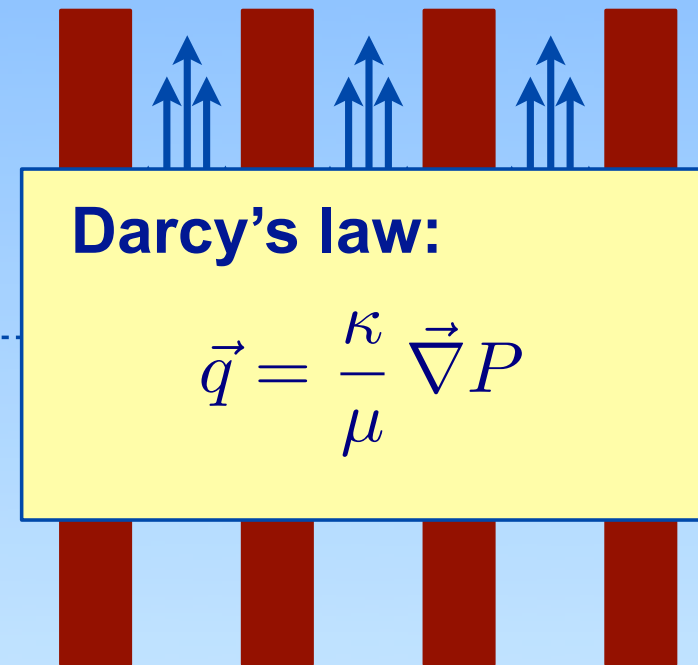
Why this difference?



Why this difference?

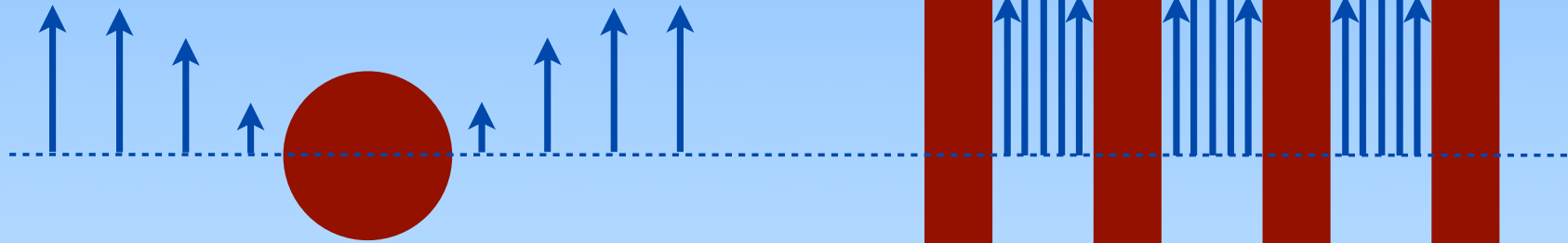


- ▶ space around sphere
- ▶ moderate shear rate and shear stress



- ▶ narrow channels
- ▶ large shear rate and shear stress

Why this difference?



- ▶ **space around sphere**
- ▶ **moderate shear rate and shear stress**

- ▶ **narrow channels**
- ▶ **large shear rate and shear stress**

III

Example 1

**When air is forced
through a granular layer**

Faraday heaping

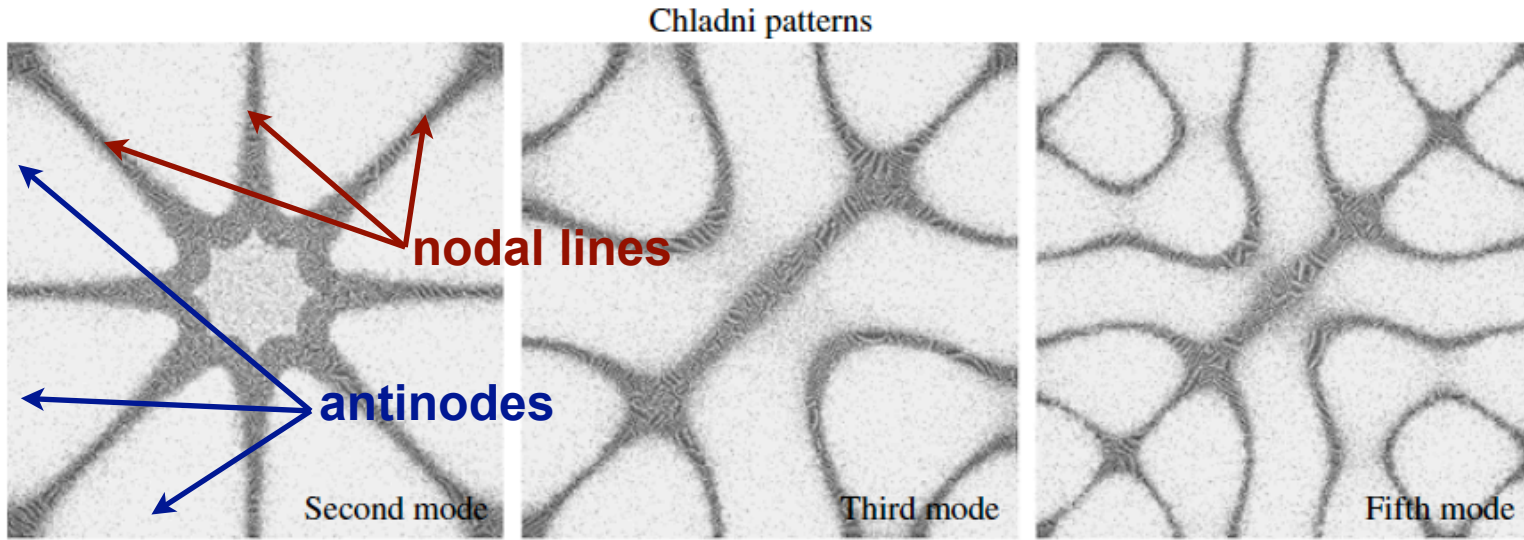
... goes back all the way to
Michael Faraday

M. Faraday, *On a peculiar class of acoustical figures;
and on certain forms assumed by groups of particles
upon vibrating elastic surfaces*,
Philos. Trans. R. Soc. London **52**, 299 (1831).

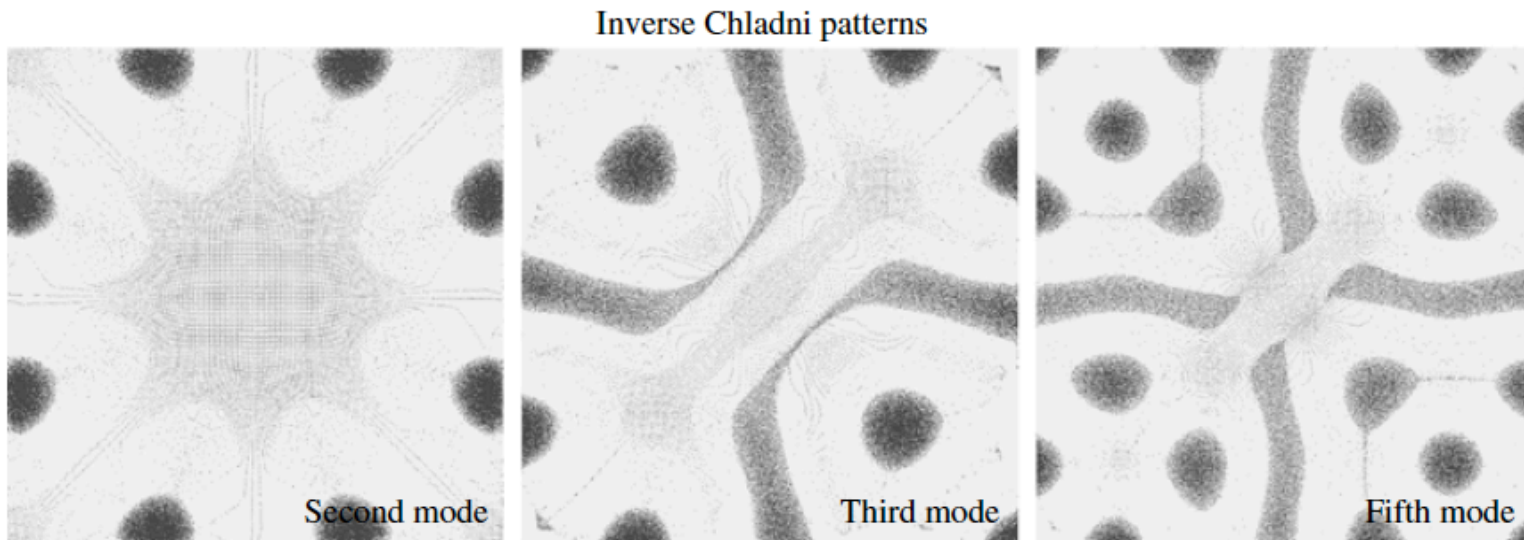


Not: Chladni patterns

without air



with air



Faraday heaping

23.52000 s

Particle diameter: 0.5 mm

Width of box: 10 cm

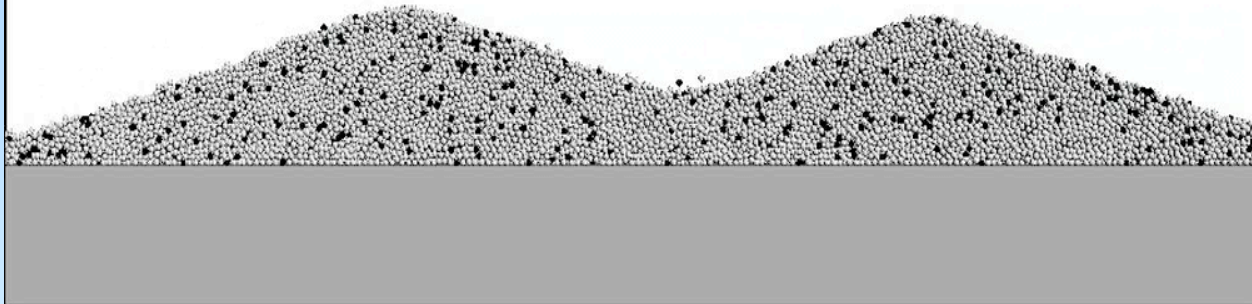
Number of particles: 13500

Vibration frequency: 6.25 Hz

Vibration amplitude: 1.0 cm

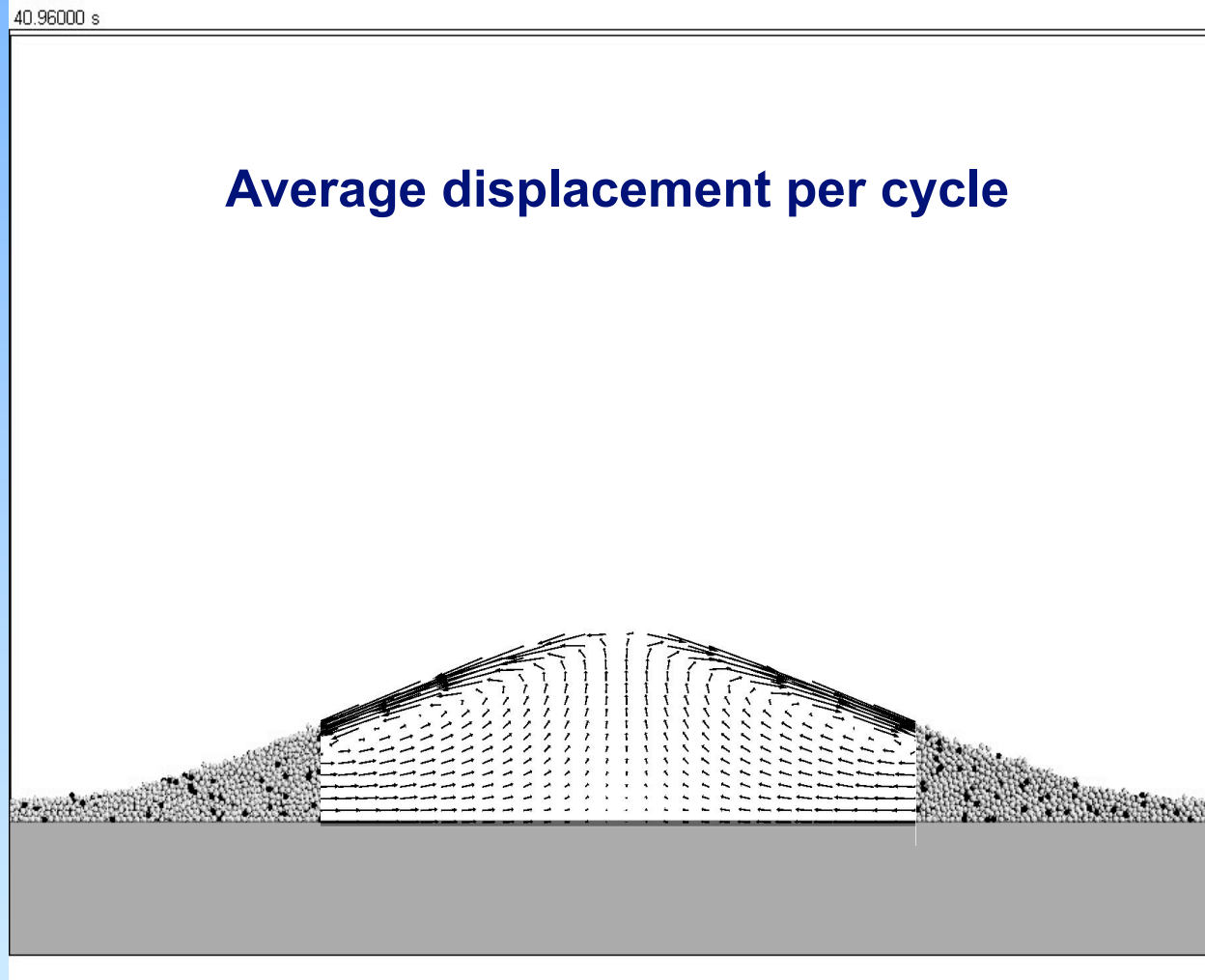
Maximum acceleration: 1.6 g

Number of CFD elements: 80 x 60 x 1



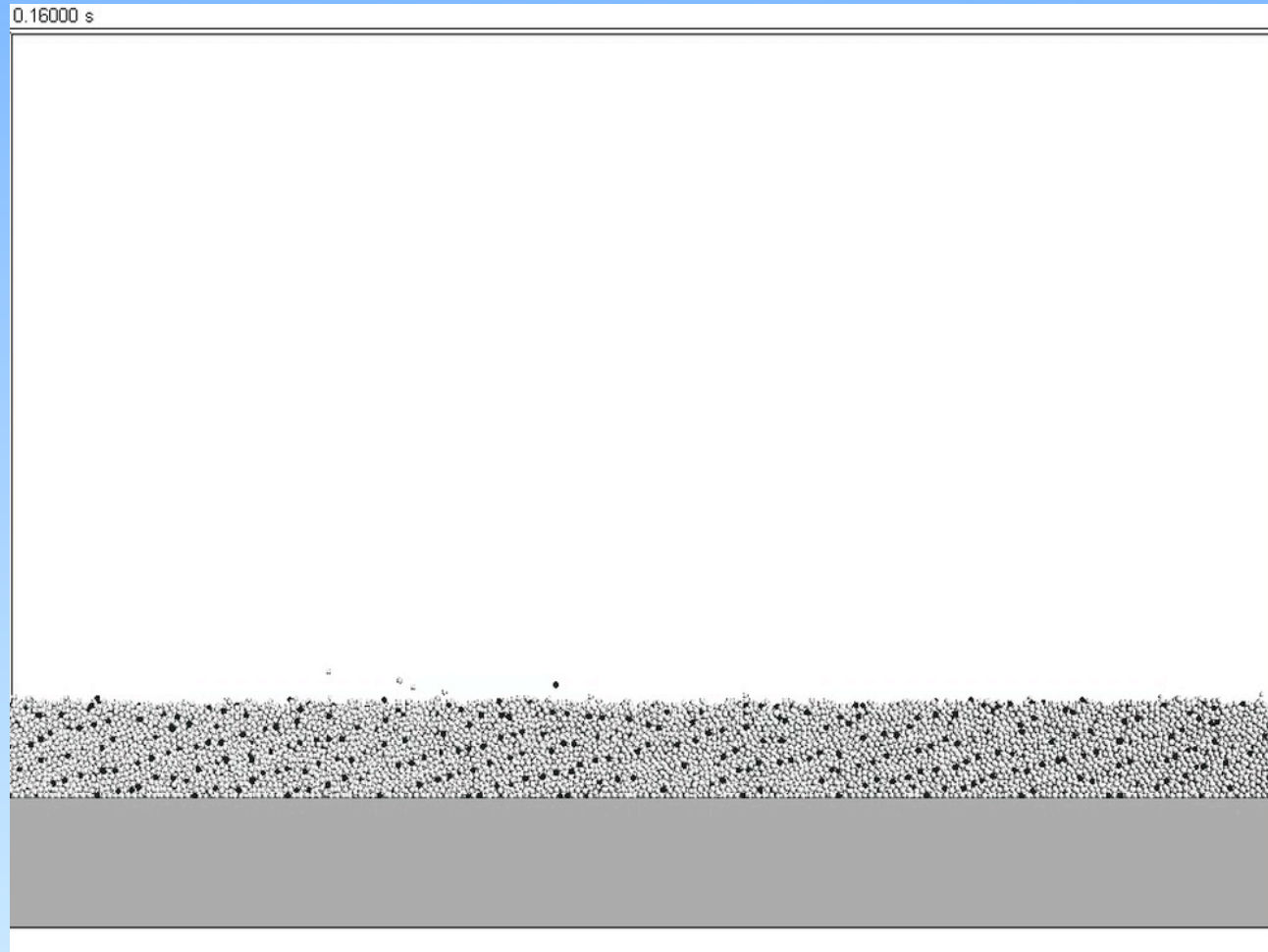
Numerical simulation of heaping with a hybrid GD-CFD code

Faraday heaping



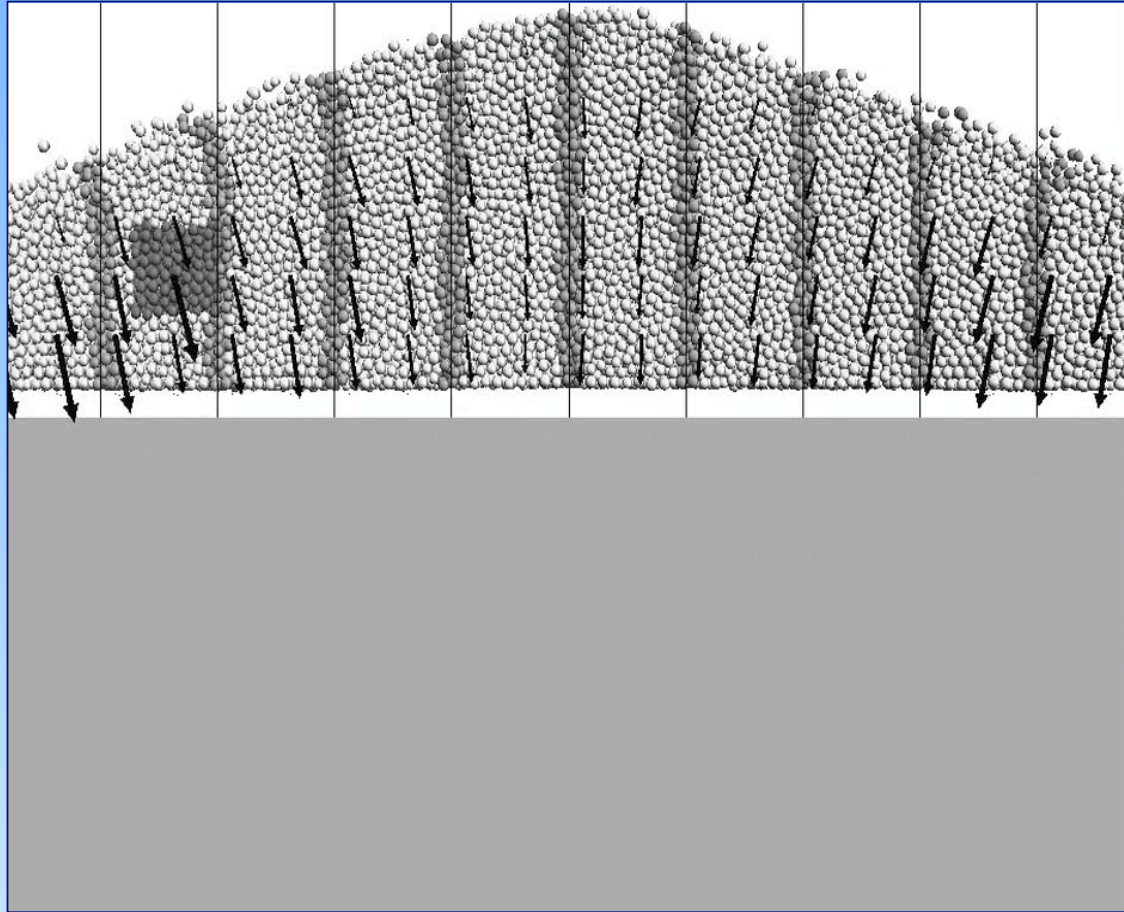
Numerical simulation of heaping with a hybrid GD-CFD code

Without air...



... there is no heap !

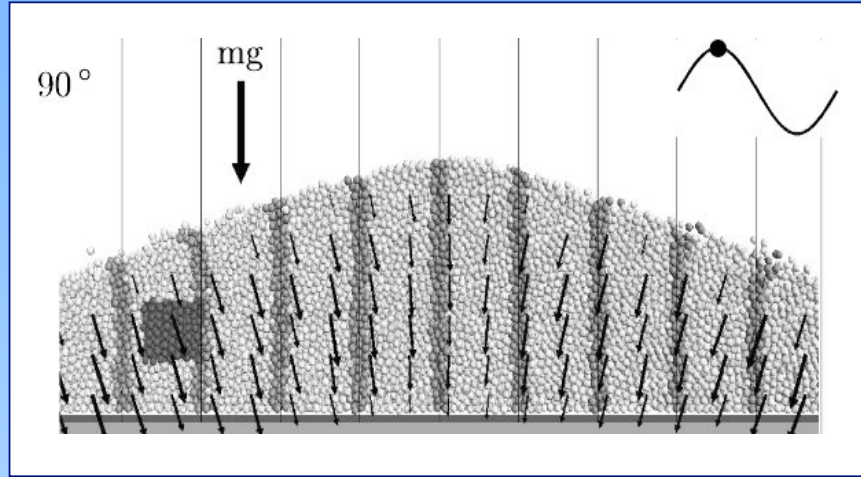
Steady state



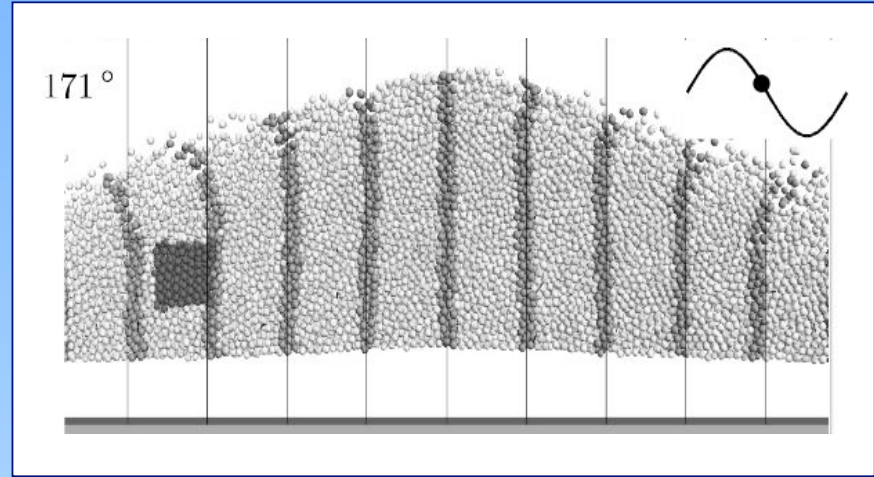
arrows = air drag on particles

But why does the bulk only move inwards ?

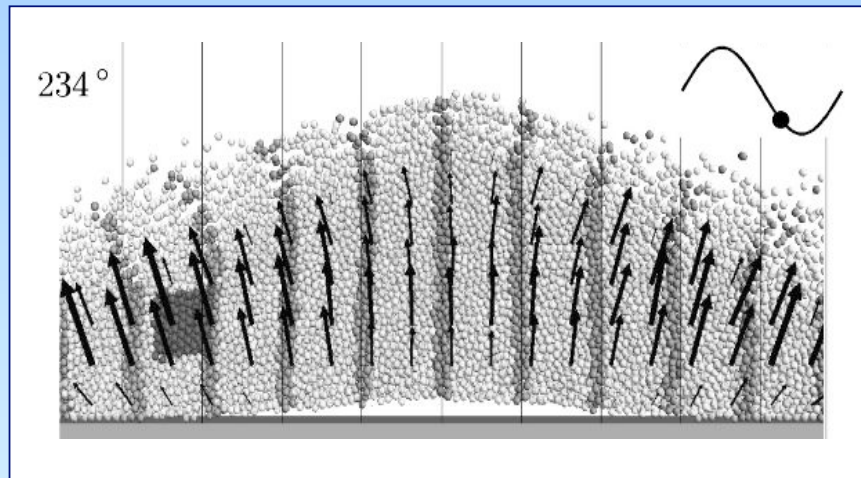
4 snapshots



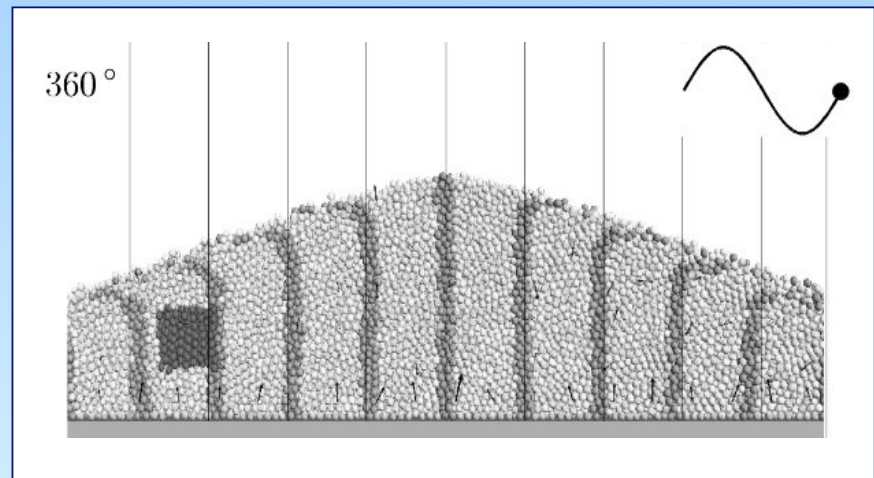
inward drag, loose packing



no drag, loose packing

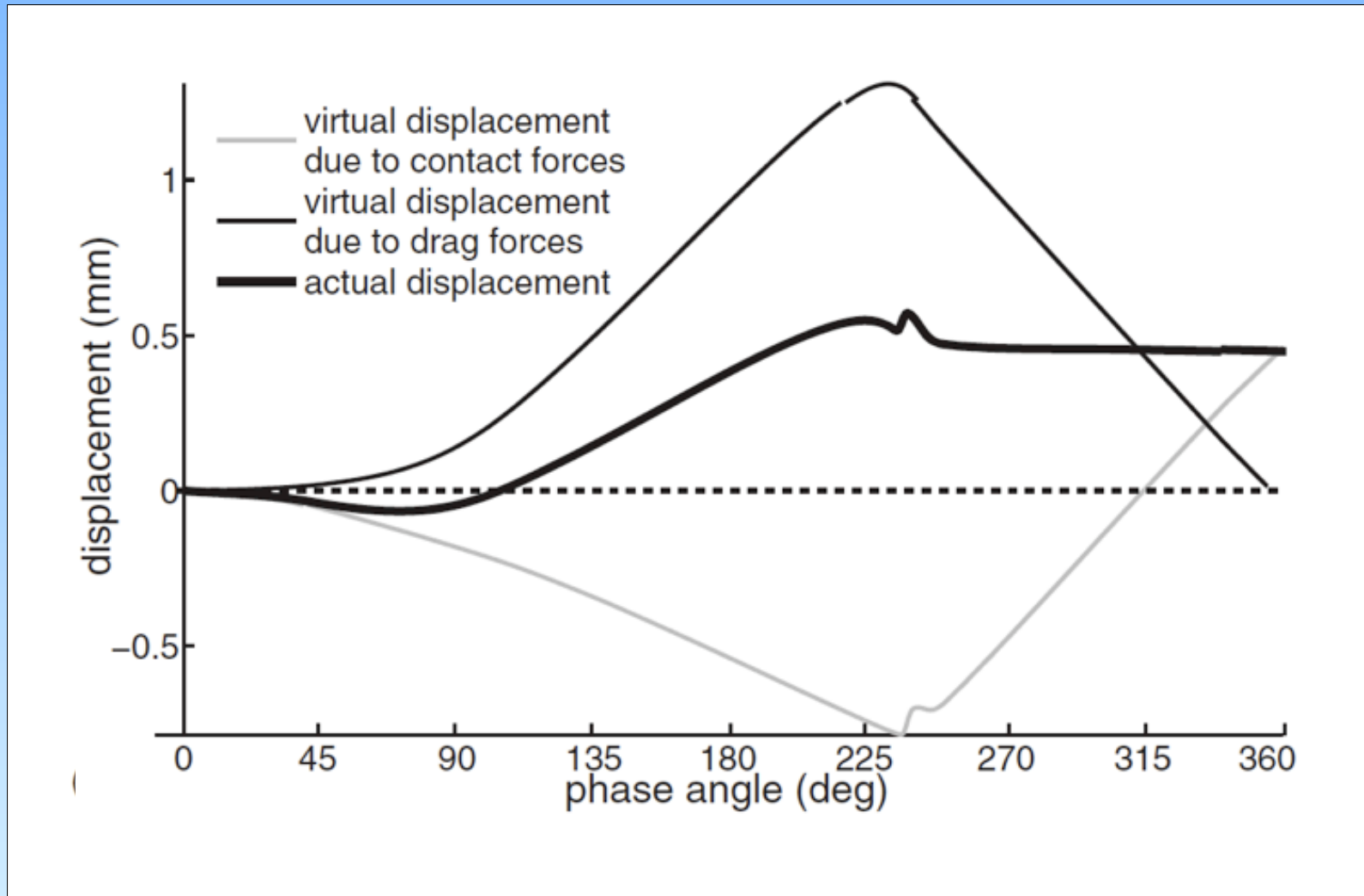


outward drag, dense packing

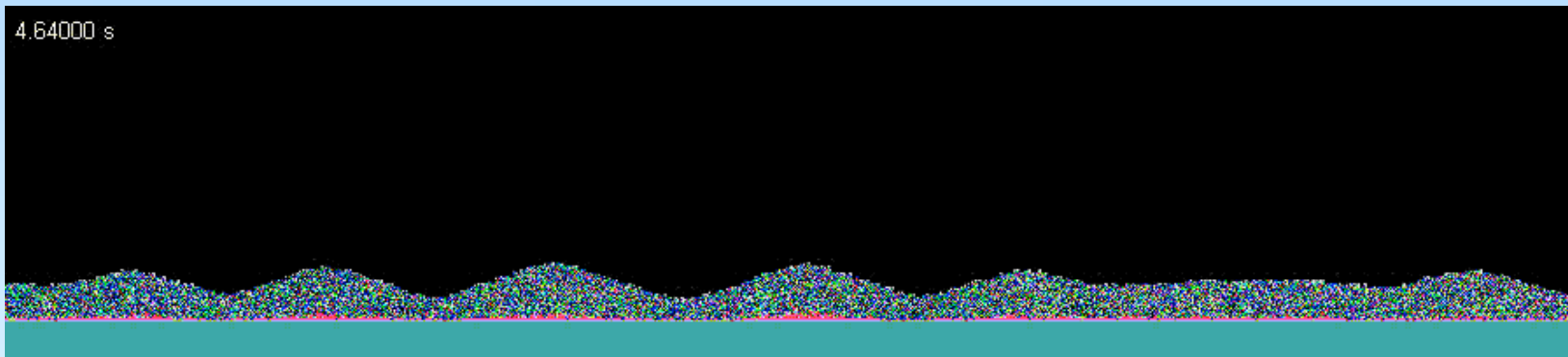
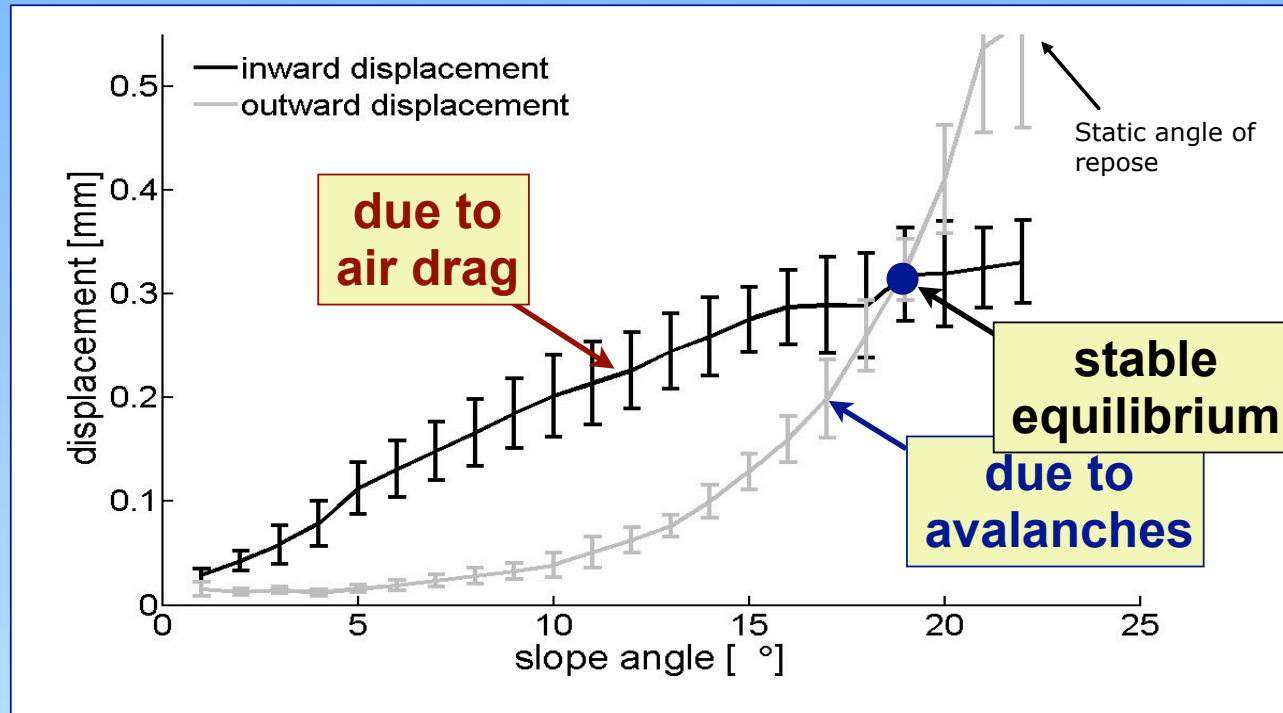


no drag, dense packing

Force analysis (x-direction)



How does heaping start ?



$t=6.24$ s

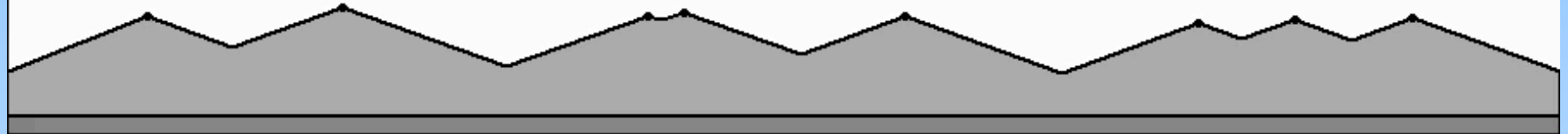
experimental result



simulation result



model result



t=4.00 s

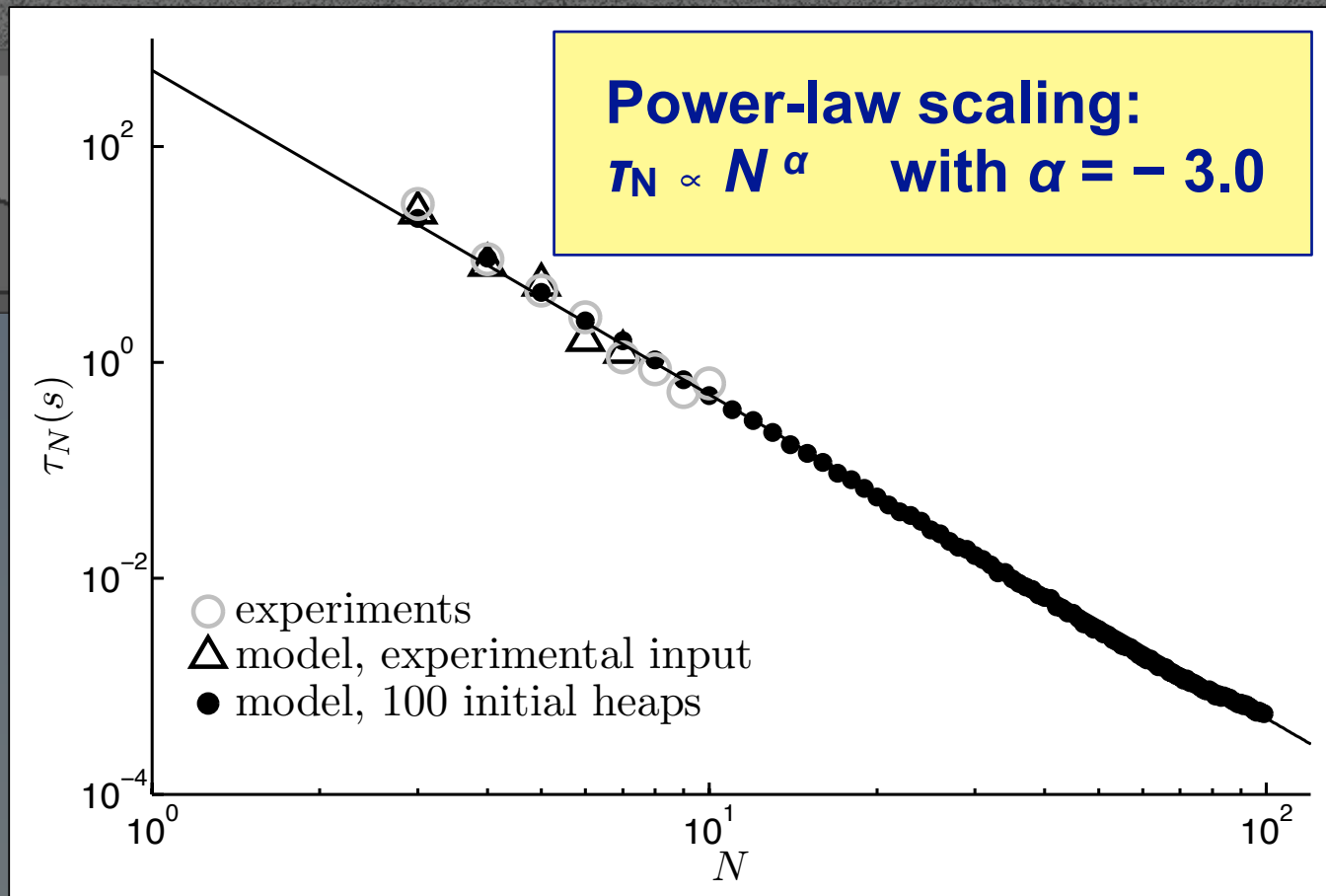
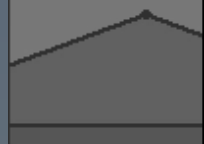
experimental result



simulation result



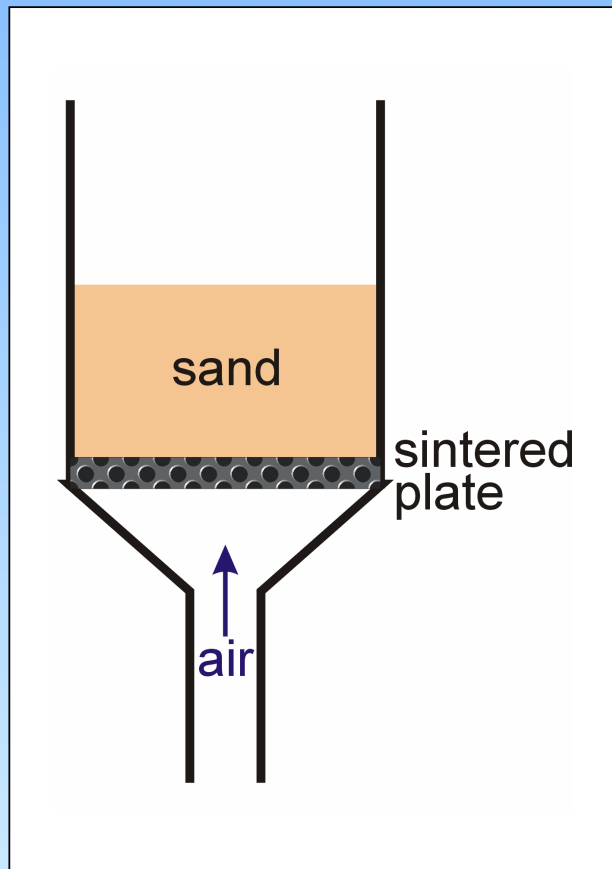
model result



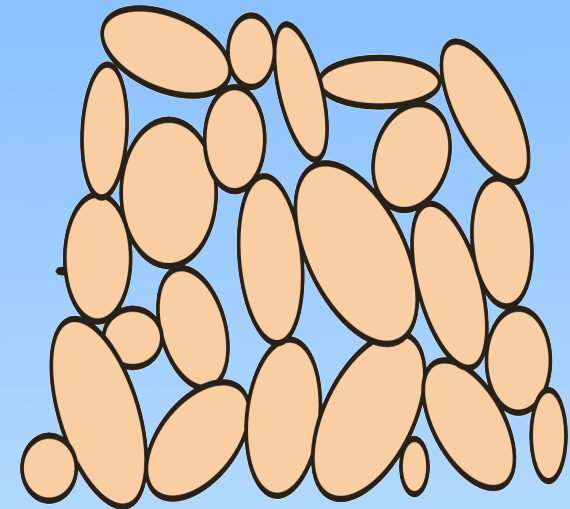
Example 2

**The influence of air on
drag in a granular bed**

Preparing the sand



turn
off
air

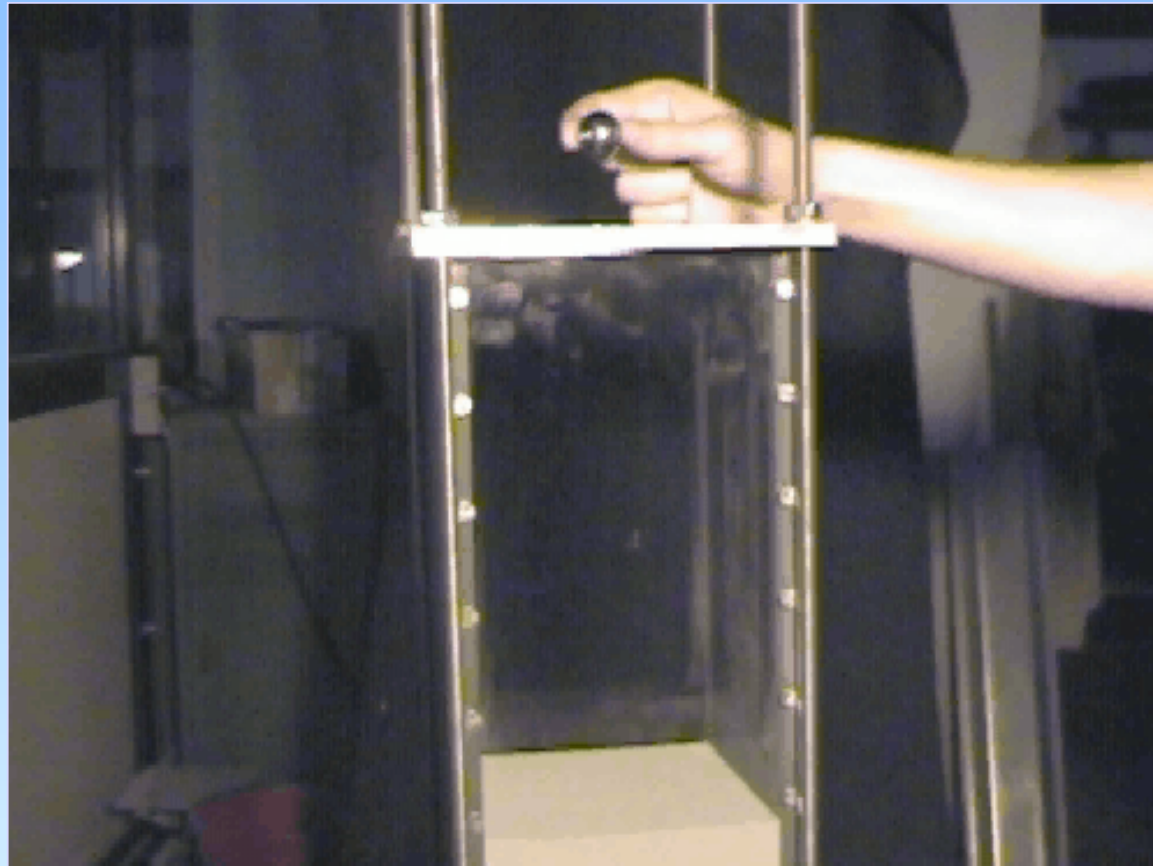


very loose
packing:

solid fraction
= 41 %

Controlled experiments

Ball dropped on **decompactified**, very fine sand

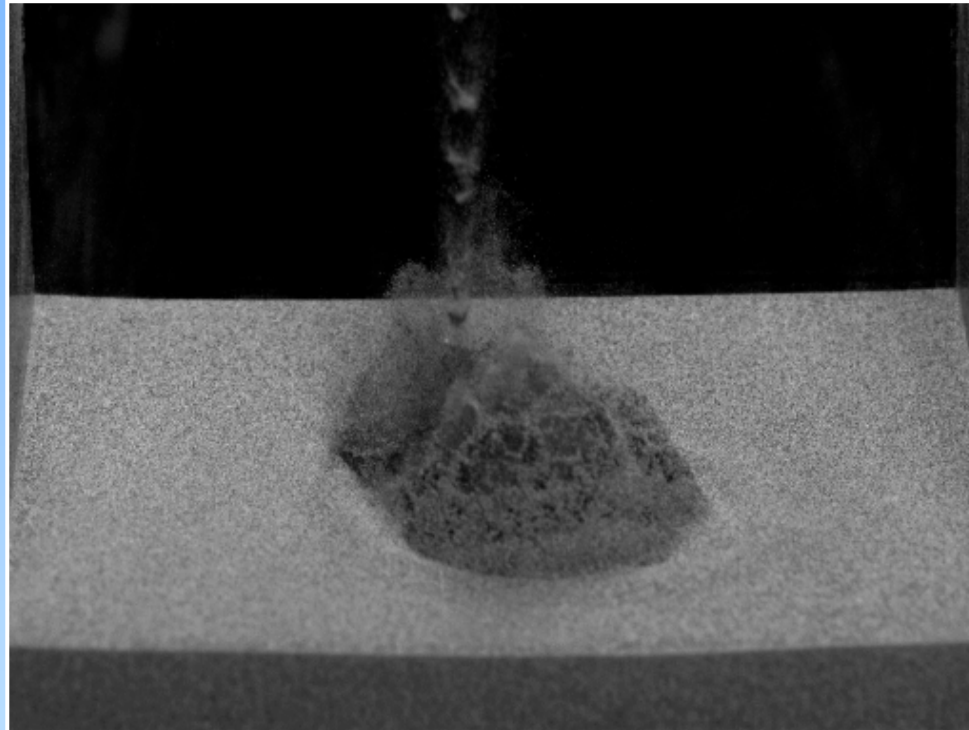


Controlled experiments

Ball dropped on **decompactified**, very fine sand



Ball impact on sand



3 events:

- Impact creates splash

- A jet is formed

- Granular eruption

**Mechanism similar to
disk impact on water**





Disk impact on water (side view)

$$V_{\text{impact}} \approx 1.0 \text{ m/s}$$

$$R_{\text{disk}} = 0.03 \text{ m}$$



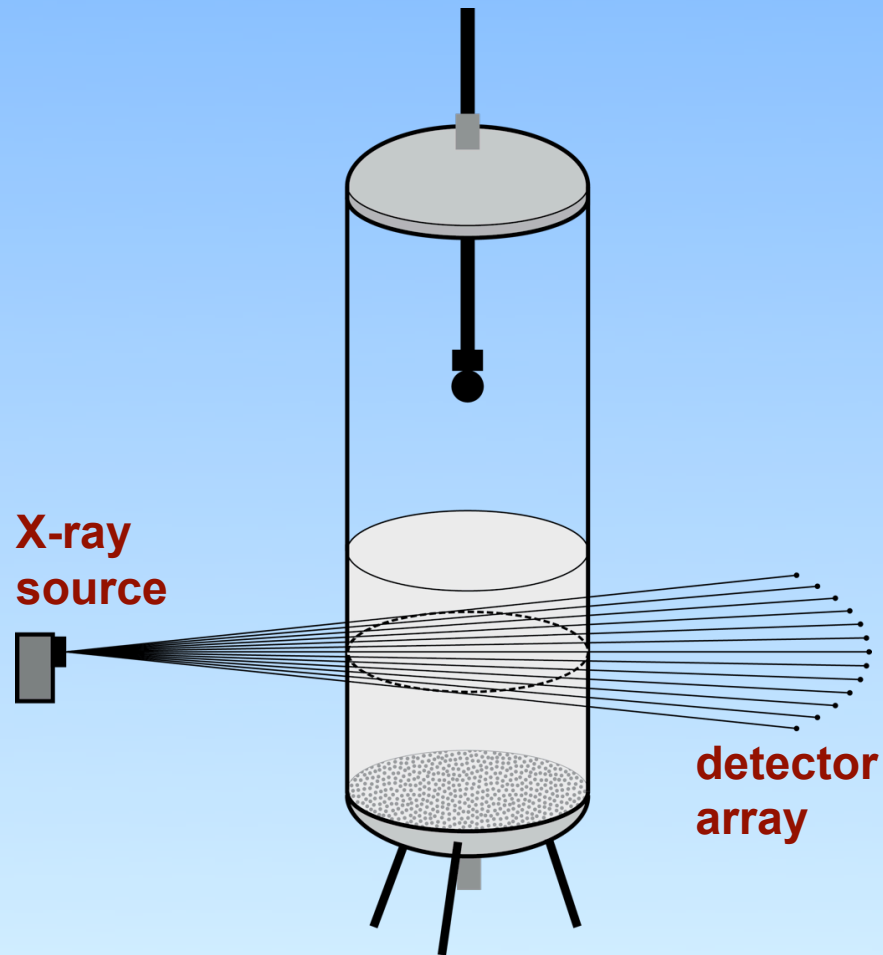
Bergmann, DvdM, Stijnman, Sandtke, Prosperetti,
Lohse, Phys. Rev. Lett. **96**, 154505 (2006)

Gekle, Peters, Gordillo, DvdM, Lohse,
Phys. Rev. Lett. **104**, 024501 (2010)

Fr=92 | 892.4 ms

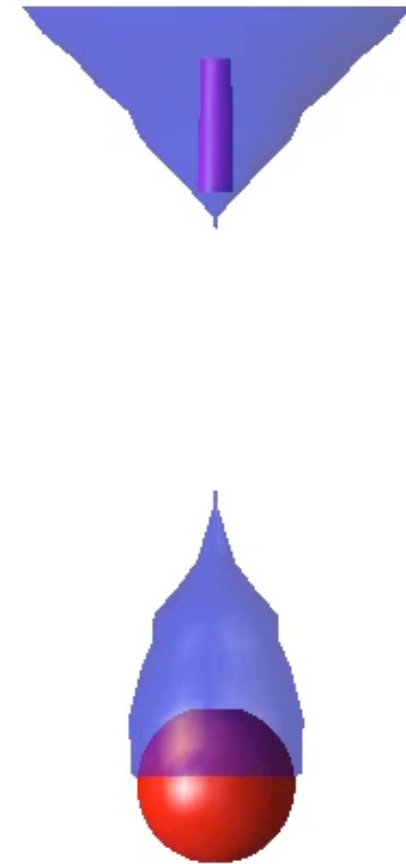


X-ray imaging: Measuring jet formation



X-ray
source

detector
array



reconstruction

Rob Mudde, TUD

What is the role of air in granular jet formation ?

Royer, Corwin, Flior, Cordero,
Rivers, Eng, and Jaeger,
Nature Physics 1, 164 (2005).

Caballero-Robledo, Bergmann,
DvdM, Prosperetti, and Lohse,
Phys. Rev. Lett. 99, 018001 (2007)

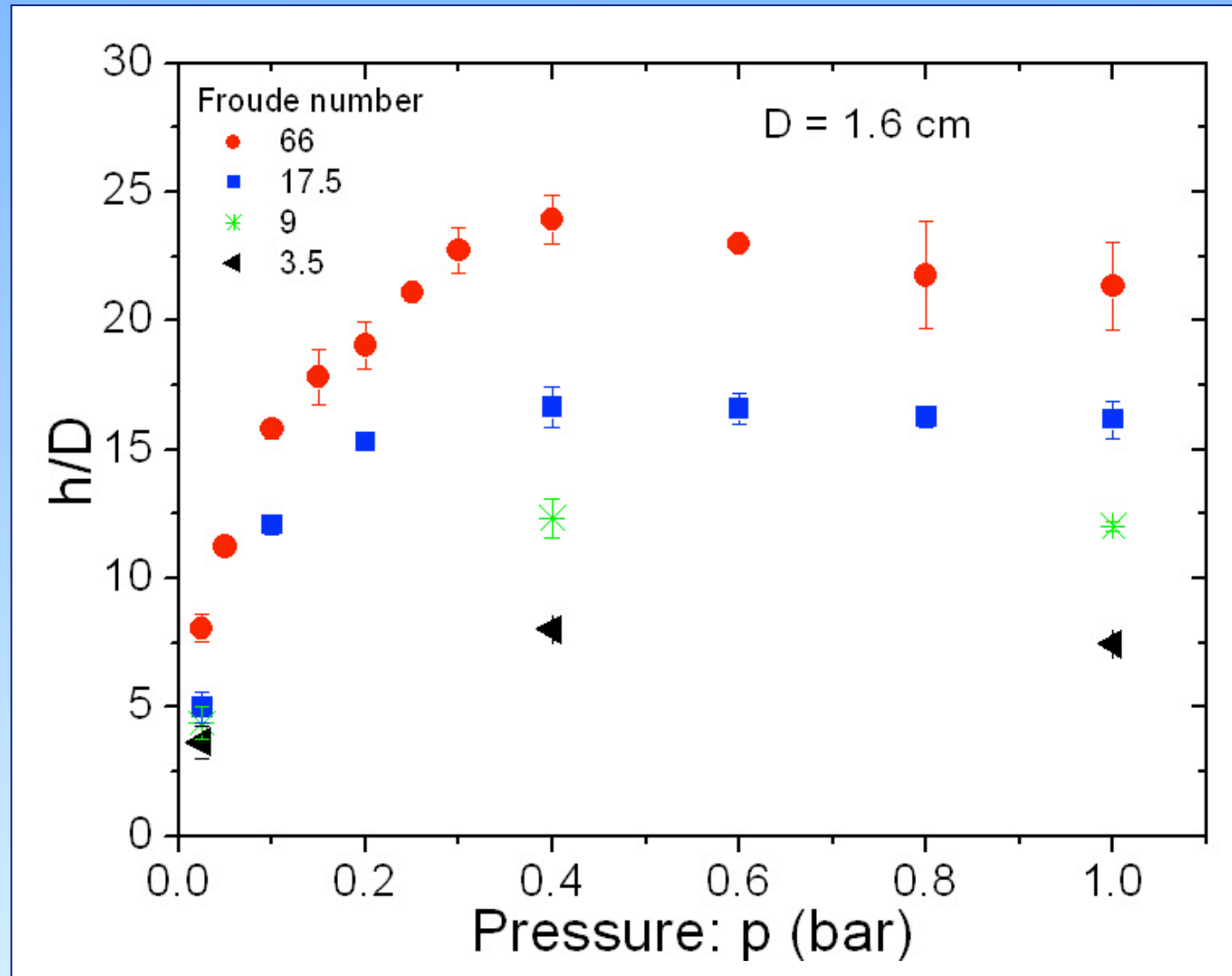


25 mbar



1 bar

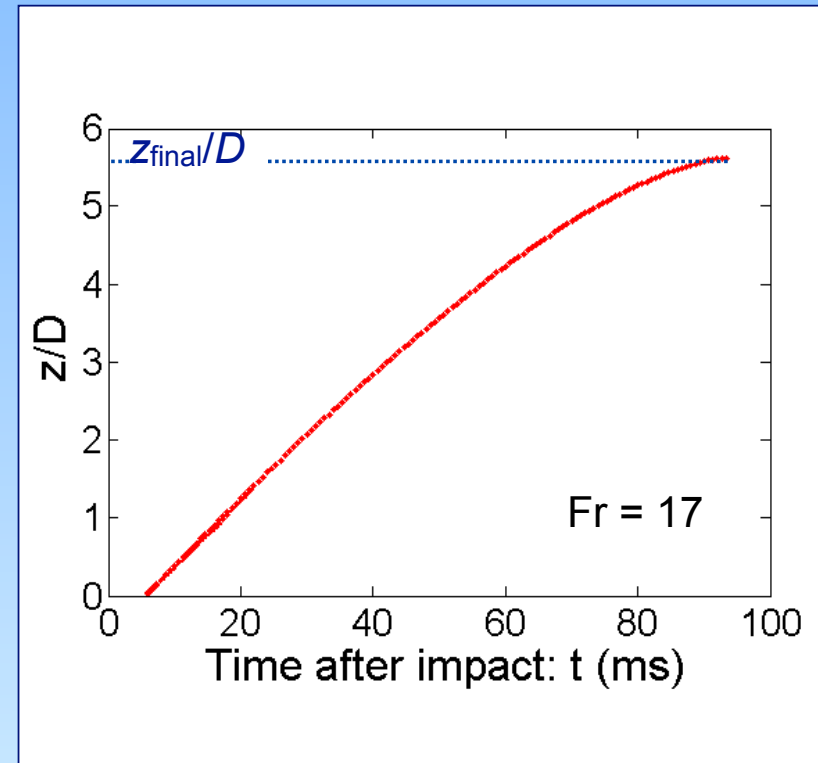
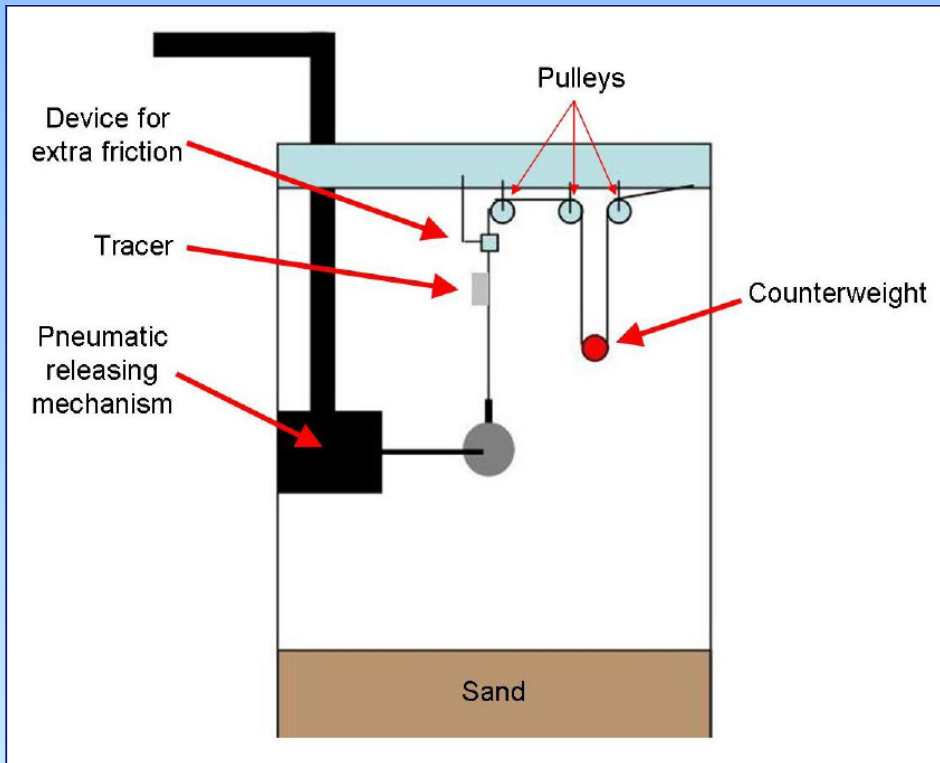
Jet height vs. pressure



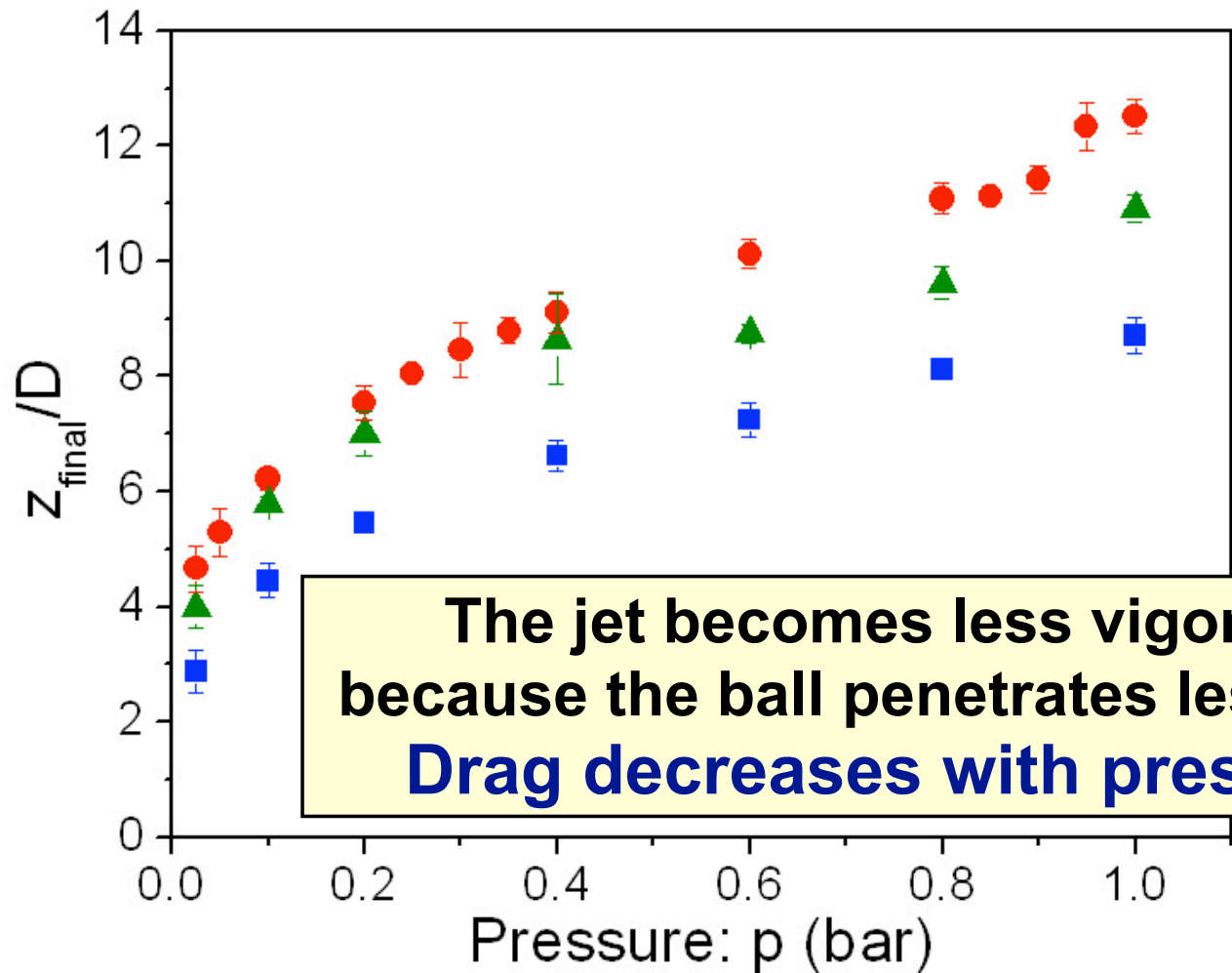
**Froude
number:**

$$Fr \equiv \frac{U^2}{gD}$$

Trajectories in the sand



Final depth vs. pressure

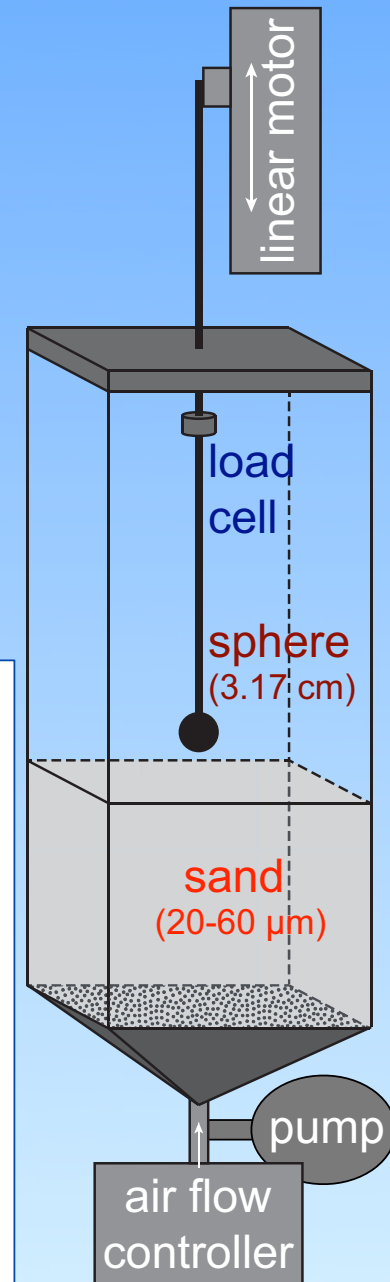


The jet becomes less vigorous
because the ball penetrates less deep
Drag decreases with pressure

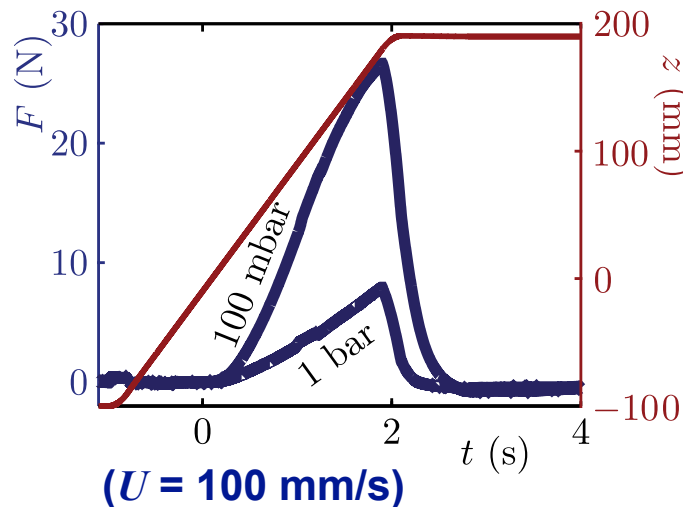
Directly measuring drag:

Modified penetrometer

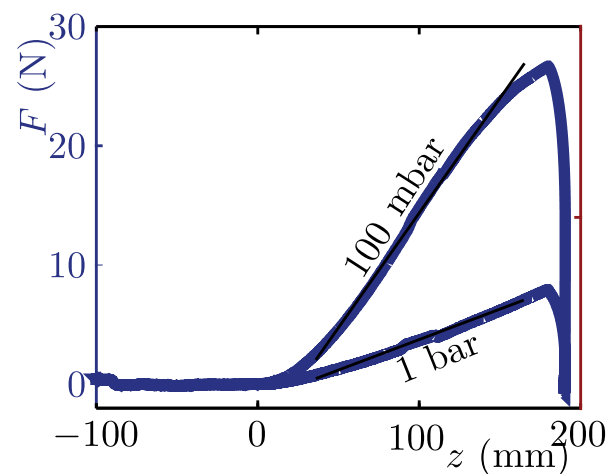
- ▶ linear motor controls velocity U
- ▶ load cell measures drag F directly
- ▶ pump controls ambient pressure P_0



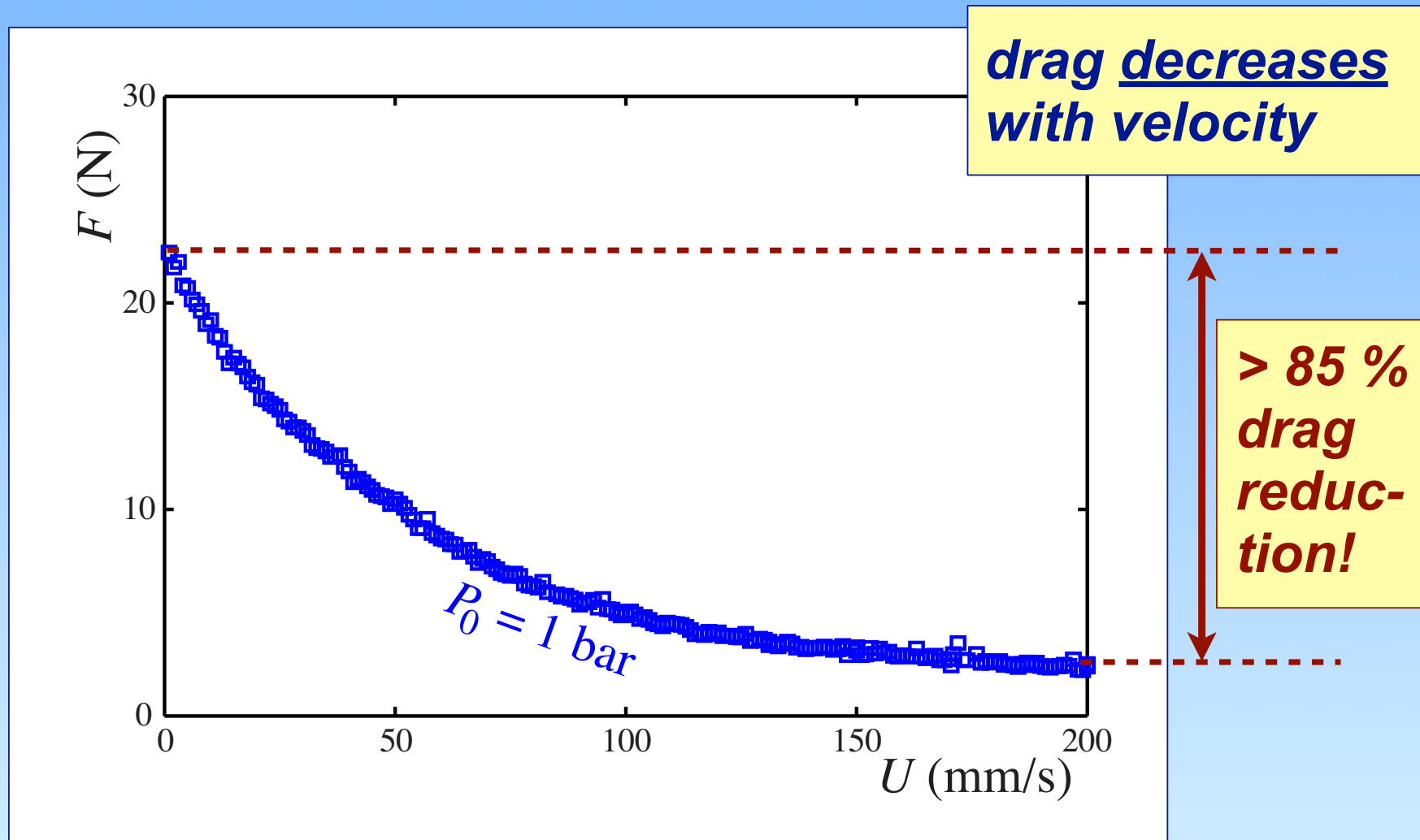
drag vs time



drag vs position

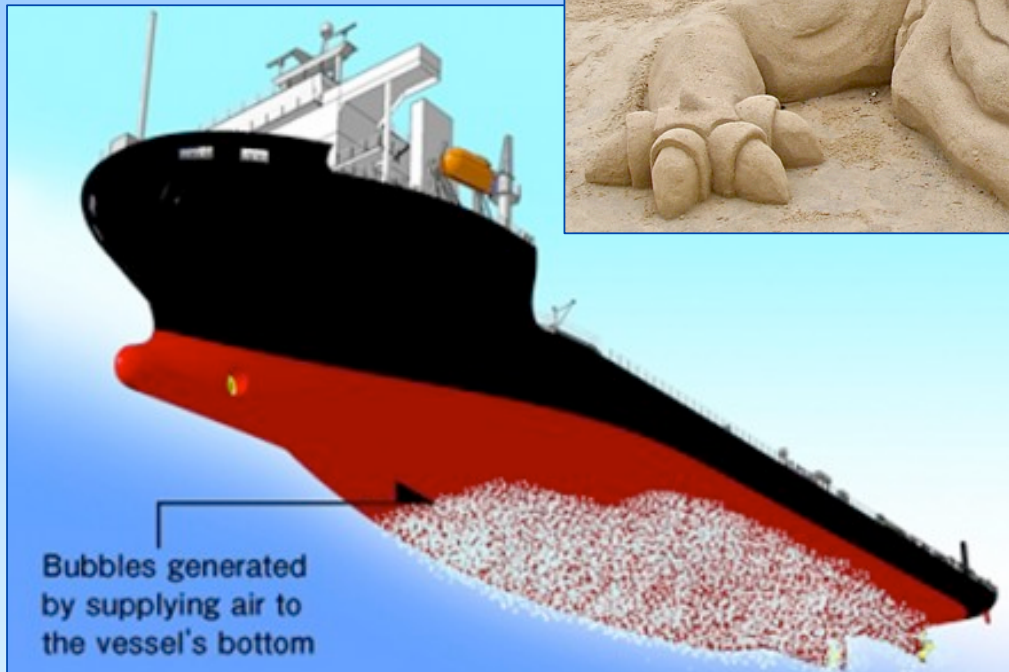


Drag F versus velocity U ($P_0 = 1$ bar)



(drag F measured at $z = 10$ cm below surface)

Drag reduction in literature

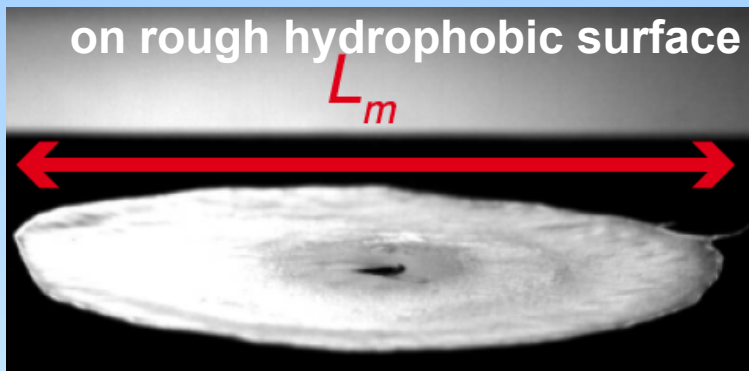
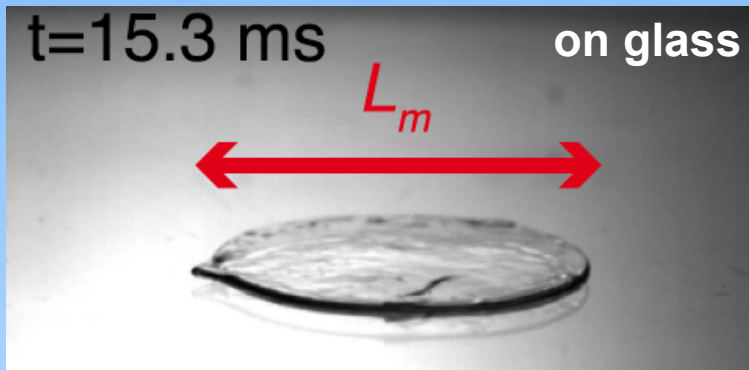


Bubbles generated
by supplying air to
the vessel's bottom

***drag reduction
≈ 5 % to 30 %***

Drag reduction in literature

Impact Carbopol droplet



drag reduction $\approx 85\%$

Luu, Forterre,
Phys. Rev. Lett. 110, 184501 (2013).

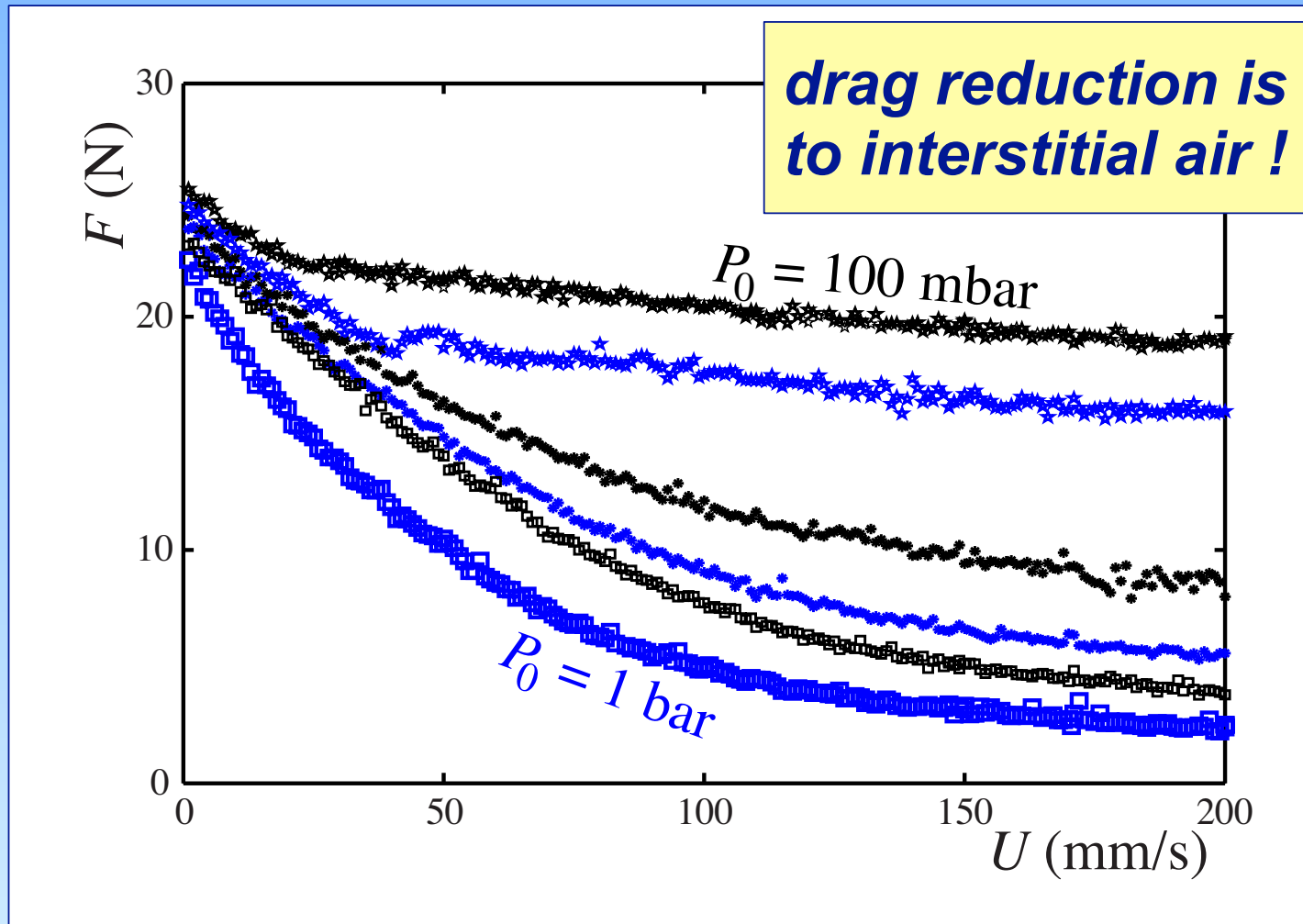
Impact heated sphere



drag reduction $\geq 85\%$

Vakarelski, Marston, Chan, Thoroddsen,
Phys. Rev. Lett. 106, 214501 (2011).

Drag F versus velocity U ($P_0 \leq 1$ bar)



(drag F measured at $z = 10$ cm below surface)

Model

assumption:

air modifies the contact forces between grains.

drag without air:

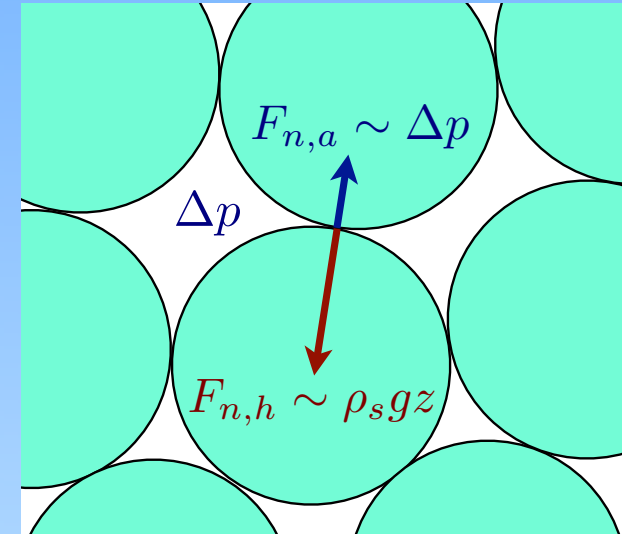
grains perform work against contact forces \sim hydrostatic pressure $\rho_s g z$

$$\frac{F}{\rho_s g z D^2} = f$$

drag with air:

excess air pressure ΔP works against hydrostatic pressure and therefore decreases the contact forces

$$\frac{F}{\rho_s g z D^2} = f \left(\frac{\Delta P}{\rho_s g z} \right)$$



**Problem:
 $f()$ is unknown**

What determines ΔP ?

Time evolution of the excess pressure:

$$\frac{d\Delta P}{dt} =$$

$$\alpha \frac{P_0 U}{D}$$

–

$$\beta \frac{P_0}{\eta} \Delta P$$

$$\eta = \frac{\mu D^2}{\kappa}$$

$$\approx 4.5 \cdot 10^4 \text{ Pa s}$$

increase due to compressional compaction

decrease due to Darcy flow inside the sand

For constant U this linear ODE is directly solved ($t = z/U$):

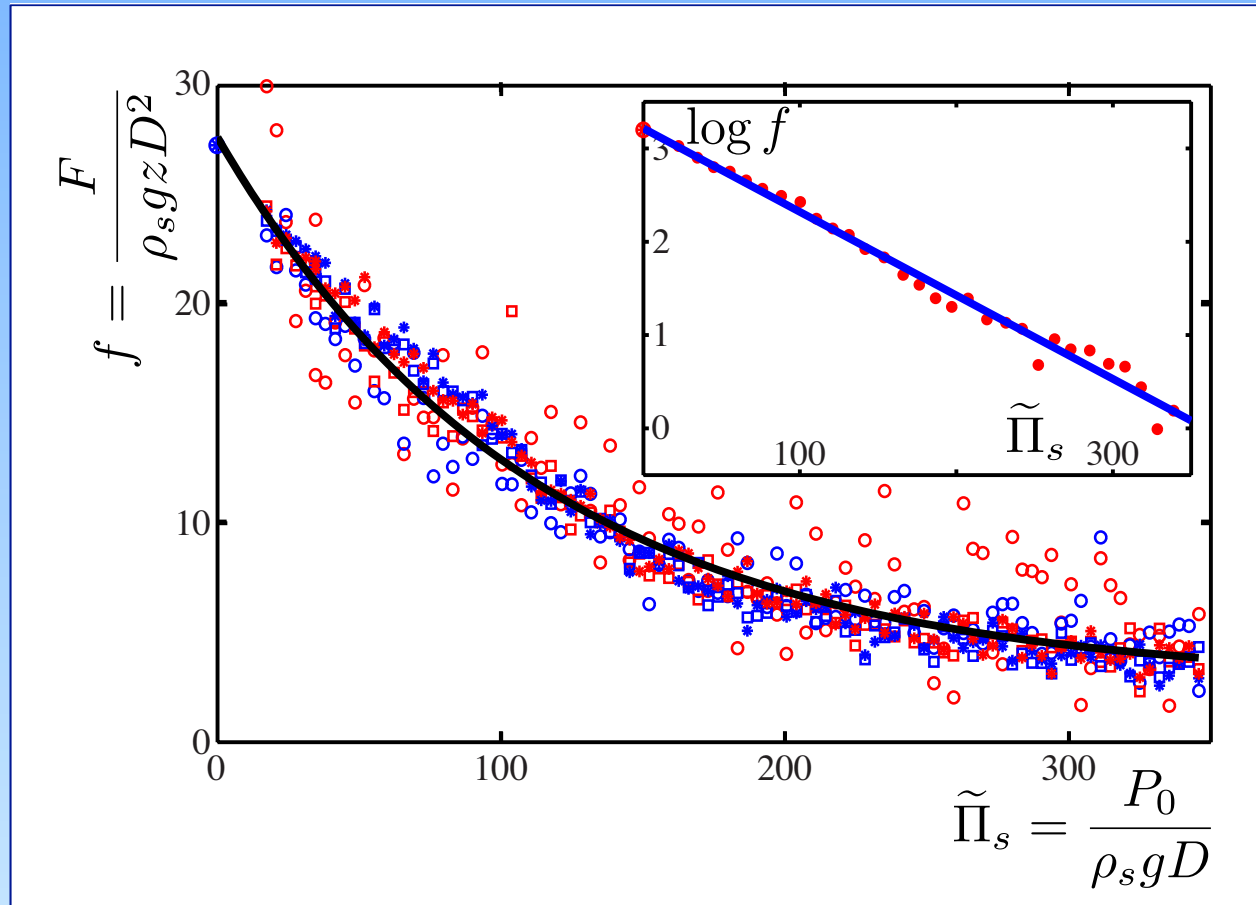
$$\tilde{\Pi} = \frac{\Delta P}{\alpha \rho_s g z} = \frac{1}{\beta} \frac{\eta U}{\rho_s g D z} \left[1 - \exp \left(-\beta \frac{P_0}{\eta U} z \right) \right]$$

which in the limit of large U becomes constant (z -independent):

$$\tilde{\Pi} \rightarrow \tilde{\Pi}_s = \frac{P_0}{\rho_s g D}$$

Can we use this to determine $f()$?

Drag F versus pressure P_0 ($U=200$ mm/s)



Calculate $\tilde{\Pi}_s$ from P_0 and f from F in this limit of large U

Fit to functional form: $f(\tilde{\Pi}) = f_s + f_0 \exp(-\tilde{\Pi}/\tilde{\Pi}_0)$

model v

Turn back to the time ev

$$\tilde{\Pi} = \frac{\Delta P}{\alpha \rho_s g z} = \frac{1}{\beta}$$

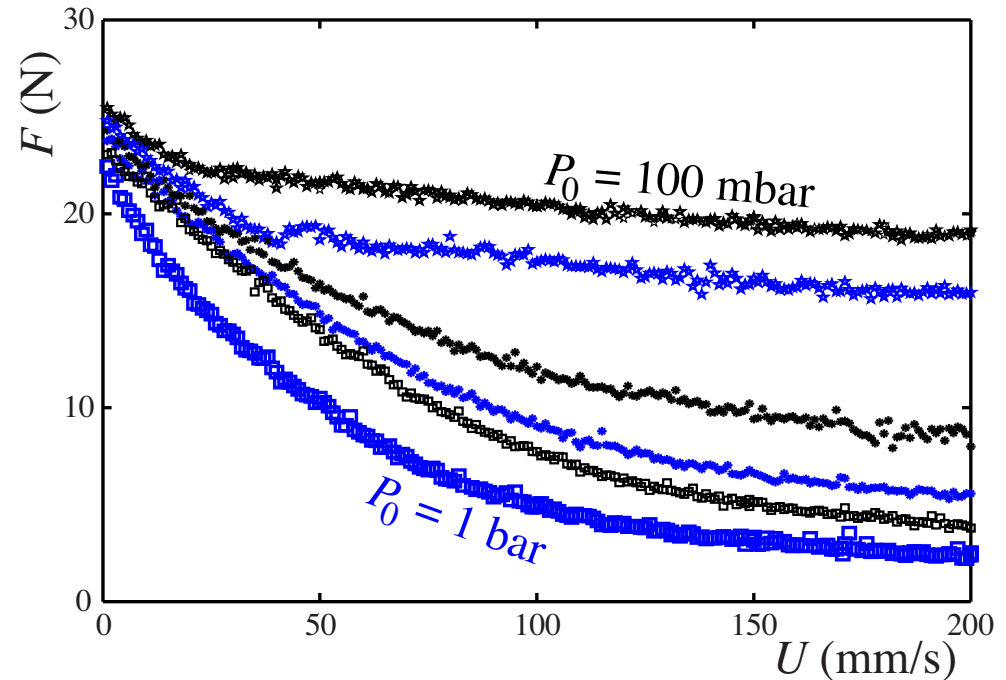
For all of our $F(z, U, P_0)$ da

$$\zeta = \frac{P_0 z}{\eta U}$$

$$\tilde{\Pi}^* = \frac{\rho_s g D}{P_0} \tilde{\Pi}$$

which turns the equation into:

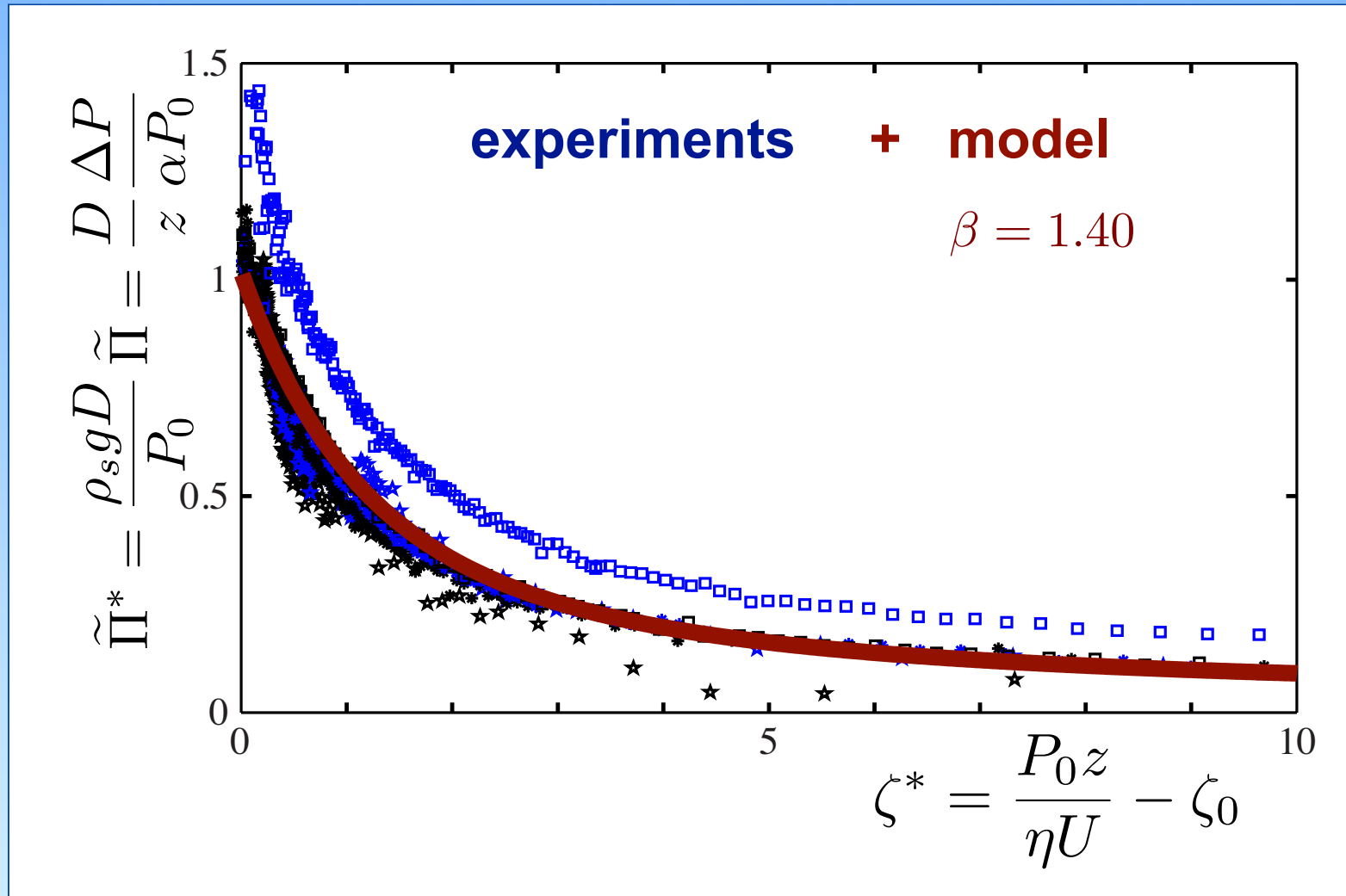
$$\tilde{\Pi}^* = \frac{[1 - \exp(-\beta \zeta)]}{\beta \zeta}$$



with $\tilde{\Pi}$ determined from the dimensionless drag force f by inverting $f(\tilde{\Pi})$.

Does this single parameter equation fit the data?

comparison



Winter

Granular matter and water

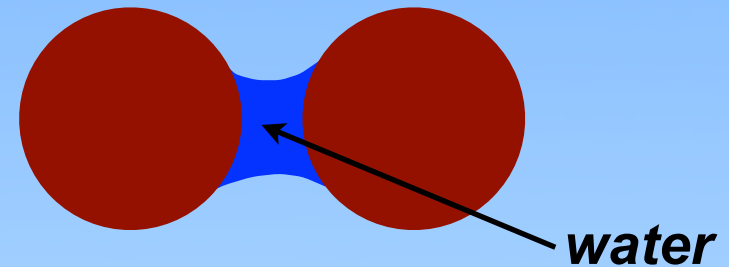
Wet granular matter



*little liquid,
much particles*

**liquid consolidates
granular material**

capillary bridges



$$F_{cap} \sim F_g$$

$$\sigma \pi d \sim \frac{1}{6} \pi d^3 \rho g$$

$$d \sim \sqrt{\frac{6\sigma}{\rho g}} \approx 4 \text{ mm}$$

$$\frac{F_{cap}}{F_g} \sim \frac{1}{d^2}$$

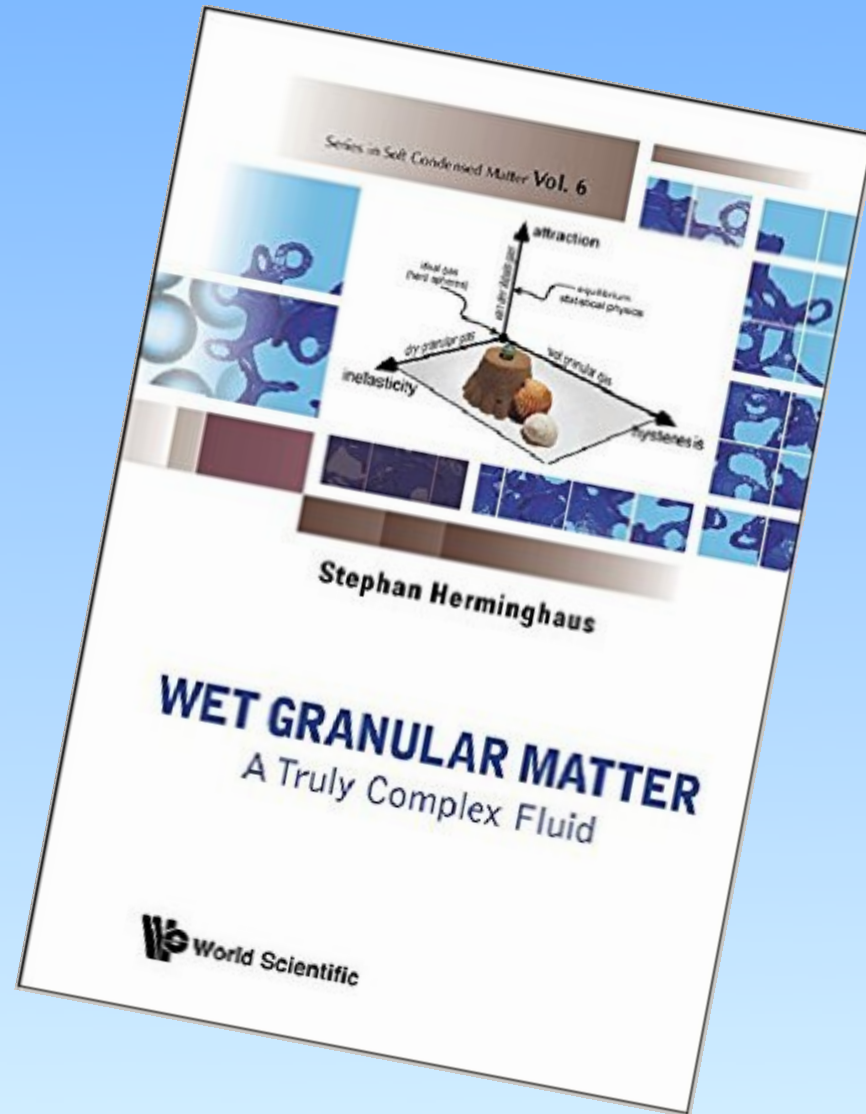
Granular matter and water

Wet granular matter



*little liquid,
much particles*

liquid consolidates
granular material



Granular matter and water

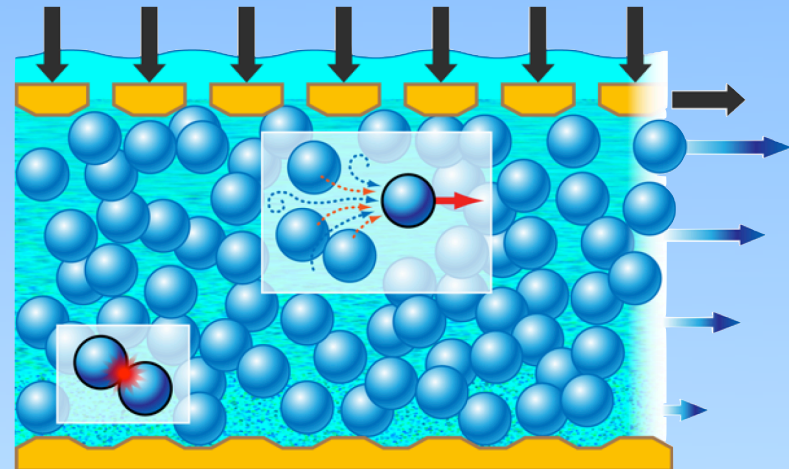
Wet granular matter



*little liquid,
much particles*

liquid consolidates
granular material

Suspension



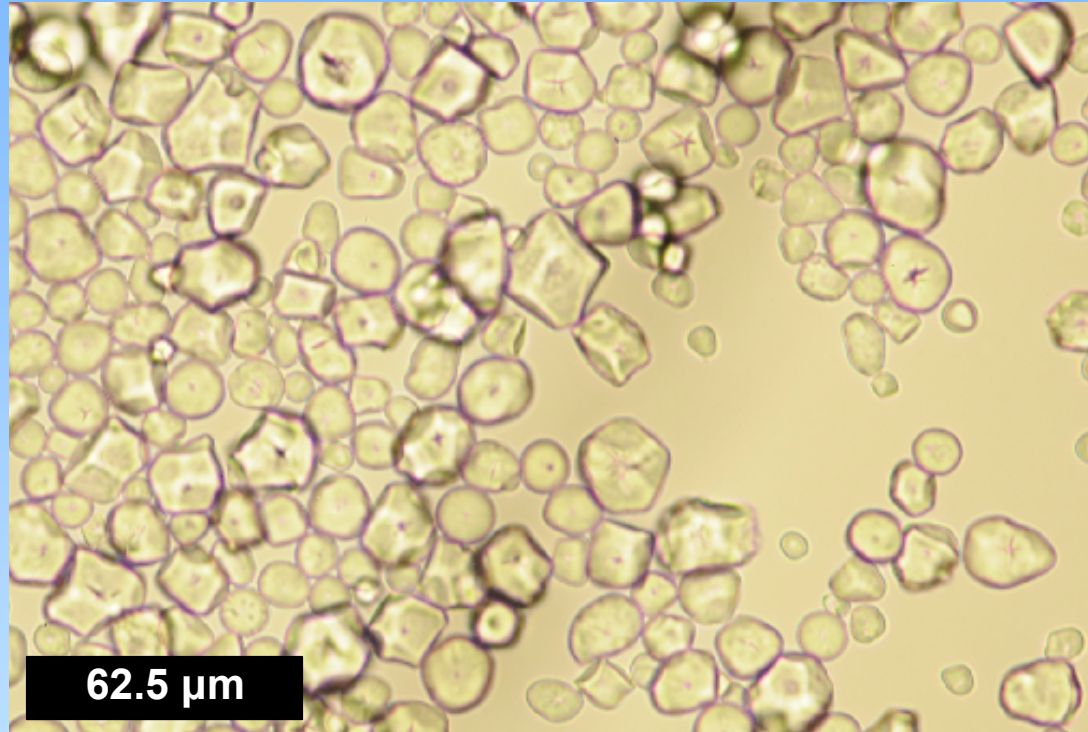
*much liquid,
few particles*

particles determine
suspension rheology

**equal amount
of liquid and
grains**



Cornstarch



62.5 μm

diameter: 5-20 μm ,
flat distribution of sizes (numbers)
Irregular shapes
 $\rho = 1.5 \text{ g/cm}^3$

“shear thickening suspension”

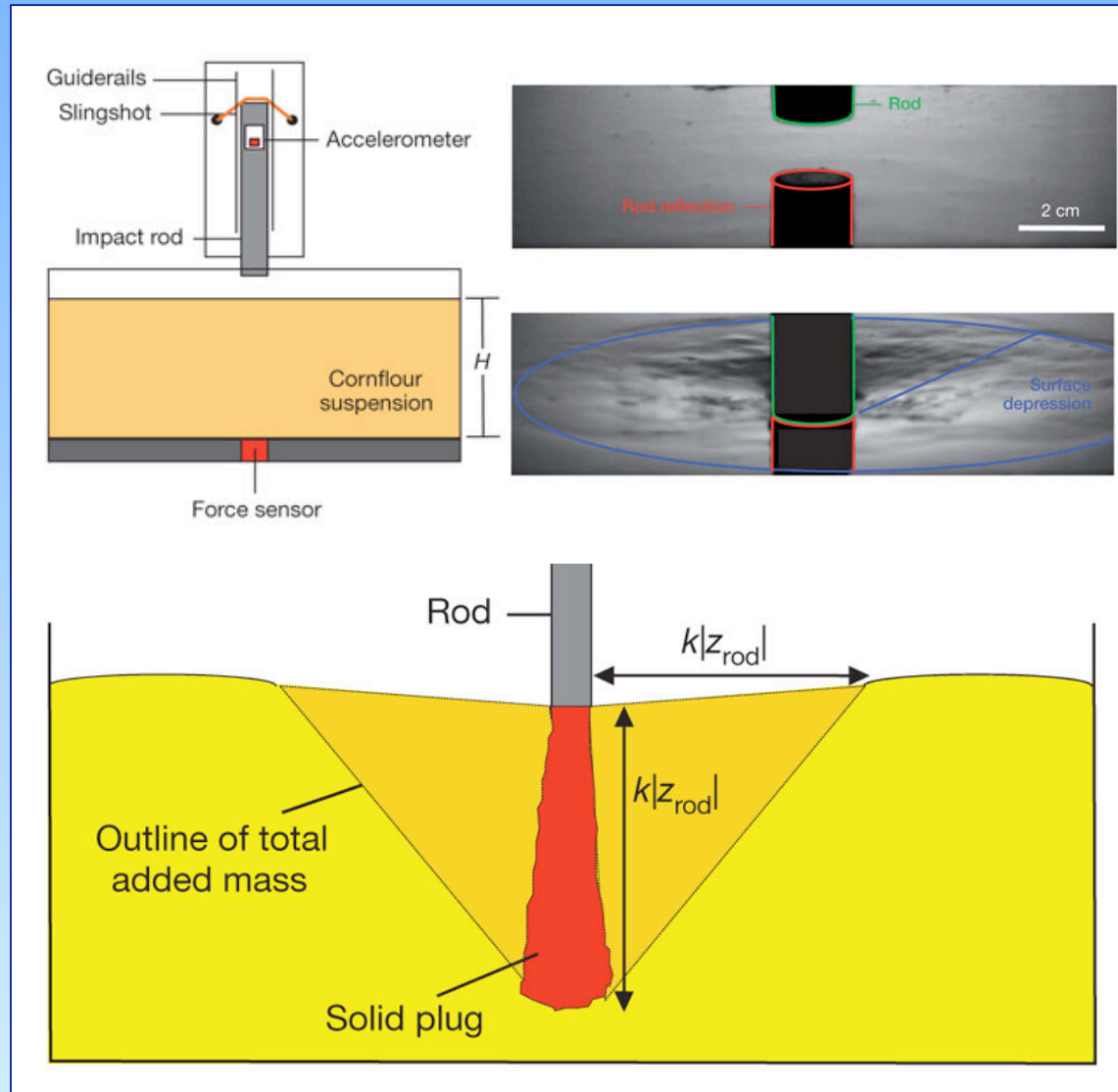
Cornstarch on a shaker



Walking on cornstarch



How is this possible?

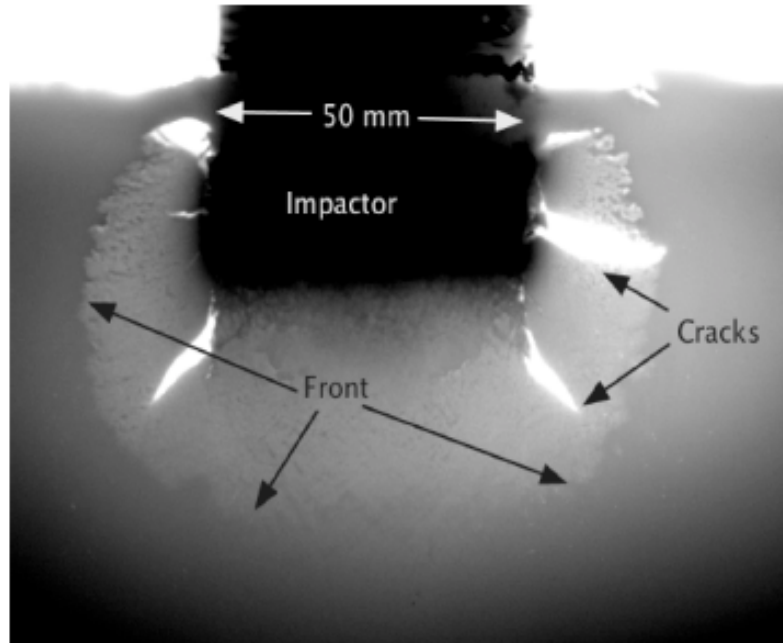


added mass
provides force

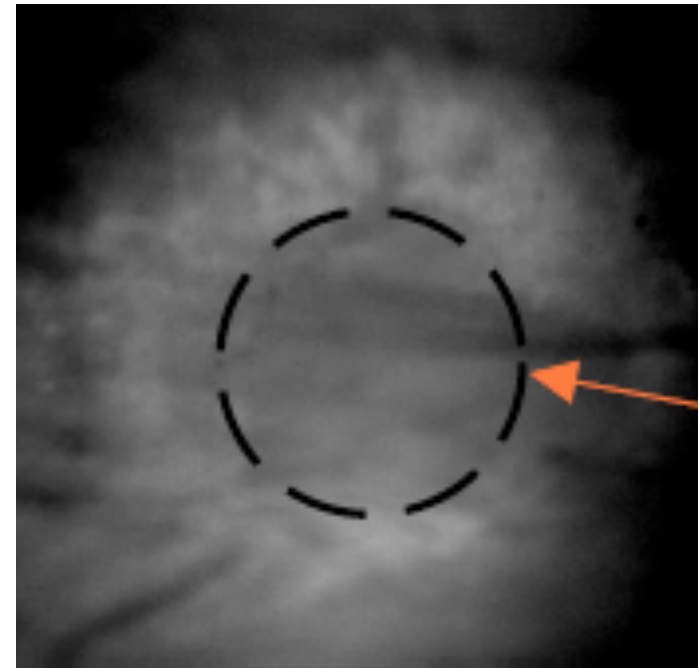
Waitukaitis & Jaeger,
Nature (2012)

Is this force large enough?

side view



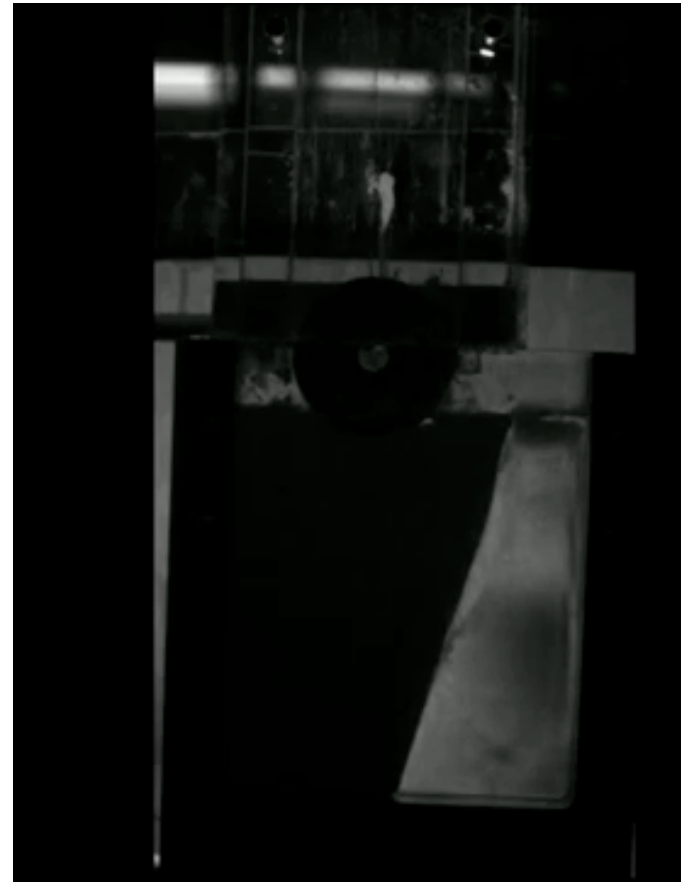
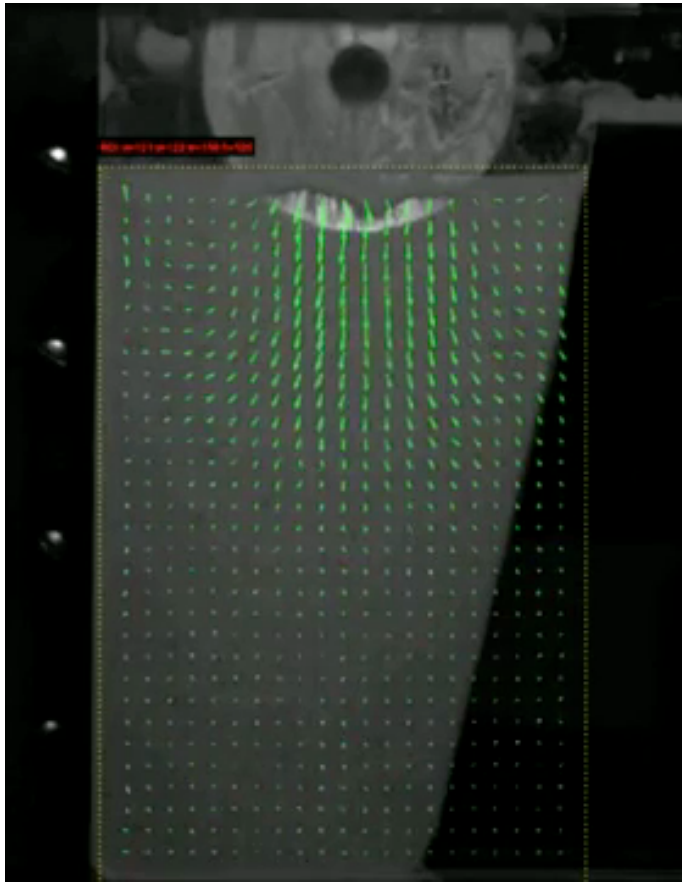
bottom view



above a critical impact velocity a solid-like (jammed) front moves towards bottom and provides the force

Mukhopadhyay, Allen & Brown, *cond-mat* (2014)

How fast is the shock wave?



shock wave speed $> 2,000$ m/s (!)

Lim, Barés & Behringer, *youtube* (2016)

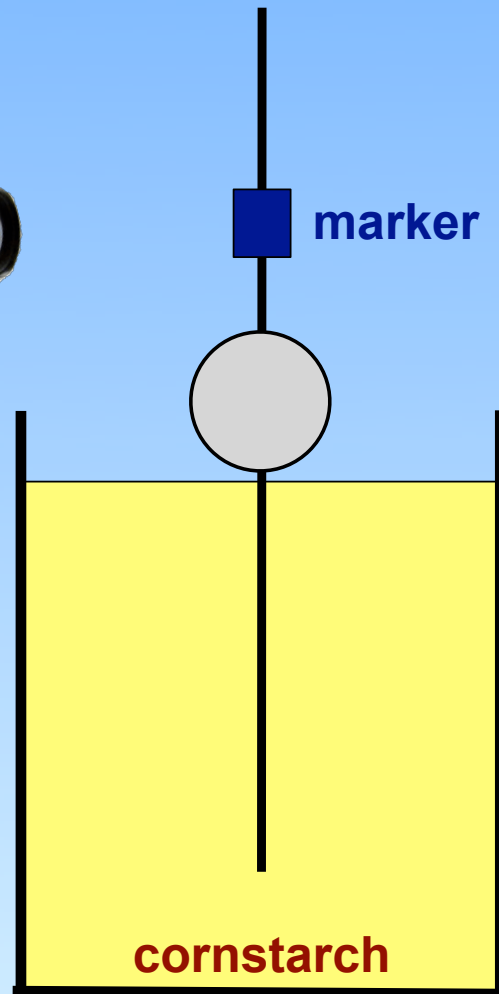
Example 3

**Settling in a cornstarch
suspension**

Experimental setup



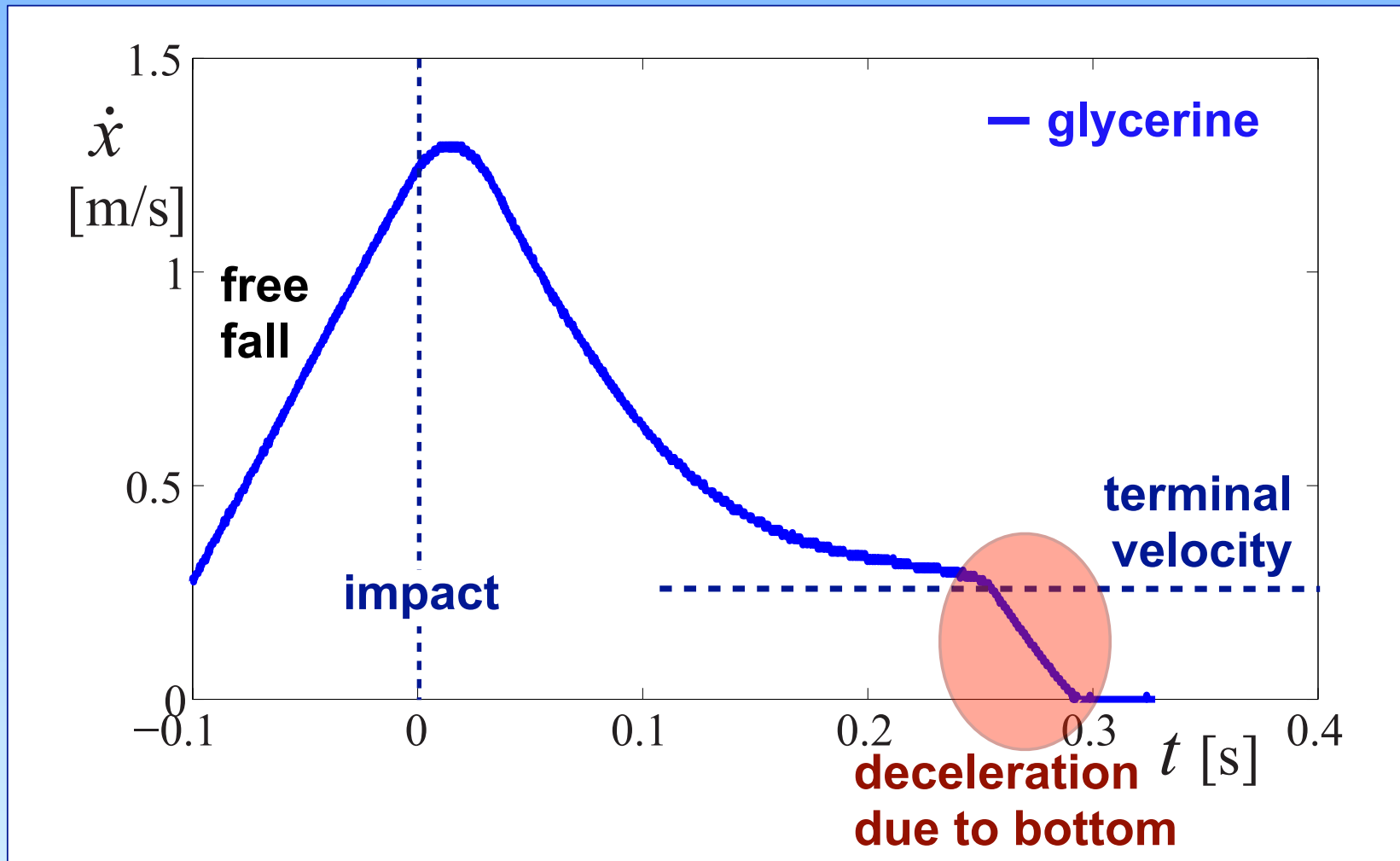
high-speed
camera



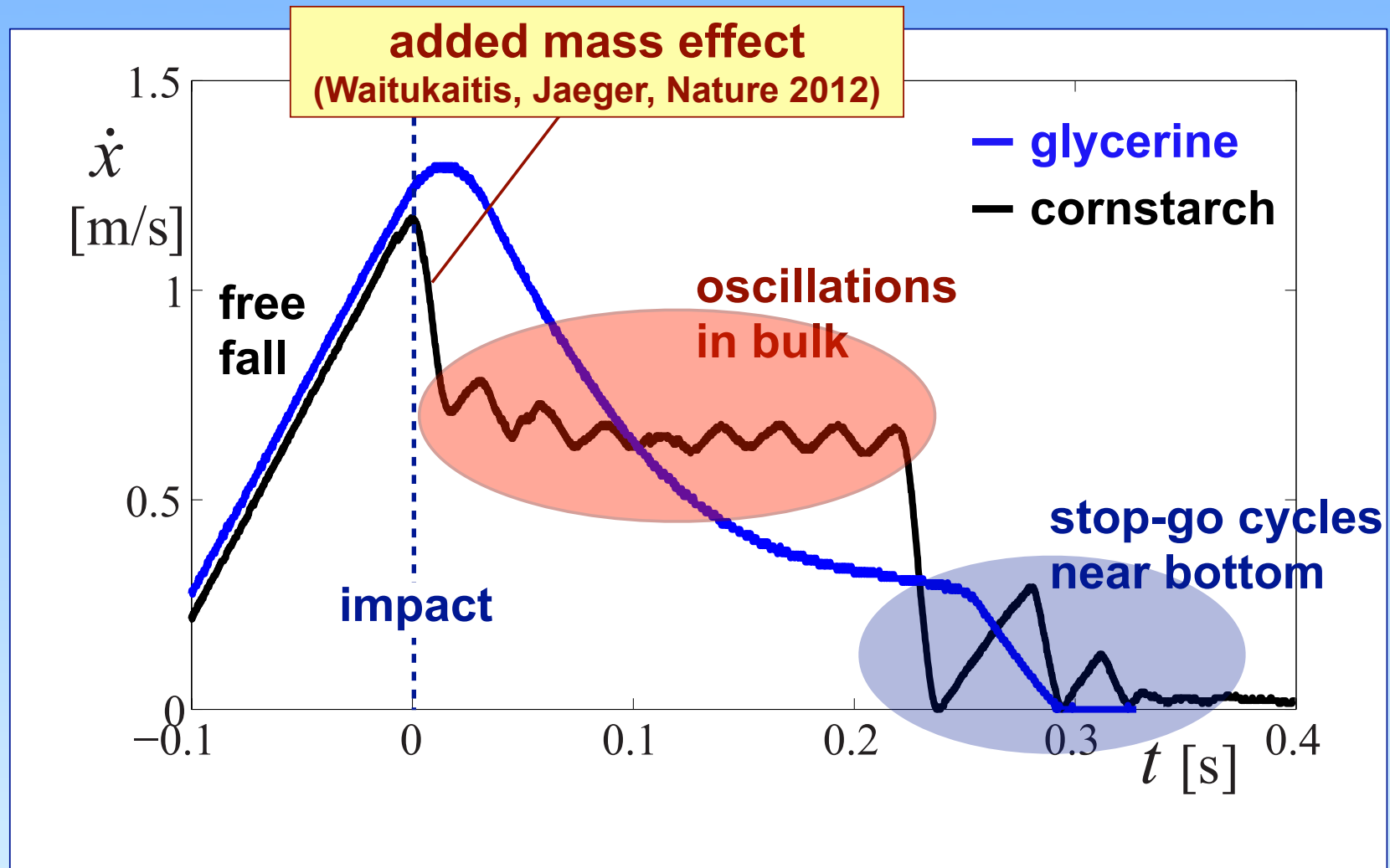
$x(t)$ (depth sphere
inside suspension)

Control parameters:
▶ packing fraction φ
▶ object mass

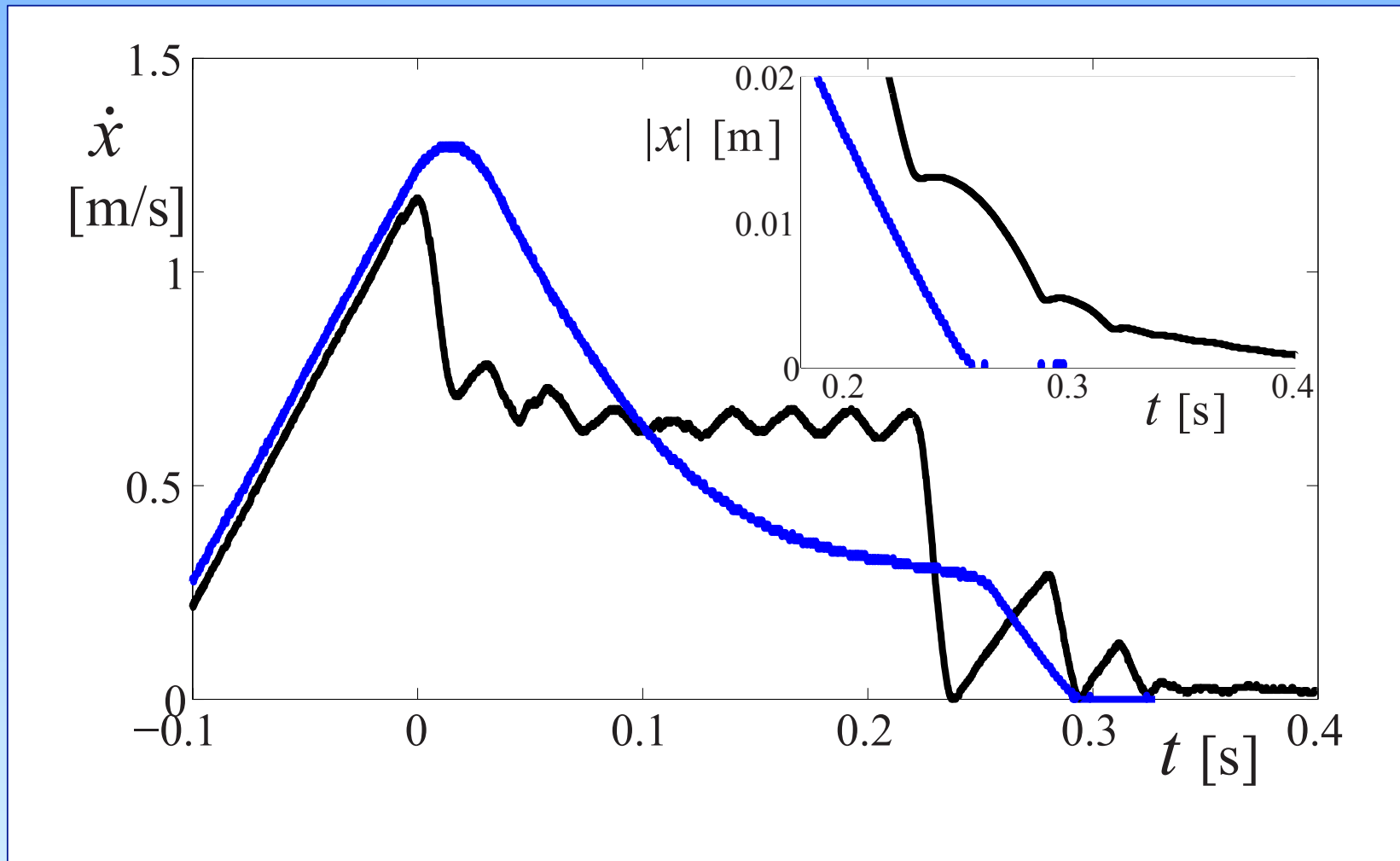
Liquid vs suspension



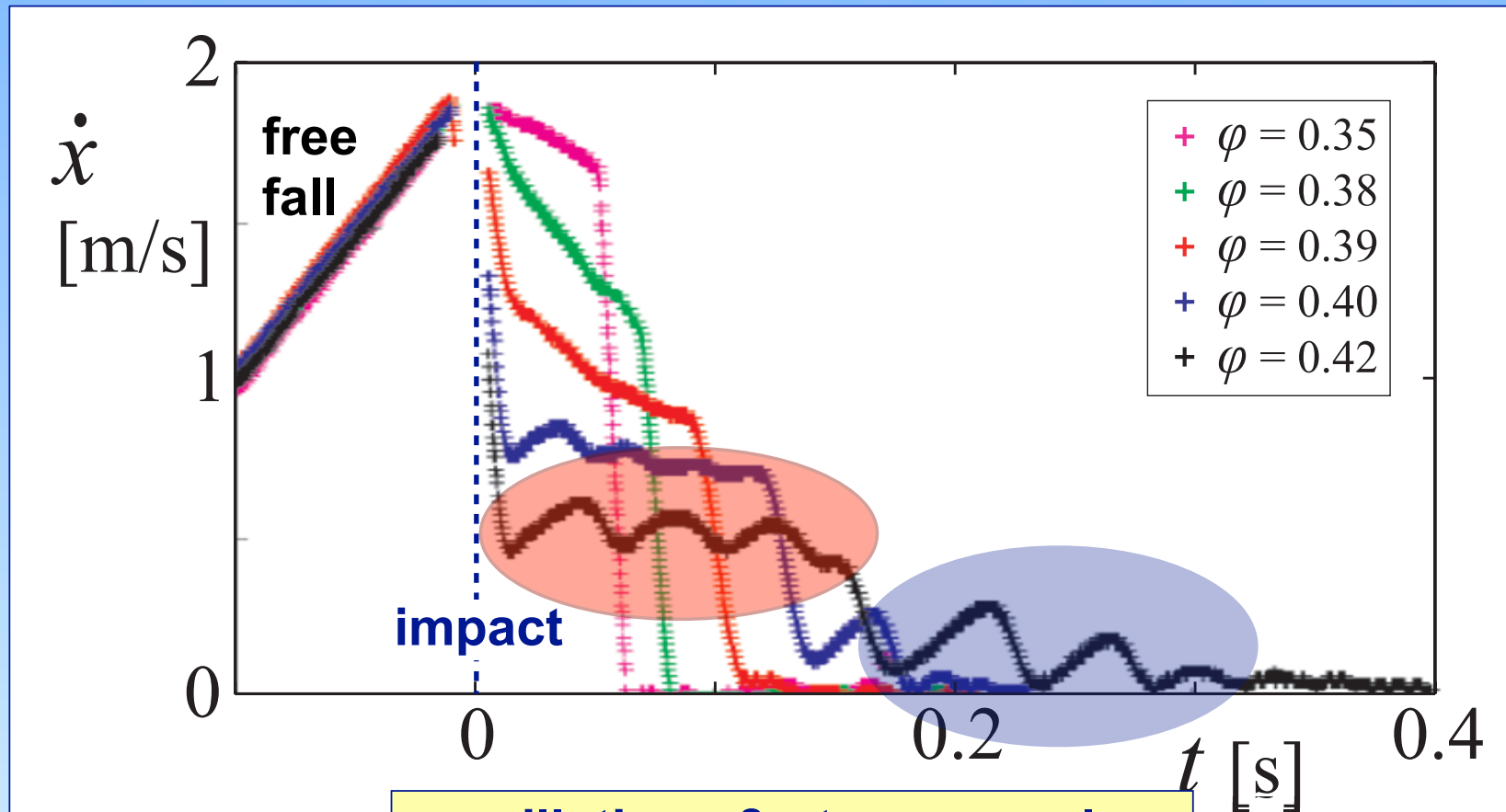
Liquid vs suspension



Liquid vs suspension



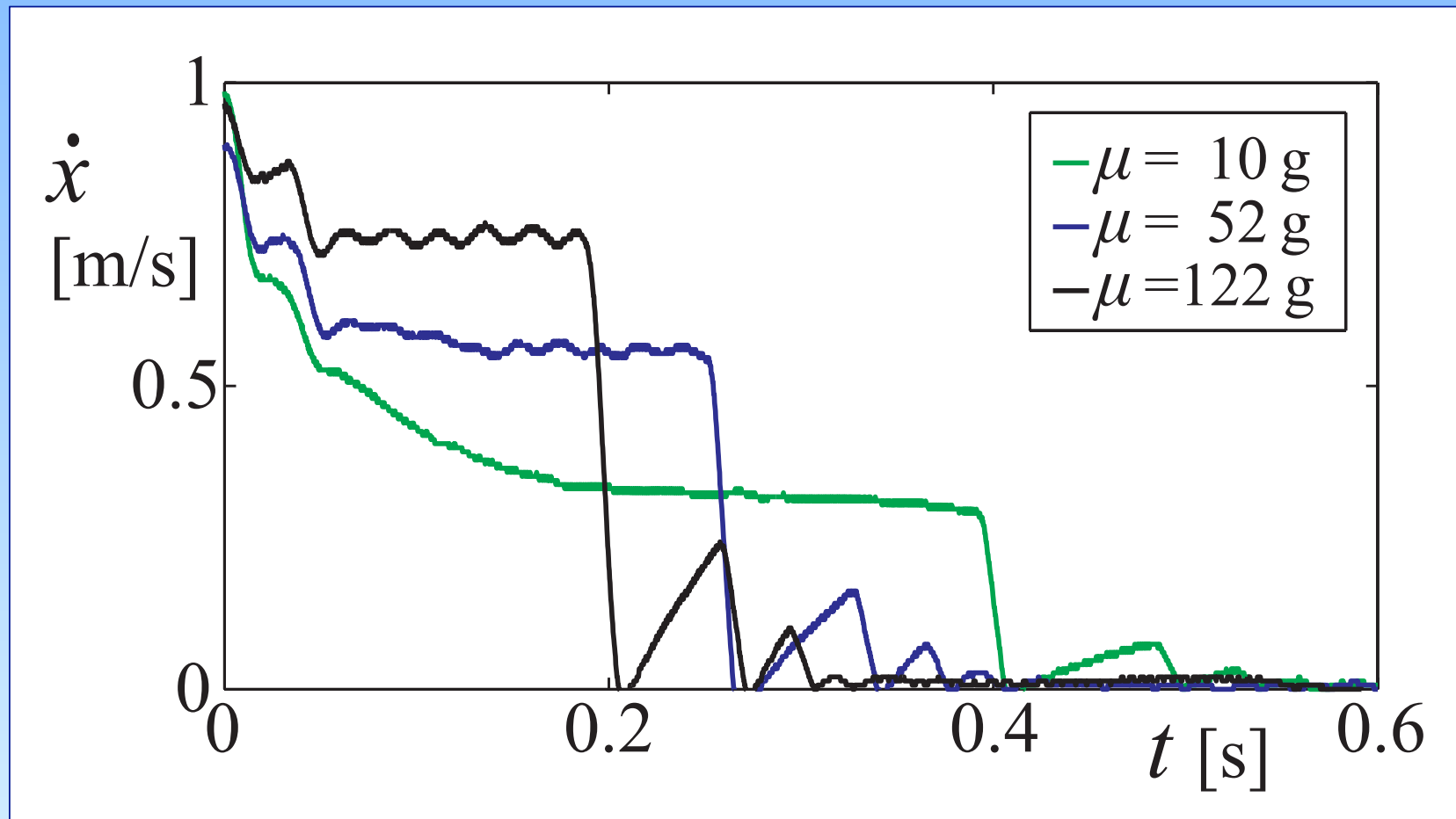
Increasing packing fraction ϕ



oscillations & stop-go cycles
appear for $\phi > 0.39$

Increasing sphere mass μ

$$\varphi = 0.44$$



Equation of motion

$$m\ddot{x} = \mu g + D$$

Added mass corrected mass:

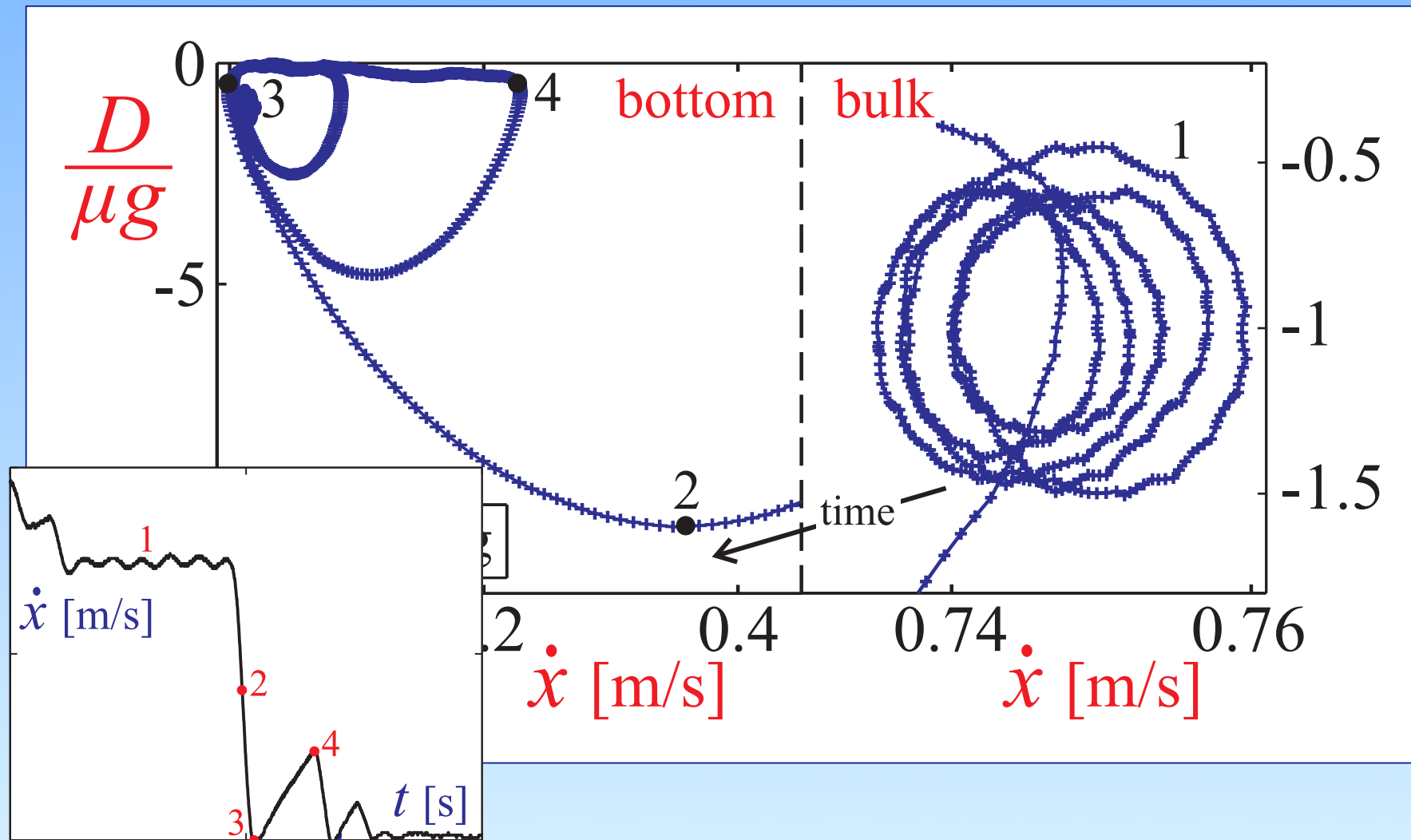
$$m = m_{sphere} + m_{added} = m_{sphere} + \frac{1}{12}\pi d^3 \rho_{susp}$$

Buoyancy corrected mass:

$$\mu = m_{sphere} - m_{buoy} = m_{sphere} - \frac{1}{6}\pi d^3 \rho_{susp}$$

use this equation to calculate drag D vs velocity \dot{x}

Drag D vs velocity \dot{x}



Bulk oscillations

What type of model could describe the bulk oscillations?

Shear thickening or other

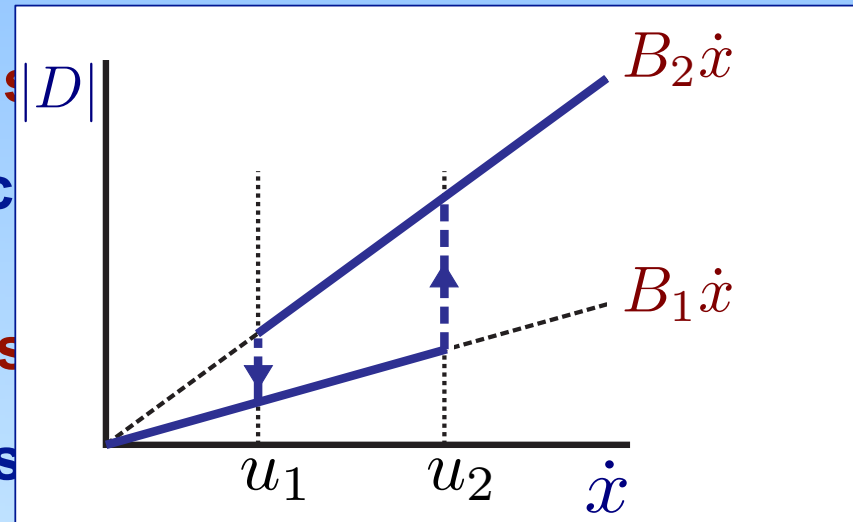
No. Leads to monotonic

Visco-elastic liquid models

No. Leads to damped os

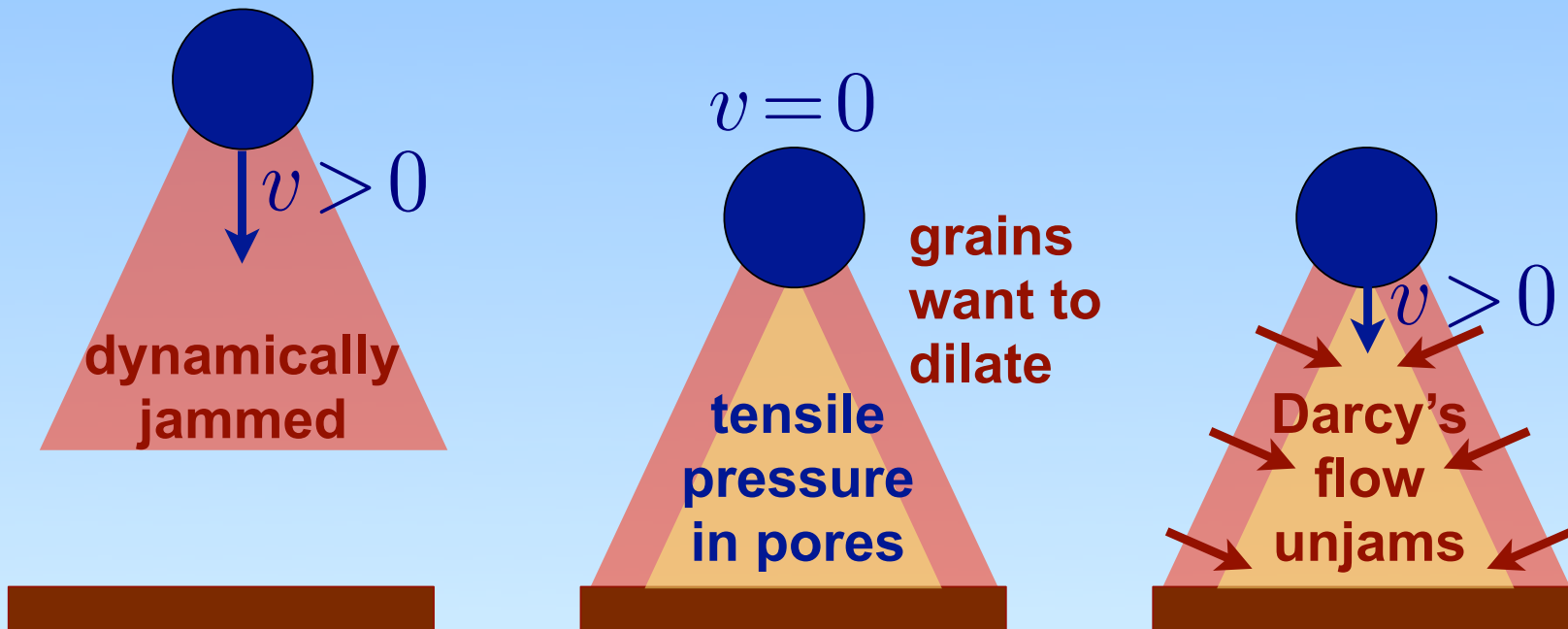
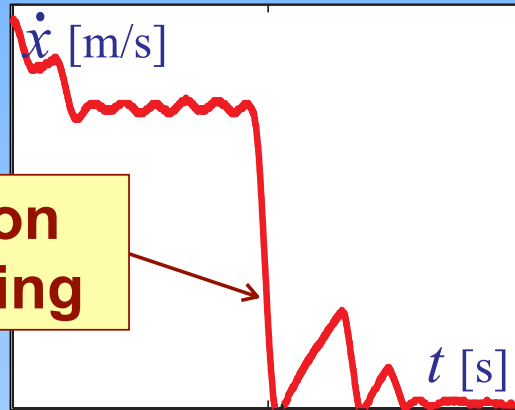
Hysteretic drag model? [R.D. Deegan, *Phys. Rev. E* 81, 036319 (2010).]

Works reasonably well



Stop-go cycles at the bottom

Fast deceleration points to jamming



similar to: S. Mukhopadhyay, B. Allen, E. Brown, arXiv:140719 (2014).

A minimal model

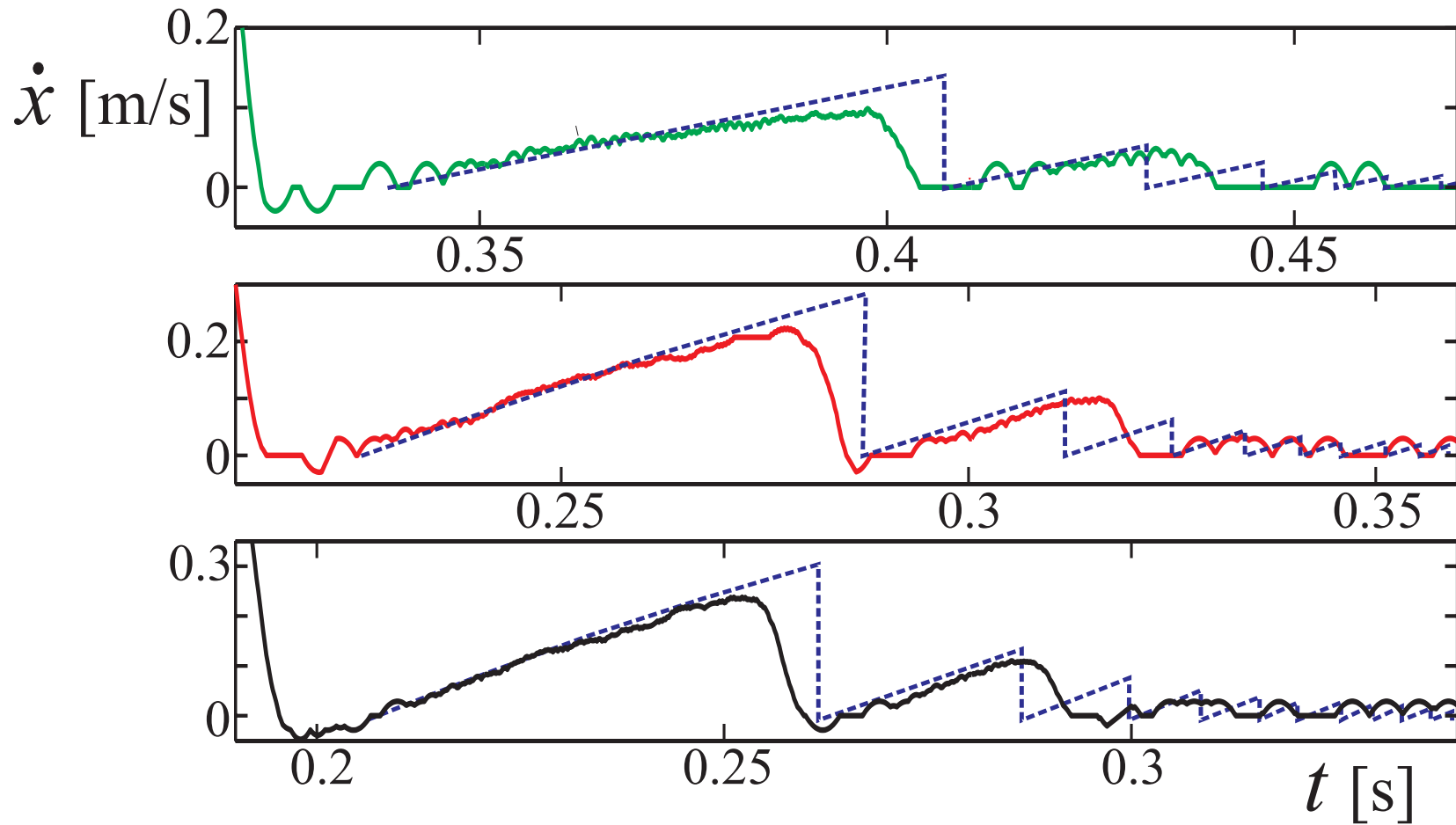
$$\begin{cases} m\ddot{x} = \mu g + D & \text{when } \phi < \phi_{cr} \\ \dot{x} = 0 & \text{when } \phi \geq \phi_{cr} \end{cases}$$

$$\dot{\phi} = -c \frac{\dot{x}}{x} - \kappa(\phi - \phi_{eq})$$

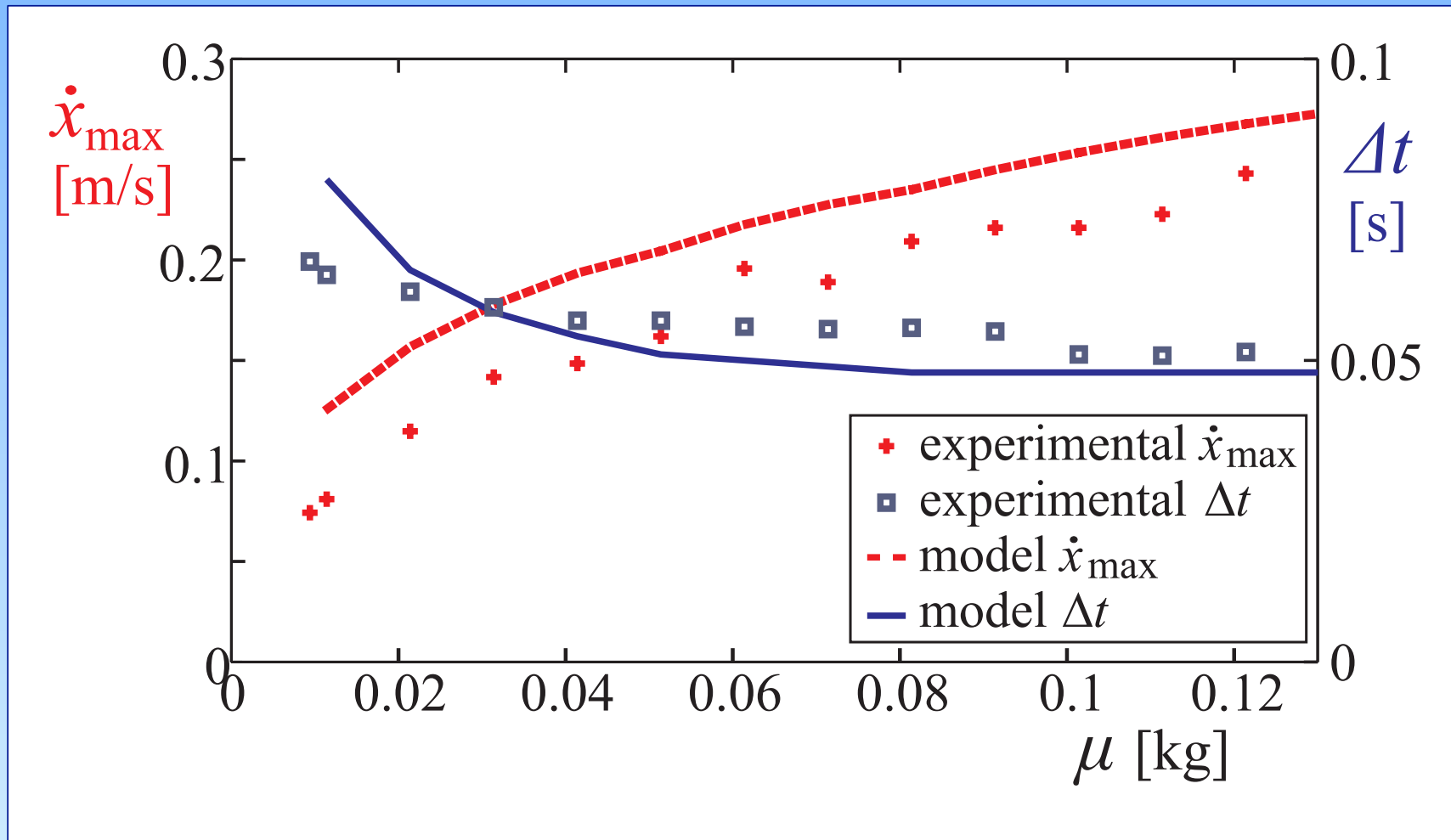
increases ϕ due to compression
($-\dot{x}/x =$ compression rate)

decreases ϕ due to relaxation

Comparing to experiment



Comparing to experiment





THANK YOU !