

JMBC course : Particle Technology
April 29 – May 03, 2019 U-Parkhotel,
UTwente, NL

Cyclone design



JMBC course 2019

Dr Pablo Garcia-Trinanes

p.garciatrinanes@gre.ac.uk

1

What is a cyclone?

- A device that separates particulate from gas (fluid) by centrifugal force.
- Works simply by the kinetic energy of the incoming mixture (flow stream) and the geometry of the cyclone.

2

How a cyclone works?

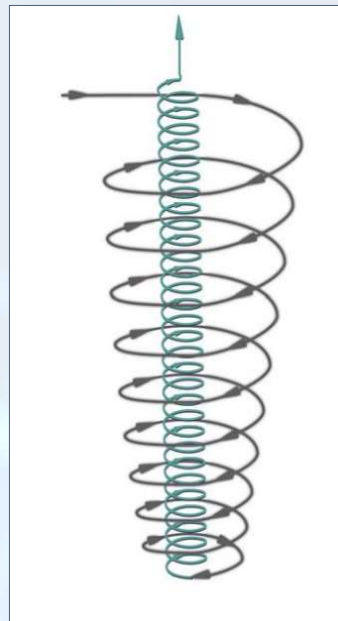
- **Two main factors affect cyclone efficiency**
 - velocity particle moves towards the wall or collection area of the cyclone where it is theoretically collected
 - length of time available for collection: Residence Time
- **Two main metrics describe cyclone performance**
 - Pressure drop
 - Fractional efficiency curve

JMBC

3

3

Basic flow patterns



JMBC

4

4

Industrial use



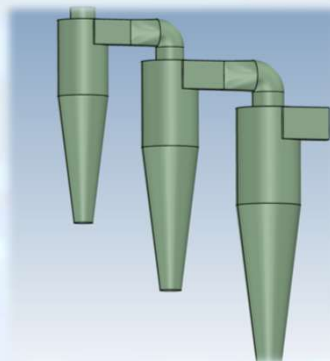
JMBC

5

5

Cyclone design

- Cyclones in series



JMBC

6

6

Cyclone design



JMBC

7

7

Cyclone design

- The rate of settling of suspended particles in a gas stream may be greatly increased if **centrifugal** rather than gravitational forces are employed.
- The gas mixture is introduced tangentially into a cylindrical vessel at a velocity of about 20-30 m/s and the clean gas is taken off through a central outlet at the top.
- The solids are thrown outwards against the cylindrical wall of the vessel, and then move away from the gas inlet and are collected in the conical base of the plant.

JMBC

8

8

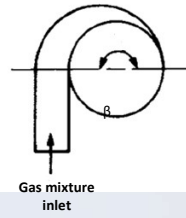
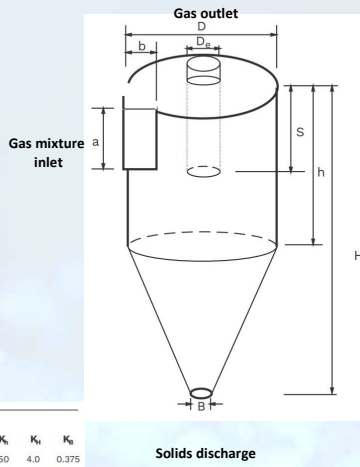
Cyclone design

$$D = \sqrt{\frac{IA}{0.1}} \quad K_s = \frac{S}{D}$$

$$K_a = \frac{a}{D} \quad K_h = \frac{h}{D}$$

$$K_b = \frac{b}{D} \quad K_B = \frac{B}{D}$$

$$K_e = \frac{D_e}{D} \quad K_H = \frac{H}{D}$$



Cyclone Design Configurations

Source	Recommended Duty	D	K _a	K _b	K _e	K _h	K _s	K _B	K _H	K _v	K _w
Stairmand	High efficiency	1.0	0.50	0.20	0.50	0.50	1.50	4.0	0.375		
Swift	High efficiency	1.0	0.44	0.21	0.40	0.50	1.40	3.9	0.40		
Lapple	General purpose	1.0	0.50	0.25	0.50	0.525	2.00	4.0	0.25		
Swift	General purpose	1.0	0.50	0.25	0.50	0.60	1.75	3.75	0.40		
Peterson and Whitby	Experimental	1.0	0.583	0.208	0.50	0.583	1.333	3.17	0.50		

JMBC

9

9

Cyclone design

High efficiency

High throughput



10

10

Cyclone design

High efficiency



High throughput



11

11

Cyclone design

High efficiency



High throughput



12

12

Cyclone design

High efficiency

High throughput



Cyclone design

Cyclone design	Collecting efficiency (%)		
	Koch & Licht	Enliang & Yingmin	Average
Stairmand HE	87.5	84.9	86.2
Swift HE	87.8	83.0	85.4
Lapple LE	86.9	85.2	86.1
Swift LE	86.9	85.2	86.1
Peterson/Whitby LE	86.1	85.4	85.8

Cyclone design

- The cyclone pressure drop is a function of the cyclone dimensions and its operating conditions.
- The pressure drop over a cyclone is caused by the area changes, the wall friction, change of the flow direction and the dissipation in the vortex finder (outlet tube).
 - Entry pressure loss in the tangential inlet duct
 - Frictional pressure loss
 - The pressure loss caused by the change of the flow direction
 - Entry pressure loss at the inner vortex entrance

15

15

Cyclone design

Cyclone design	Collecting efficiency (%)		
	Koch & Licht	Enliang & Yingmin	Average
Stairmand HE	87.5	84.9	86.2
Swift HE	87.8	83.0	85.4
Lapple LE	86.9	85.2	86.1
Swift LE	86.9	85.2	86.1
Peterson/Whitby LE	86.1	85.4	85.8

Cyclone design	Pressure drop (hPa)
Stairmand HE	1.7
Swift HE	1.6
Lapple LE	1.5
Swift LE	1.5
Peterson/Whitby LE	1.6

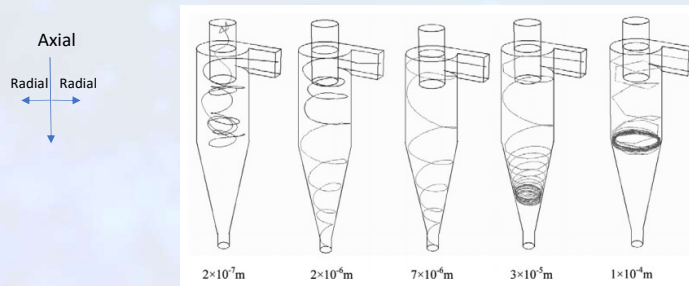
1hPa=100Pa

16

16

Cyclone design

- This separator is very effective unless the gas contains a large proportion of particles less than about 10 μm in diameter.
- Trajectories of particles with different diameters (an example)



JMBC

17

17

The Dietz model

$$\eta = 1 - \left[K_0 - (K_1^2 + K_2)^{0.5} \right] \times \exp \left[\frac{-\pi(2S - a)\rho_p d^2 v_i}{18\mu ab} \right]$$

$$K_0 = \frac{1}{2} \left[1 + \left(\frac{D_c}{D} \right)^{2n} \left(1 + \frac{9\mu ab}{\pi\rho_p l d^2 v_i} \right) \right]$$

$$K_1 = \frac{1}{2} \left[1 - \left(\frac{D_c}{D} \right)^{2n} \left(1 + \frac{9\mu ab}{\pi\rho_p l d^2 v_i} \right) \right]$$

$$K_2 = \left(\frac{D_c}{D} \right)^{2n}$$

- η fractional collection efficiency for particles of one size (dimensionless)
- μ gas viscosity, Pa · s
- a cyclone inlet height, m
- b cyclone inlet width, m
- l natural length of cyclone, m
- S cyclone gas outlet duct length, m
- d particle diameter, m
- v_i gas inlet velocity, m/s
- D cyclone body diameter, m
- D_c cyclone gas outlet diameter, m
- n cyclone vortex exponent

JMBC

18

18

Cyclone design

- Trajectories of tracing particles entering from different inlet regions



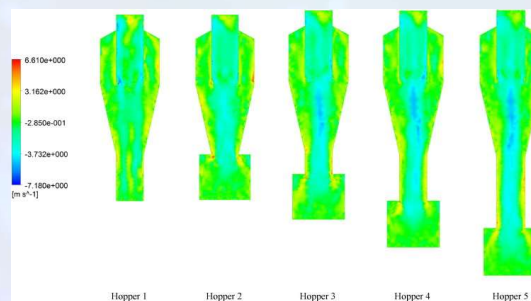
JMBC

19

19

Cyclone design

- There have been several studies in which the flow patterns within the body of the cyclone separator have been modelled using a computational Fluid Dynamics (CFD) technique.



Axial velocity contours along the vertical axis of cyclone separators with different dust outlet geometries

See also

<https://youtu.be/Le9UJXJvKpM>

JMBC

20

20

(Some references)

- C.B. Shepherd, C.E. Lapple, (1939) Flow pattern and pressure drop in cyclone dust collectors, *Ind. Eng. Chem.* 31 (8) 972–984
- M. Shapiro, V. Galperin, (2005) Air classification of solid particles: a review, *Chem. Eng. Proc.* 44 (2) 279–285
- Sakura Ganegama Bogodage, Andrew Y.T. Leung, (2015) CFD simulation of cyclone separators to reduce air pollution, *Powder Technology*, Vol. 286, 488-506
- B. Wang, D.L. Xu, K.W. Chu, A.B. Yu, (2006) Numerical study of gas–solid flow in a cyclone separator, *Applied Mathematical Modelling*, Vol. 30, 11, 1326-1342